

Development of Unified PEM Fuel Cell Models

DOE CARAT Program

**Hongtan Liu
University of Miami**

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DOE Fuel Cells for Transportation Program
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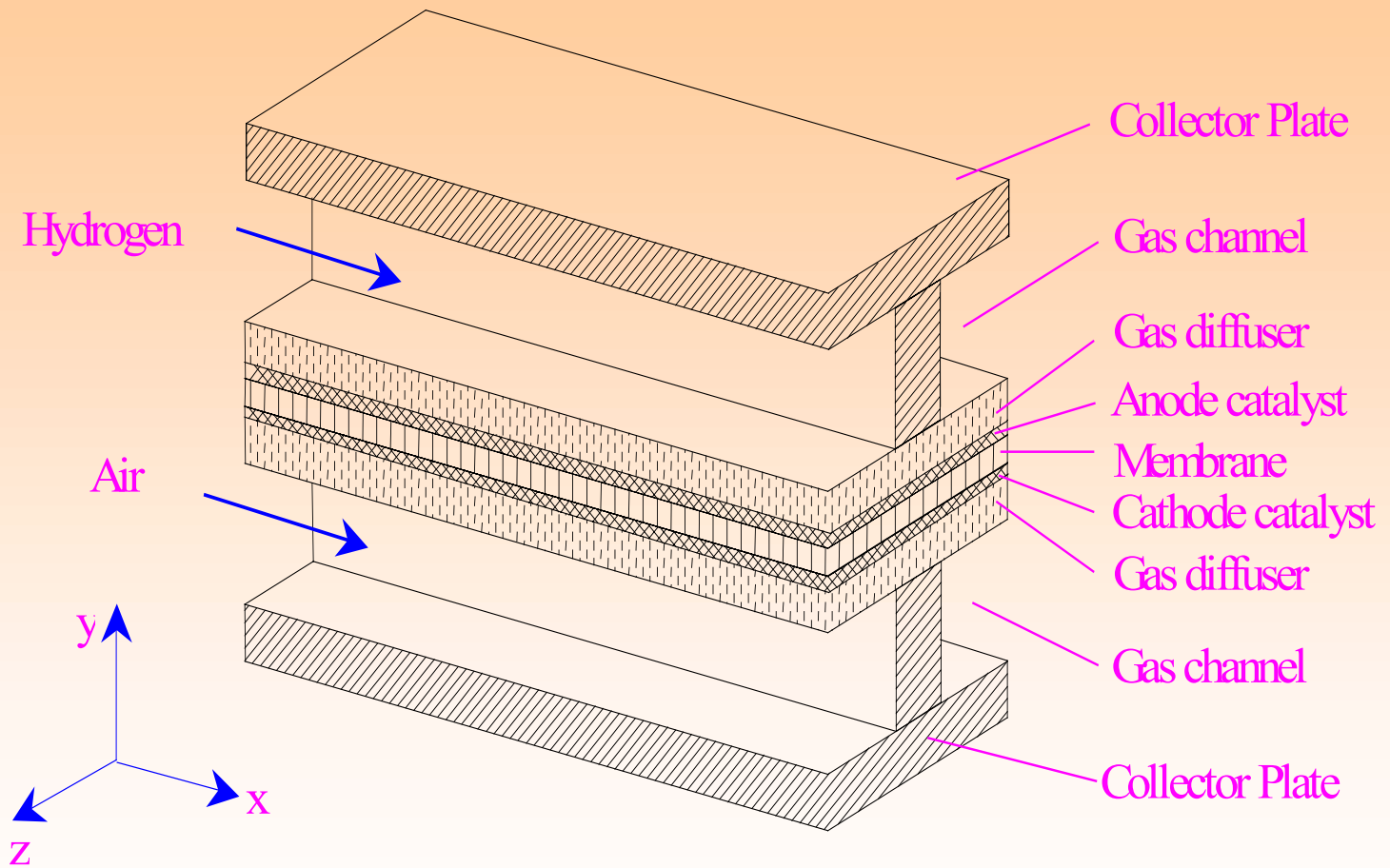
Objective

- **Demonstrate the feasibility of unified model approach to eliminate errors due to approximate boundary conditions at various interfaces**
- **Develop a comprehensive 3-D fuel cell model**
- **Develop reliable tools for design and optimization of fuel cells, stacks, and systems (long-term)**

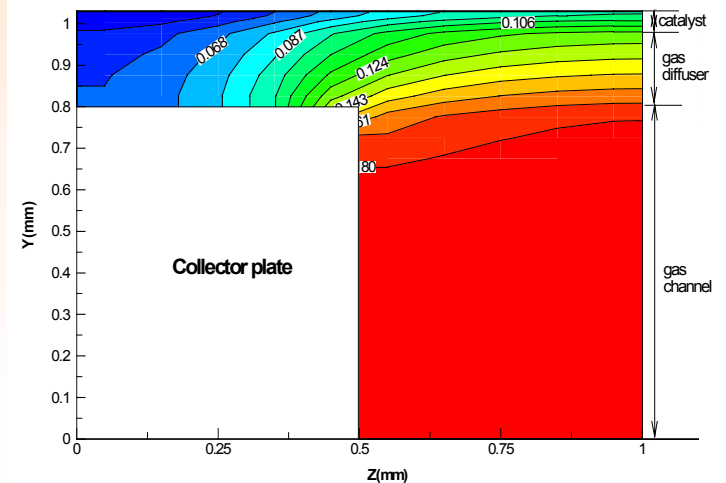
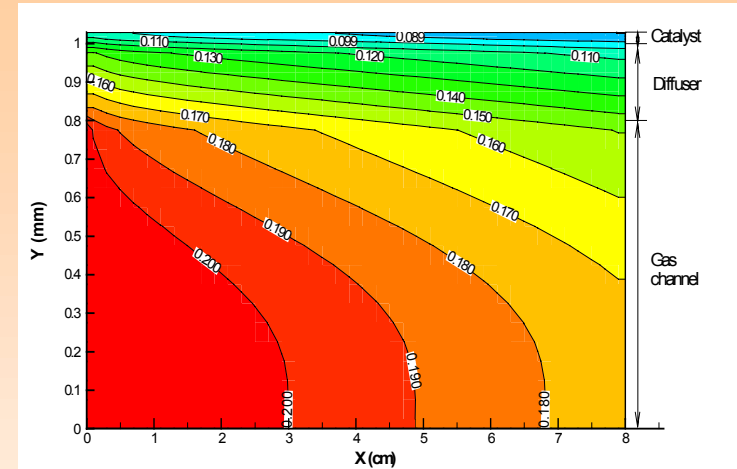
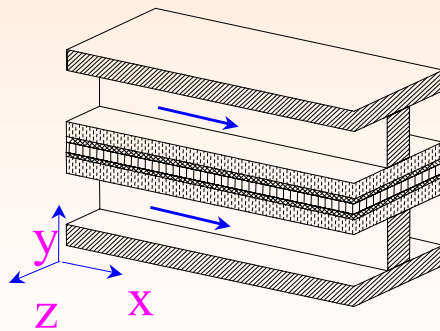
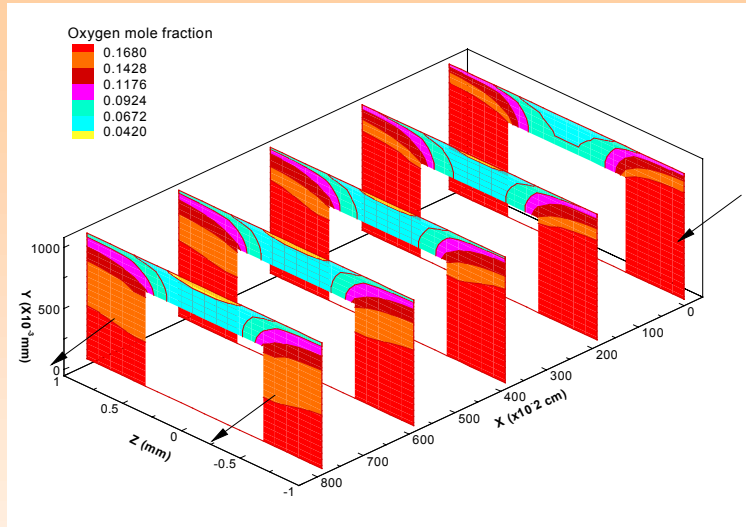
Approach

- **Develop general mathematical models valid in different parts of a fuel cell**
- **Eliminate boundary conditions at the various interfaces**
- **Adaptability: different levels of model complexity, easy to update, custom model incorporation**
- **Independent package (not based on any CFD package) - economical**
- **Robust and high-speed**

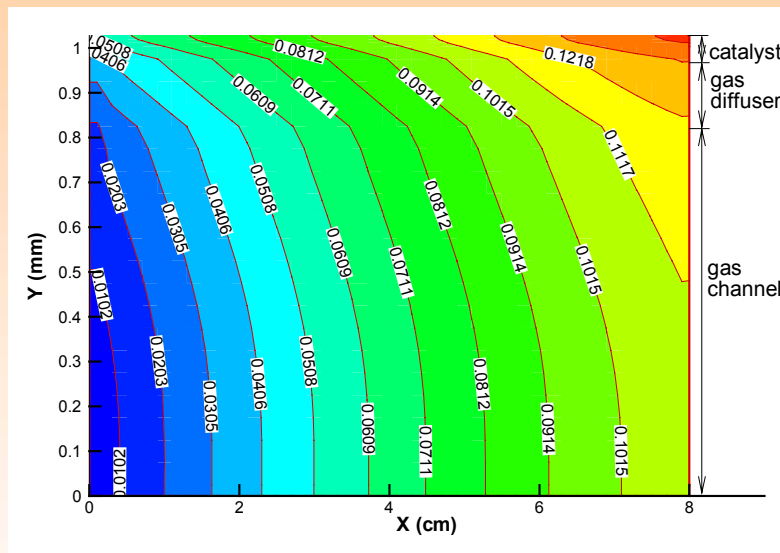
3D fuel cell model



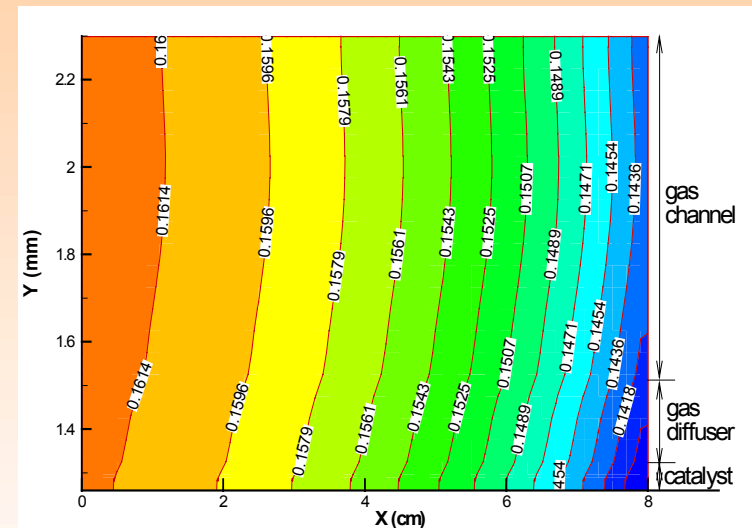
Sample results-3D model: oxygen molar fraction



Sample results - 3D model: water contours

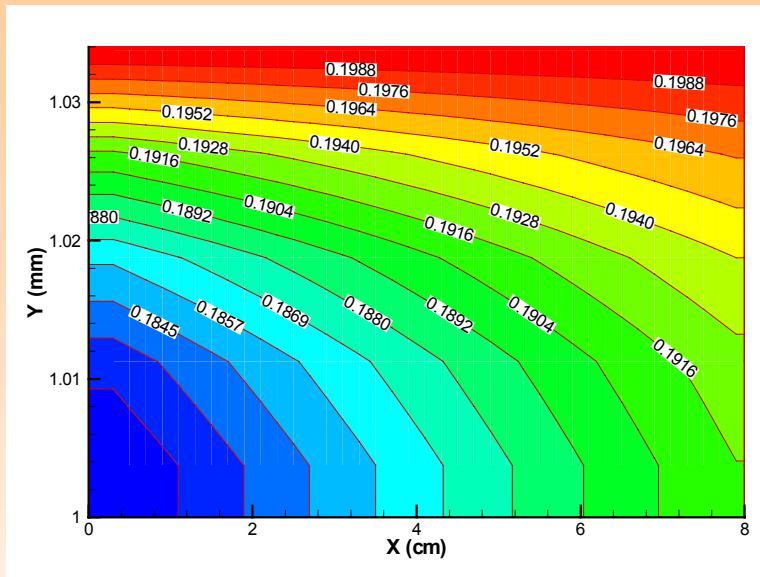


Cathode side

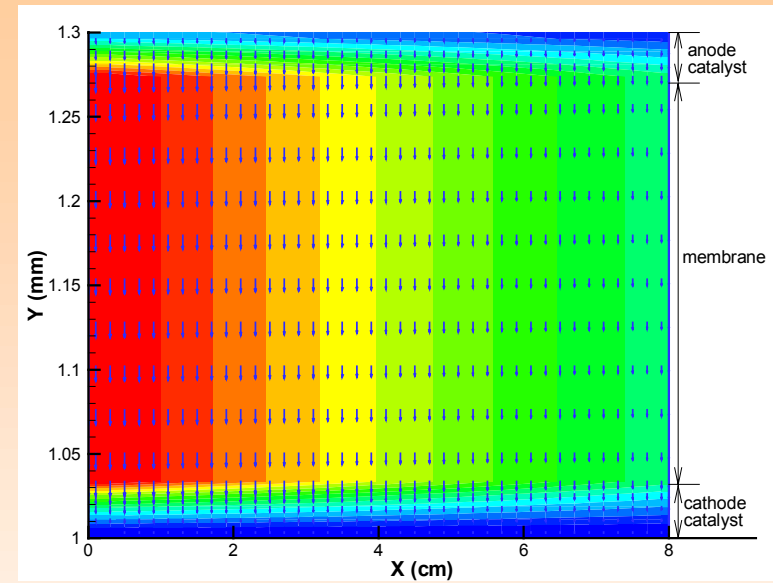


Anode side

Sample results - 3D model

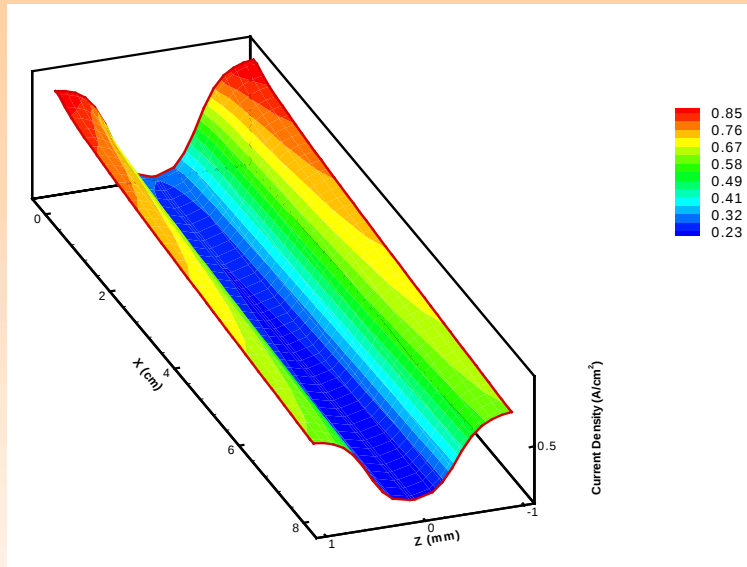


**Overpotential distribution
within the cathode catalyst
layer**

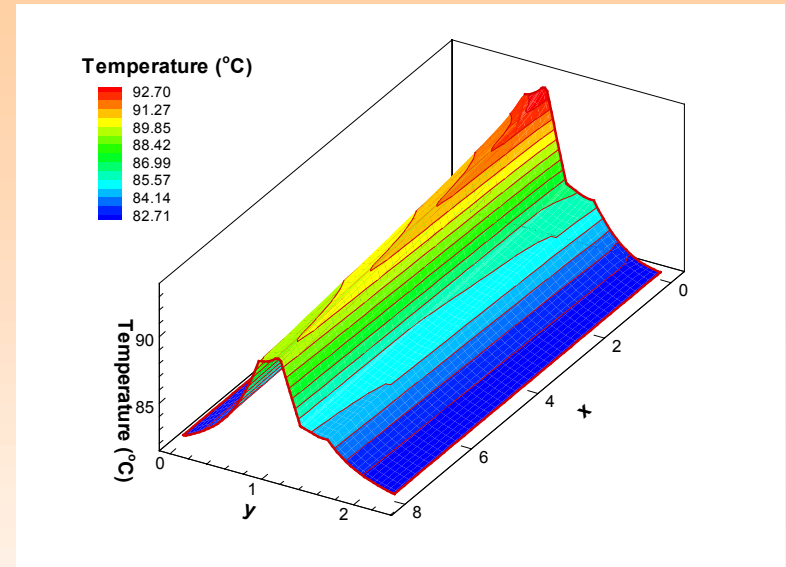


**Current density distribution
within the PEM**

Sample results – 3D model



Current density distribution

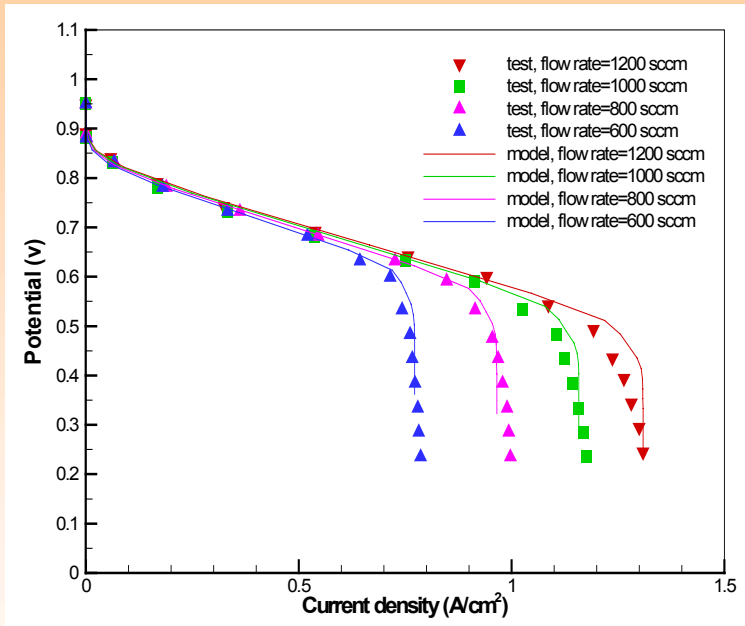


Temperature distribution

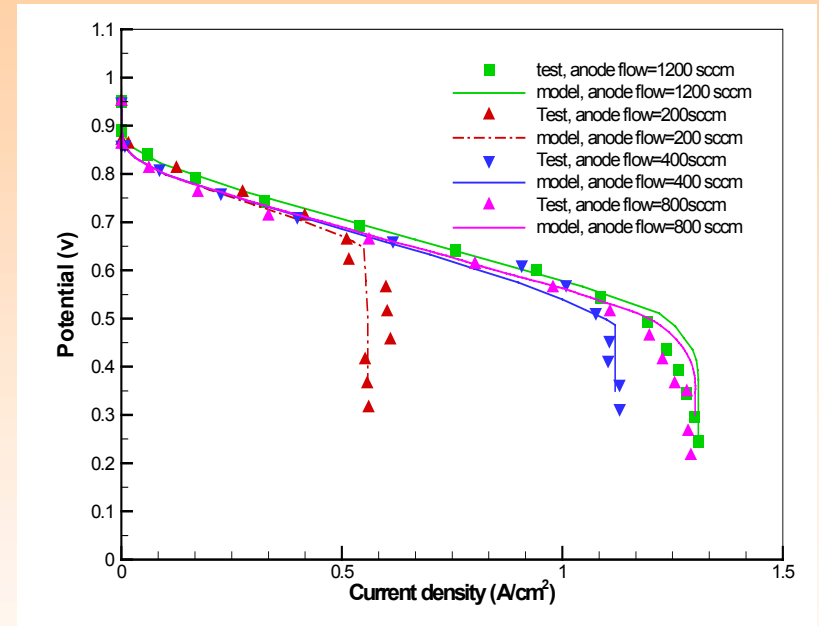
UM fuel cell test station



Comparison of 3D model with experiments

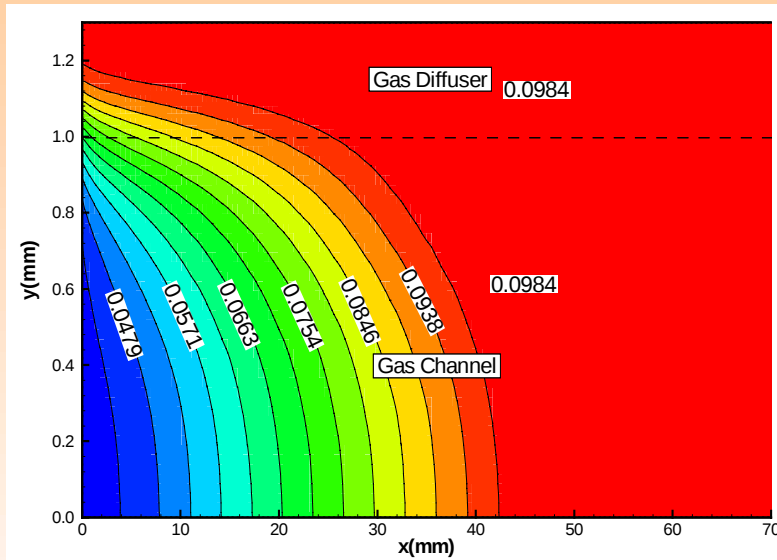


Different air flow rates

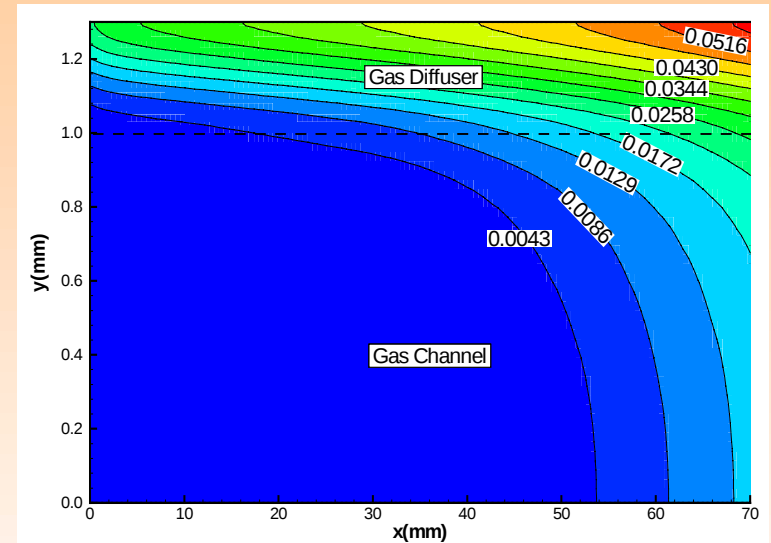


Different hydrogen flow rates

Sample results - 2-phase model

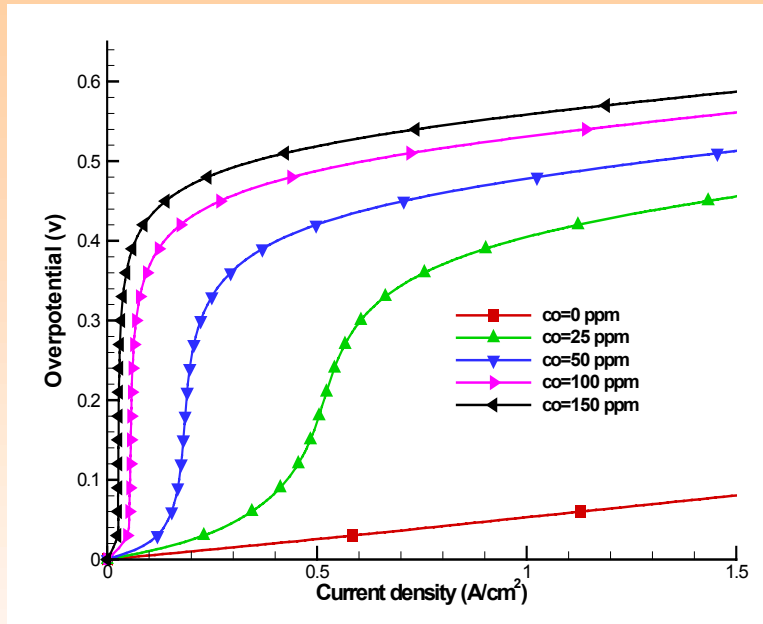


Vapor water fraction

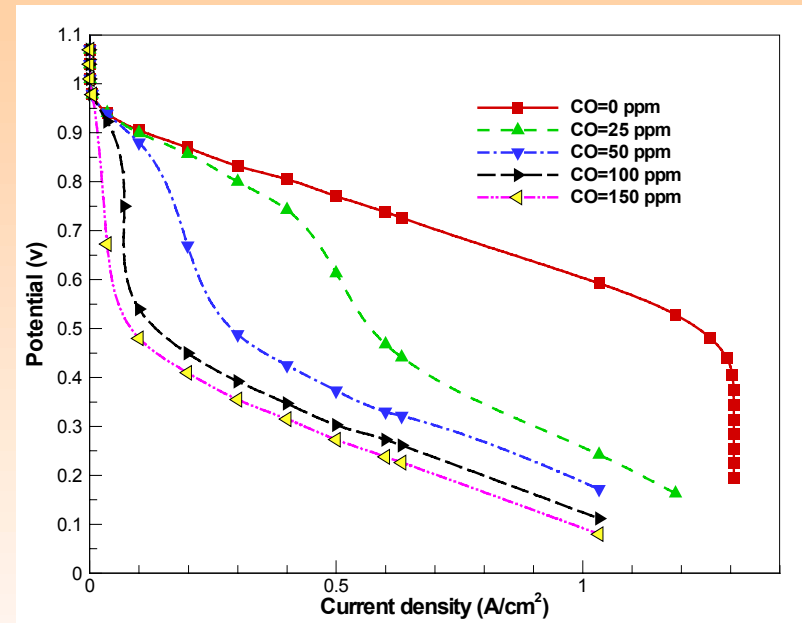


Liquid water fraction

Sample results 3D – reformat feed

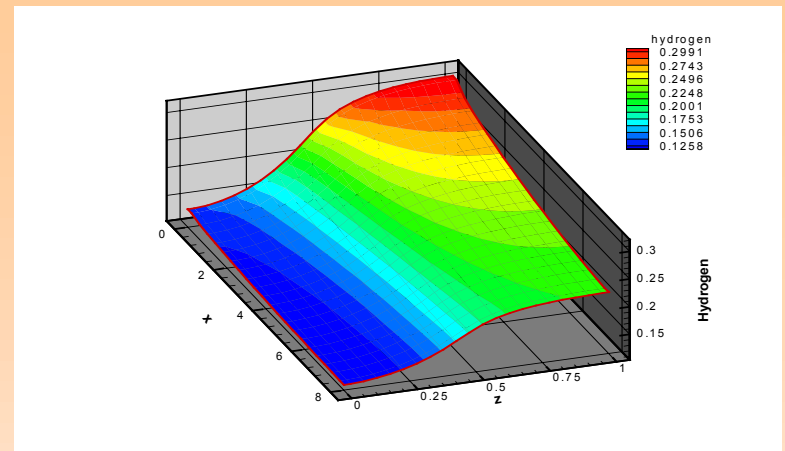
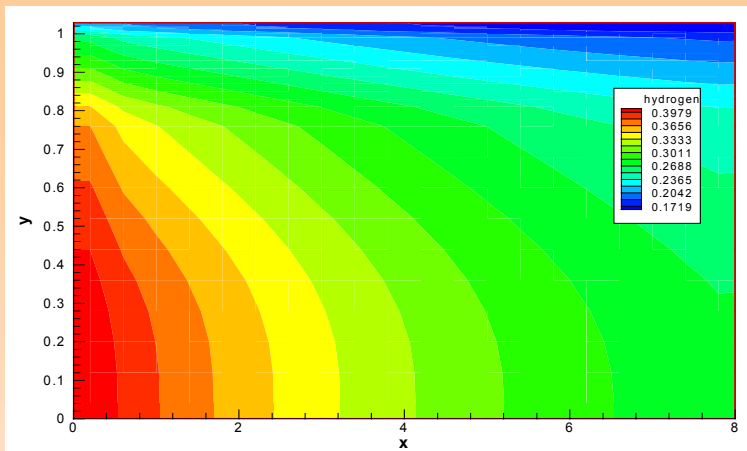


**Current densities
vs. overpotentials**

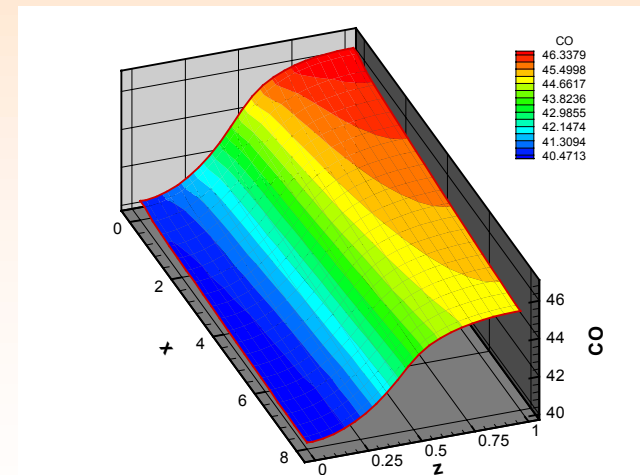
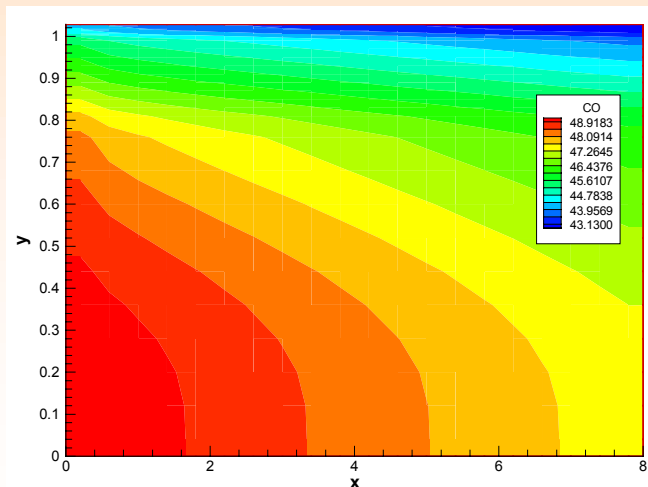


Polarization curves

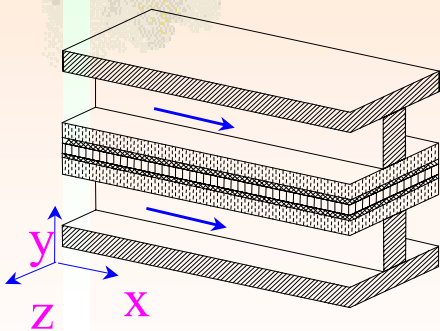
3D results – reformatate feed



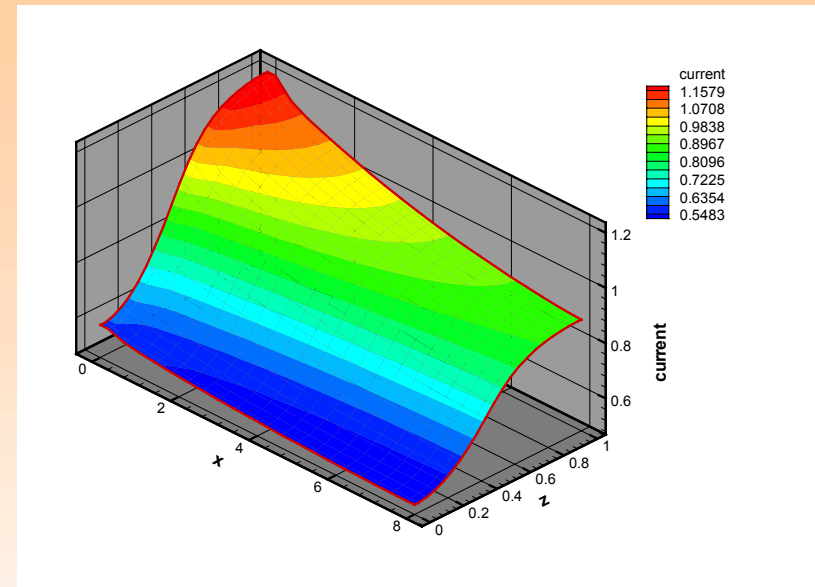
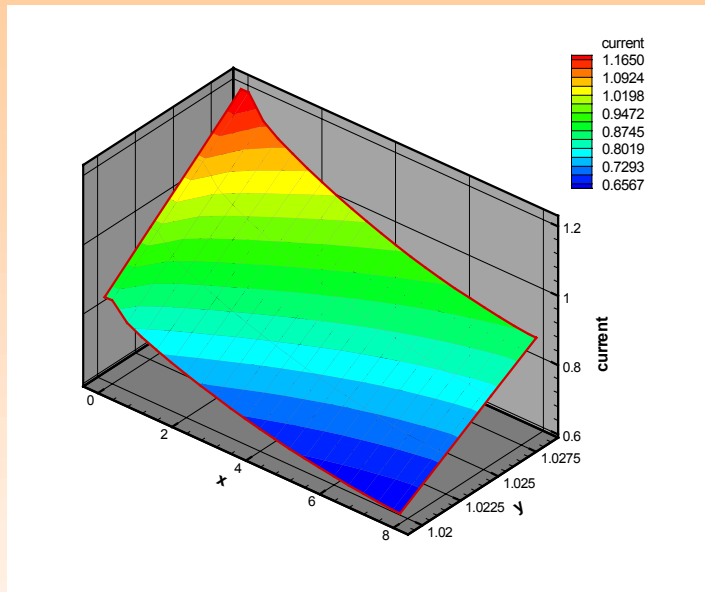
Hydrogen molar fraction at $i=0.7 \text{ A/cm}^2$



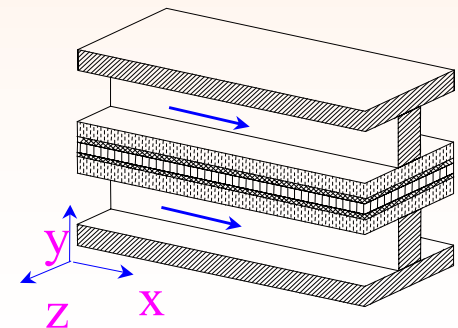
CO variation (ppm) at $i=0.7 \text{ A/cm}^2$



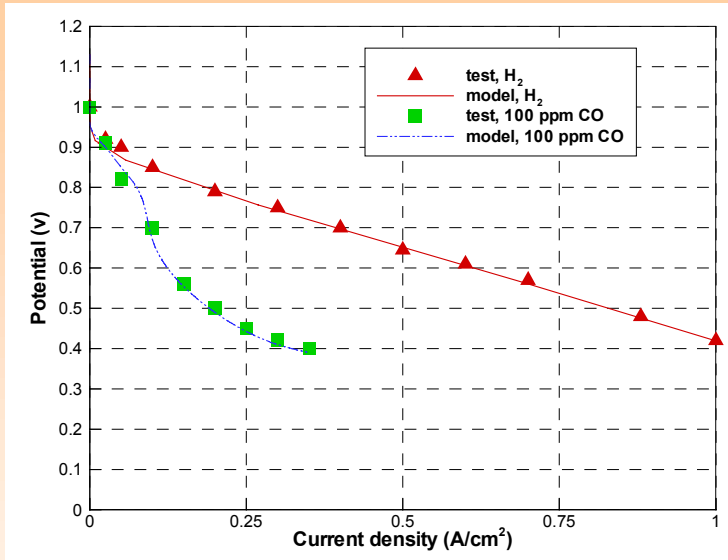
3D results – reformatate feed



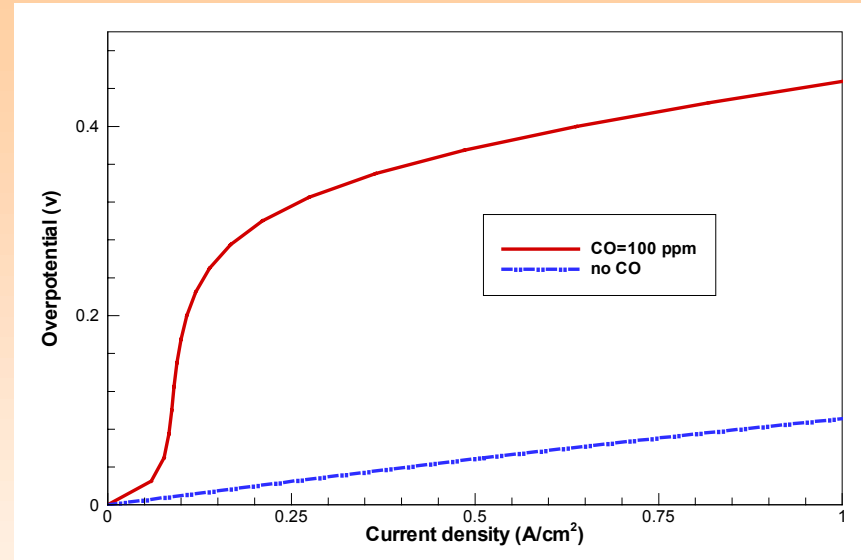
Local current density distributions



3D results – reformatate feed

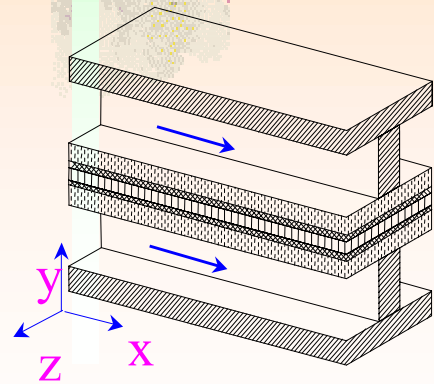
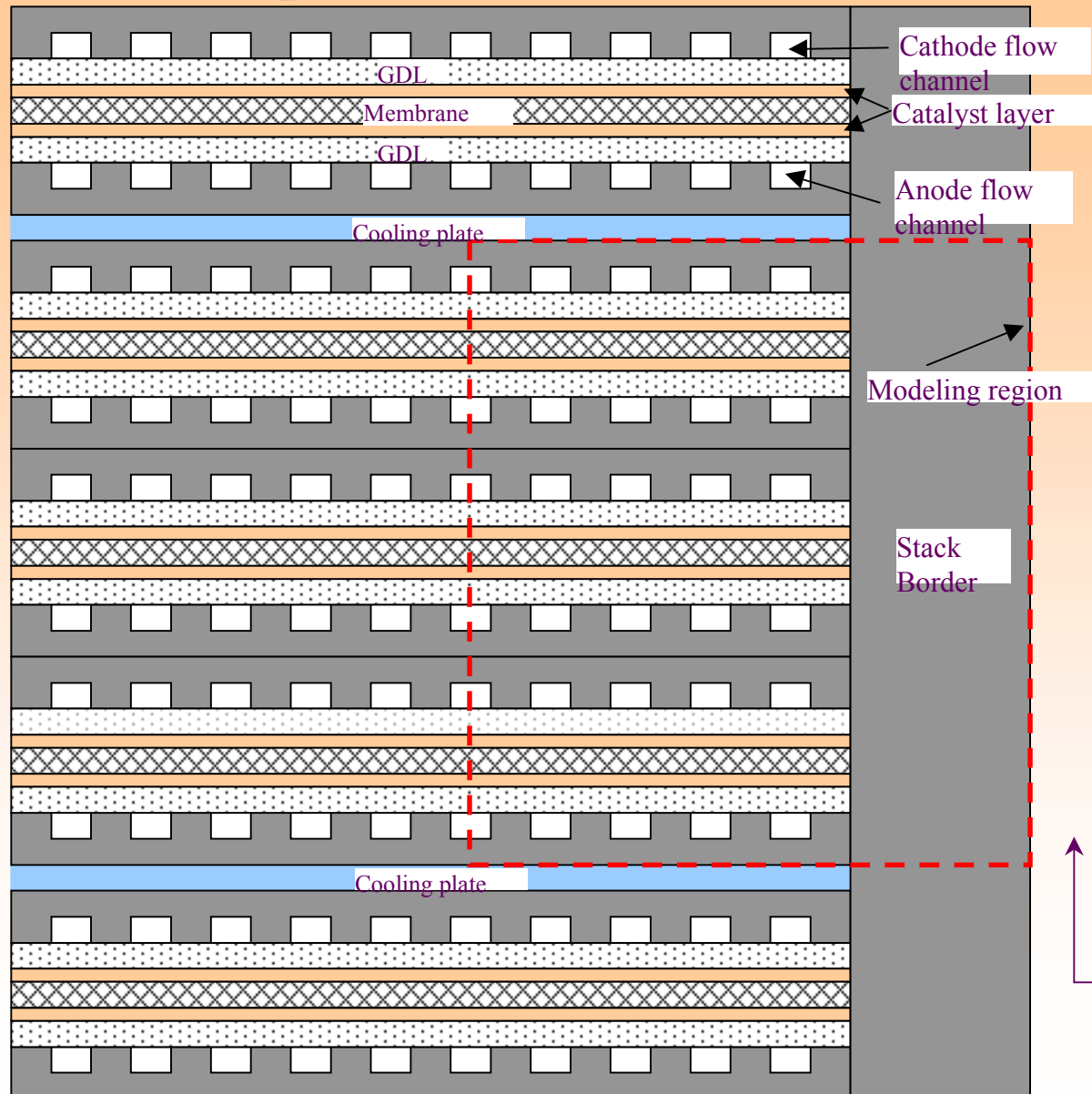


**Comparison with
experimental data**

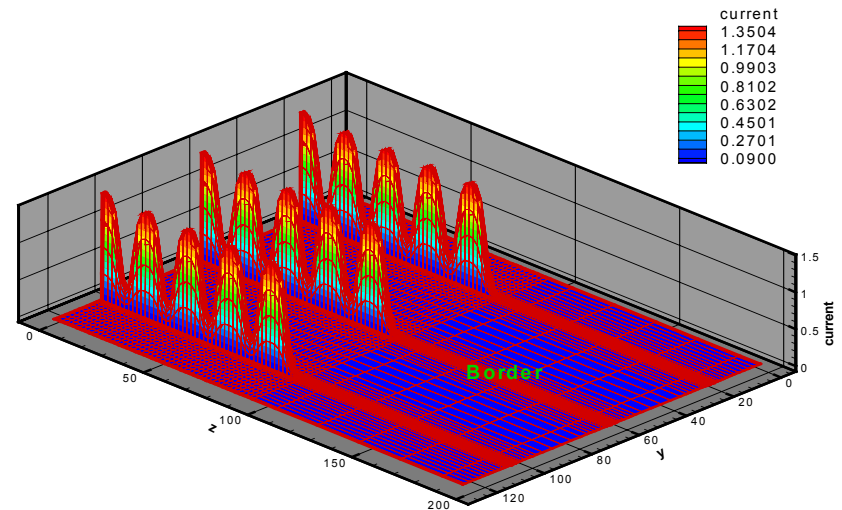
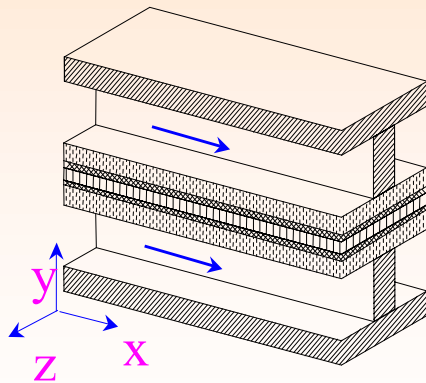
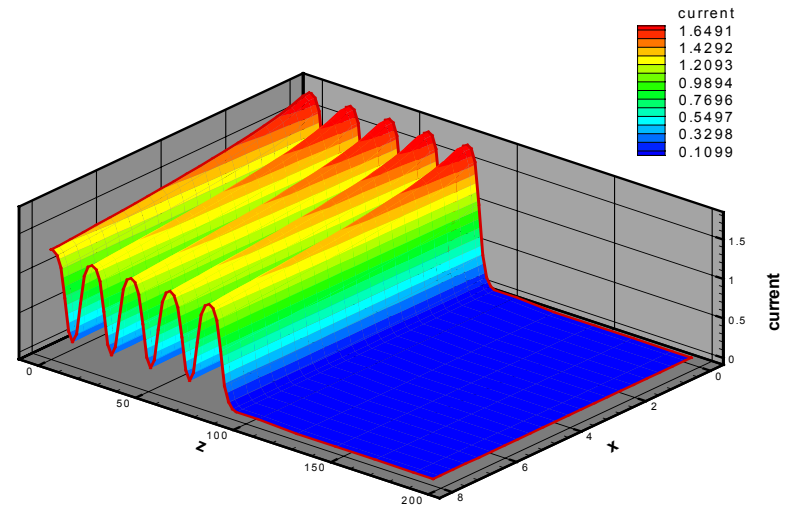
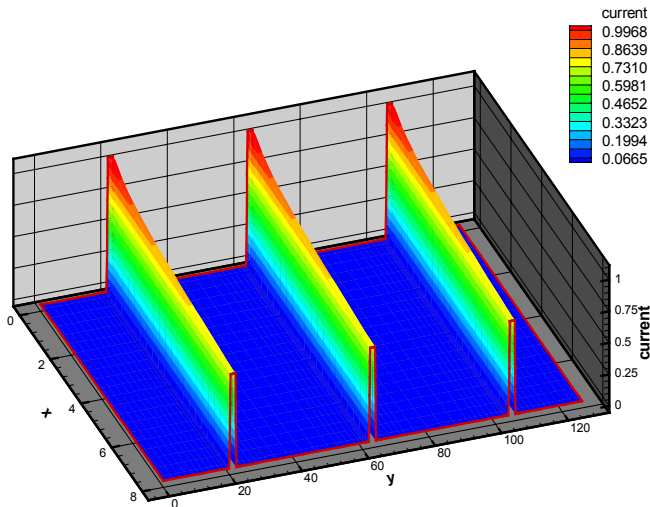


**Current density vs.
surface overpotential at
the anode**

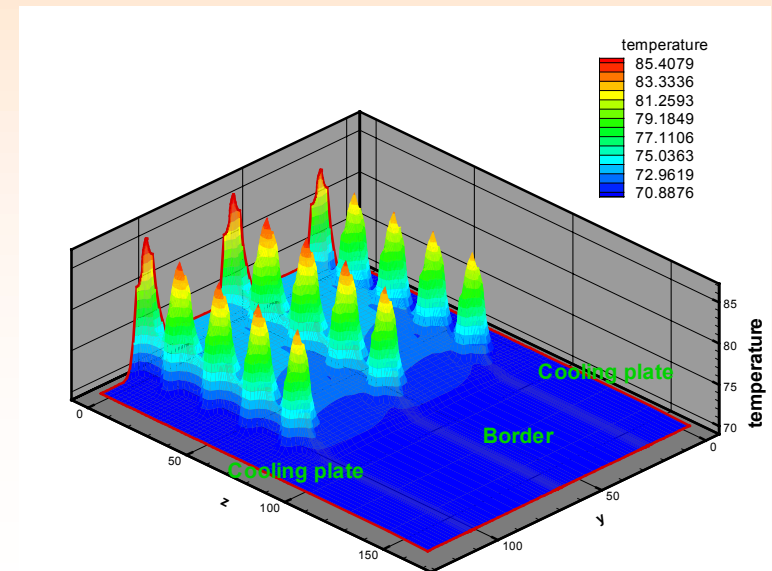
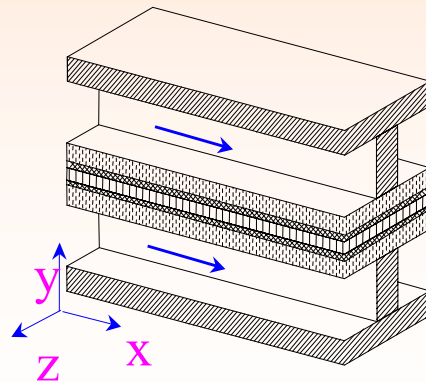
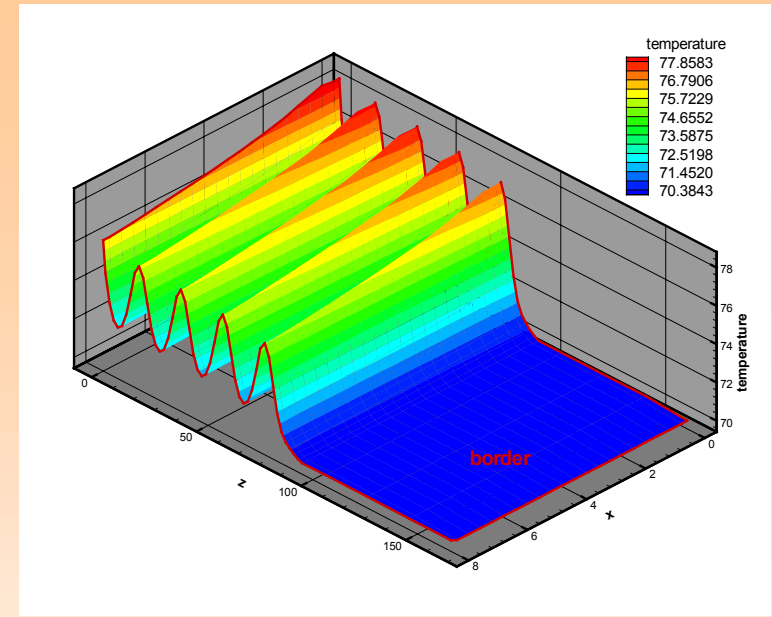
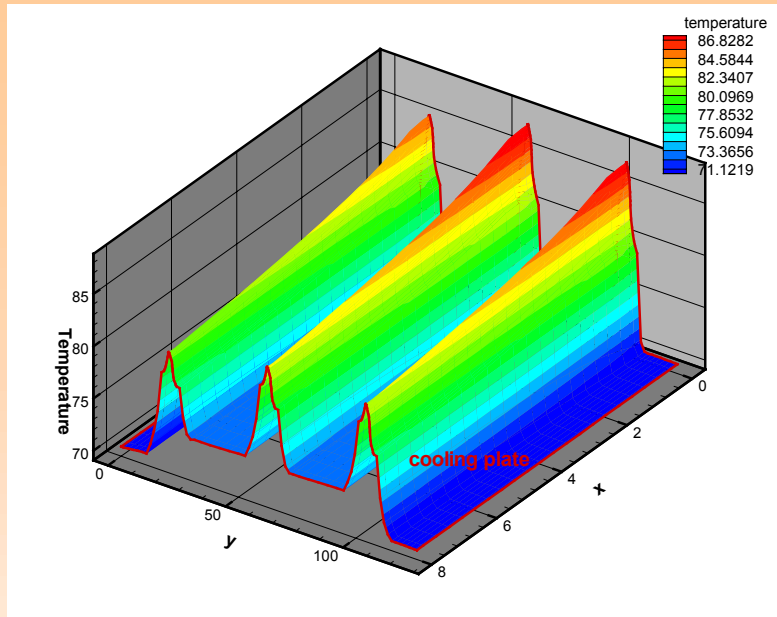
Preliminary stack model



Current density distributions



Temperature distributions



Summary and Highlights

- **The unified approach is successfully used in the 3-D model and partially in the two-phase model.**
- **Developed a fully functional “prototype”**
- **The models has been tested against experimental results (ours, in literature, and FC industry)**
- **The models are independent, no need of any CFD package**
- **7 journal papers published since 11/1998 (3 in FY02)**
- **14 conference papers published/presented**
- **2 journal and 3 conference papers accepted/submitted**

Major Publications

- *AIChE Journal*, pp. 2410 – 2422, Vol. 44, Nov. 1998.
- *Journal of Applied Electrochemistry*, pp. 1409 – 1416, Vol. 29, Dec. 1999.
- *Journal of The Electrochemical Society*, Vol. 147 (7), pp. 2468 – 2477, 2000.
- *Int. J. Hydrogen Energy*, Vol. 26, pp. 991-999, 2001.
- *Int. J. Transportation Phenomena*, Vol. 3, pp. 177 – 198, 2001.
- *Int. J. Heat Mass Transfer*, Vol. 45, pp. 2277 –2287, 2002.

Future Plans

- **Further development of the 3-D single-phase model: improve on reformat, different flow fields.**
- **Develop a 3-D two-phase model.**
- **Improve the a stack model.**
- **Couple the stack model with a system model.**
- **Extend the models to other type of fuel cells.**
- **Further interactions with industry and national labs.**