

## Techno-Economic Analysis

- Setting R\&D priorities
- Benchmarking
- Informing multi-sectoral analytical activities
- Track Program R\&D progress against goals
- Identify technology process routes and prioritize funding
- Program direction decisions:
- Are we spending our money on the right technology pathways?
- Within a pathway: Are we focusing our funding on the highest priority activities?


## Terminology and Concepts

- Nth plant economics
- Costs represent the case where several biorefineries with this technology have been built, which assumes lower contingency and other cost escalation factors
- Assumes no risk premiums, no early-stage R\&D, or start-up costs
- Pioneer plant
- Costs represent a first-of-a-kind construction, where added cost factors are included for contingency and risk
- Most closely represented by IBR projects
- Few estimates available in the public domain
- Design Case:
- Detailed, peer reviewed process simulation based on ASPEN or Chemcad
- Establishes cost of production at biorefinery boundary
- Provides estimate of nth plant capital and operating costs
- Based on best available information at date of design case
- Scope: feedstock cost, feedstock logistics, conversion cost, profit for biorefinery
- Excludes: taxes, distribution costs, tax credits or other incentives


## Introduction

- R\&D targets for cellulosic ethanol achieved in 2012
- Technical targets met corresponding to a MESP \$2.05 (thermochem) and $\$ 2.15$ (biochem)
- Validated with integrated pilot at NREL
- In March 2012, initiated effort to select new pathways to hydrocarbon fuels and intermediates
- Focus on full pathways - feedstock to end product


## Pathway Selection Process



## March 2013

Preliminary cost goals published in MYPP and key areas of research identified

## September 2013

Full design cases completed for 4 pathways (Fermentation of Lignocellulosic Sugars, ALU, AHTL, Fast Pyrolysis)

## September 2012

PNNL/NREL completed joint milestone report detailing analysis effort

## October 2012

Pathways prioritized and timeline for analysis developed

Planned Activities

## September 2014

Year-by-year targets completed for 2013 pathways. Full design cases completed for 4 additional pathways (ex situ and in situ Catalytic Pyrolysis, Catalytic Upgrading of Lignocellulosic Sugars, Syngas to Hydrocarbons).

## Criteria for downselect included:

- Feasibility of achieving programmatic cost goal of $\$ 3 /$ gal
- Near/Mid/Long-term technoeconomic potential
- Potential national impact
- Feedstock availability/flexibility
- Data availability across the full pathway
- Co-product economics
- Potential volumetric impact in 2030
- Environmental Sustainability


## Selected Pathways

- Fermentation of Sugars to Hydrocarbons
- Catalytic Upgrading of Sugars to Hydrocarbons
- Fast Pyrolysis*
- Ex-Situ Catalytic Pyrolysis
- In-Situ Catalytic Pyrolysis
- Whole Algae Hydrothermal Liquefaction (AHTL)
- Algal Lipid Upgrading (ALU)
- Syngas Upgrading to Hydrocarbon Fuels
* Update to the current design case


## Fermentation of Sugars to Hydrocarbons



Biomass-derived sugars-separated from feedstocks through a series of chemical and biochemical processes-are further transformed, recovered, and purified to yield hydrocarbons for fuels and co-product commodities.

## Rationale for Selecting Pathway

- Better utilization of biomass derived carbon sources (higher yields)
- Path to 2017 cost targets achievable via reasonable co-product credits
- Leverage previous front-end modeling and research through sugar production
- Back-integration and lessons-learned from IBR projects hasten process development


## Catalytic Upgrading of Sugars to Hydrocarbons



Biomass-derived sugars-separated from feedstock through a series of chemical and biochemical processes-are upgraded via aqueous phase reforming into hydrocarbons for fuels and co-product commodities.

## Rationale for Selecting Pathway

- Better utilization of biomass derived carbon sources (higher yields)
- Path to 2017 cost targets achievable with reasonable co-product credits
- Leverage previous front-end modeling and research through sugar production
- Back-integration and lessons-learned from IBR projects hasten process development


## Algal Lipid Upgrading (ALU)



Bio-oil is extracted from algal biomass via high-pressure homogenization and a hexane solvent; the algal oil can then be hydrotreated to produce advanced hydrocarbon fuels.

Rationale for Selecting Pathway

- Raw algal oil intermediate is expected to require relatively mild upgrading (hydrotreating) to finished fuels at marginal cost
- Algal biomass can be tailored to produce specific components for fuel and/or product markets (potential for high-value coproducts)
- Nutrient recycle and heat and power integration through anaerobic digestion improves process economics and sustainability profile


# Whole Algae Hydrothermal Liquefaction (ABHTL) 



Bio-oils are separated from water via heat and pressure, so they can be catalytically hydrotreated and converted to advanced hydrocarbon fuels.

## Rationale for Selecting Pathway

- HTL both extraction and conversion process (50-70\% of carbon captured)
- Higher yield than other known extractions
- HTL is wet process using only water, no drying or solvent recovery needed
- Oil phase lower in oxygen content and easy to upgrade to hydrocarbons
- CHG is faster, smaller, and more complete than Anaerobic Digestion (AD)
- Leverages NABC, NAABB, and new AOP work in FY13


## Fast Pyrolysis and Upgrading and Hydroprocessing



Biomass is rapidly heated in a fluidized bed reactor to yield vapors, which are condensed into a liquid bio-oil. This bio-oil is subsequently hydroprocessed to produce hydrocarbon biofuel blendstocks.

Rationale for Selecting Pathway

- Continuation of existing pathway


## Ex-situ Catalytic Fast Pyrolysis



Biomass is rapidly heated in a fluidized bed reactor containing a catalyst to yield vapors, which are catalytically modified and condensed into a partially stabilized and deoxygenated liquid bio-oil. This stable bio-oil is subsequently upgraded to produce hydrocarbon biofuel blendstocks.

## Rationale for Selecting Pathway

- Oil is lower in oxygen and likely easier to upgrade to hydrocarbons than fast pyrolysis derived bio-oil
- Greater control of gas/solid/liquid distribution as compared to fast pyrolysis
- May have a lower catalyst inventory
- Pathway R\&D will facilitate upgrading step chemistry understanding and optimum catalyst/operating conditions


## In-situ Catalytic Fast Pyrolysis



Biomass is rapidly heated in a fluidized bed reactor containing a catalyst to yield a partially stabilized and deoxygenated bio-oil vapor. The vapor is condensed into a liquid bio-oil and subsequently upgraded to produce hydrocarbon biofuel blendstocks.

## Rationale for Selecting Pathway

- Requires only one liquefaction reactor and will have lower CapEX
- May have a lower OpEx if larger size feedstock particles are acceptable
- Oil is lower in oxygen and likely easier to upgrade to hydrocarbons than fast pyrolysis derived bio-oil
- Leverages ex-situ Catalytic Pyrolysis R\&D upgrading step chemistry understanding and optimum catalyst/operating conditions


## Syngas Upgrading to Hydrocarbon Fuels



Biomass feedstocks are gasified to produce a clean syngas, which is used as a feedstock for hydrocarbon biofuel production.

## Rationale for Selecting Pathway

- Exploits mixed alcohol synthesis catalysts advances, leverages existing work in gasification and syngas cleanup
- Opportunity to improve catalyst performance (selectivity, lifetime, coking) to enable higher hydrocarbon yields
- Process intensification opportunity


## Next Steps

$>$ Identify preliminary cost goals for each of the conversion pathways and determine key areas of research for each technology (2013)
$>$ Set final cost goals and technical targets for each pathway (2013-2014)
> Publish design case reports for all pathways (2014 2015)
> Continue to explore new pathway options (ongoing)

## Back-Up Slides

## Pathways included in initial analysis

| Technology Area | Pathway |
| :---: | :---: |
| Sugars | Fermentation of Sugars to Hydrocarbons |
|  | Catalytic Upgrading of Sugars to Hydrocarbons |
|  | Fermentation of Sugars via Heterotrophic Algae to Hydrocarbons |
| Oils | Fast Pyrolysis and Upgrading |
|  | Catalytic Pyrolysis - ex situ |
|  | Catalytic Pyrolysis - in situ |
|  | Hydropyrolysis |
|  | Hydrothermal Liquefaction |
|  | Solvent Liquefaction |
| Algae | Whole Algae Hydrothermal Liquefaction (ABHTL) |
|  | Algal Lipid Extraction Upgrading to Hydrocarbons (ALU) |
| Gaseous Intermediates | Syngas to Methanol to Triptyls |
|  | Syngas Fermentation and Upgrading to Hydrocarbons |
|  | Landfill Gas Upgrading to Hydrocarbons |
|  | Gasification with Fermentation to Oxygenates |
| Other | Anaerobic digestion to CNG |
|  | Anaerobic digestion to Hydrocarbons via GTL |
|  | Coal Biomass to Liquids |

