

# High Density Hydrogen Storage System Demonstration Using $\text{NaAlH}_4$ Complex Compound Hydrides

---

D. Mosher, X. Tang, S. Arsenault, B. Laube,  
M. Cao, R. Brown, S. Saitta, J. Costello

**United Technologies Research Center**  
East Hartford, Connecticut

Report to the  
U.S. Department of Energy (DOE)  
Contract Number: DE-FC36-02AL-67610

December 19, 2006\*

\* Presented to the DOE and the FreedomCAR & Fuel Partnership Hydrogen Storage Tech Team

This presentation does **not** contain proprietary or confidential information

# Overview

---

**Objective:** Identify and overcome the critical technical barriers in developing complex hydride based storage systems, especially those which *differ from conventional metal hydride systems*, to meet DOE system targets.

**Approach:** Design, fabricate and test a sequence of subscale and full scale prototypes involving material development such as safety assessment, catalysis and scaled-up processing.

Early systems development in parallel with novel materials research has been and will be important to hydrogen storage maturity.

## Current Systems Focus

- On-board rechargeable
- Based on  $\text{NaAlH}_4$  as representative complex hydride
- Generalize to materials which require moderate charging pressures

# Program Plan

- Safety Analysis
- Atomistic/Thermodynamic Modeling
- 50g H<sub>2</sub> Prototype System
- Media Kinetic Characterization & Modeling
- Heat/Mass Transfer Analysis
- High Temp. Composite Tank Development
- Component Fabrication
- Assembly System Fabrication
- Evaluation Facility Development
- 1kg H<sub>2</sub> CCHSS#1 Assembly
- CCHSS#1 Evaluation
- CCHSS#1 Model Validation
- CCHSS#2 System Design
  - *Advanced HX design*
  - *New media filling method*
  - *Compact manifold*
- Enhanced Media
  - *Advanced catalyst concepts*
  - *High volume synthesis method*
- CCHSS#2 Prototype
  - *Fabrication*
  - *Performance Testing*
  - *Model Validation*
- NaAlH<sub>4</sub> System Neutralization
  - *Process development*
  - *Prototype 1 decommissioning*
- New Materials
  - *Powder densification*

Program tasks nearing completion.

# Review of Prototypes

	LaNi <sub>5</sub>	NaAlH <sub>4</sub>
Charging pressure	10 bar	100 bar
Media volumetrics	50 kg H <sub>2</sub> / m <sup>3</sup>	25 kg H <sub>2</sub> / m <sup>3</sup> **
Powder loading	Controllable	Challenging
Expansion forces	High	< 7 bar, < 0.9 g/cc
Water reactivity	Low	High

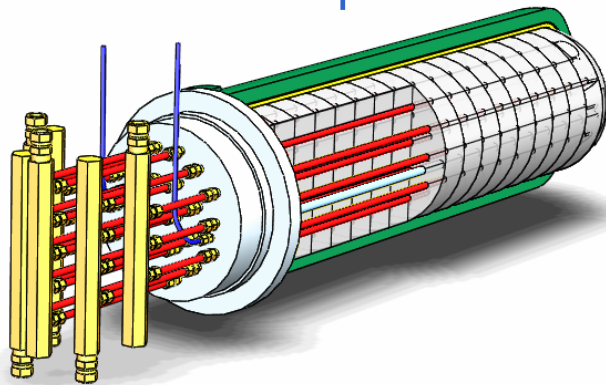
## System Element

- } Composite vessel
- } Powder densification
- Oil HT fluid

\*\* 50% powder relative density, 4% H<sub>2</sub> media capacity

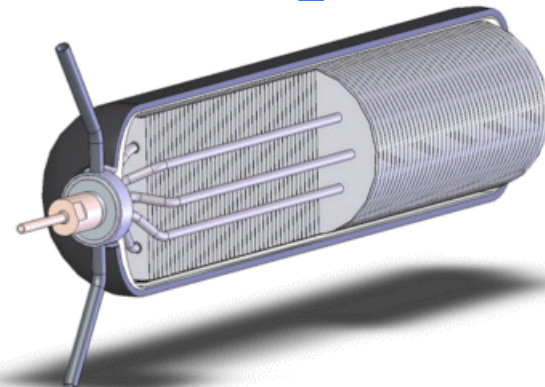
## NaAlH<sub>4</sub> Prototypes

1



Full scale – 19 kg hydride  
Aluminum foam

2



Sub scale – 3.5 kg hydride  
Aluminum fins

# Second Prototype Overview

---

## Improvements over first prototype:

- Lighter weight **composite vessel** with conventional domed end.
- Lighter weight **heat exchanger** with fins for superior long range heat transport.
- Denser **powder packing** which is performed within a pre-constructed system, improving both volumetrics and gravimetrics.

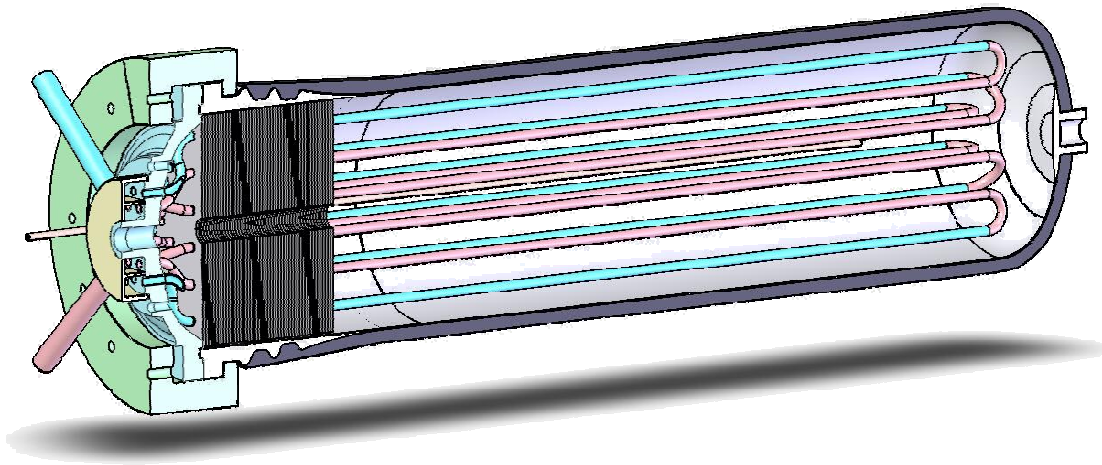
## Characteristics of second prototype

- Developed at nominally  $(1/2)^3 = 1/8^{\text{th}}$  **scale** or 1/8 kg H<sub>2</sub>.
- Intermediate size to balance:
  - Fabrication challenges – keep **unique supporting hardware** to reasonable size and cost.
  - Ability to demonstrate technologies and perform projections.

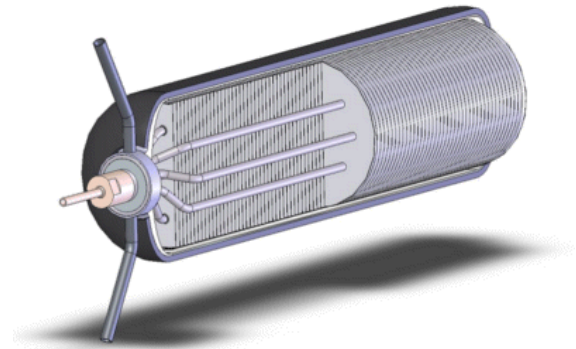
# Prototype 2 Size Scale Replan

Modifying the plan to design, fabricate and test a  $(1/2)^3 = 1/8^{\text{th}}$  scale system was the **right thing to do**.

- Greater emphasis of resources on powder densification and demonstration of lightweight, as-fabricated system.
- Lower degree of “projecting” to 2.3 wt% and 2.5 wt% systems.
- Recommend this size scale for first prototypes in future efforts.



**Original, full scale plan**  
nominally 25 kg of hydride



**Prototype 2**  
3.5 kg of hydride

# Prototype 2 Heat Exchanger Design

Fabricated heat exchanger based on the following design process:

Low Length Scale FEA

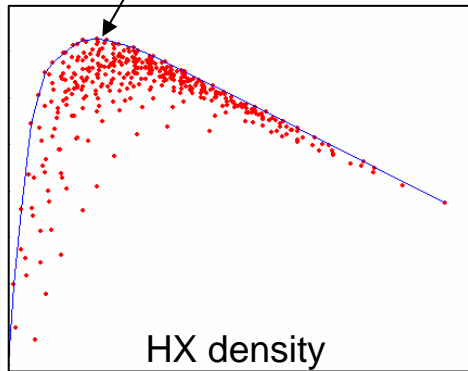
Fin unit cell



**Optimize:**

- Fin thickness
- Fin spacing
- Tubing OD
- Tubing spacing

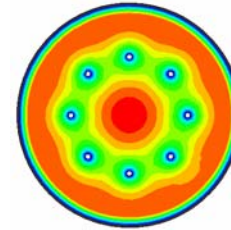
System H<sub>2</sub> capacity



HX density

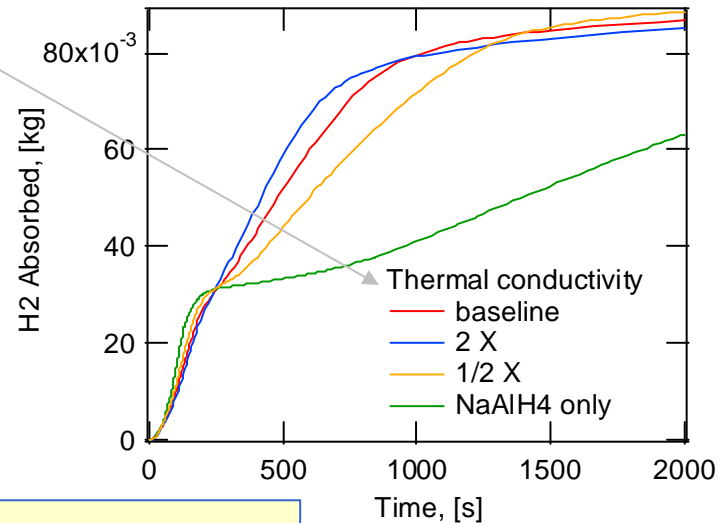
Larger Length Scale FEA

System cross section



**Optimize:**

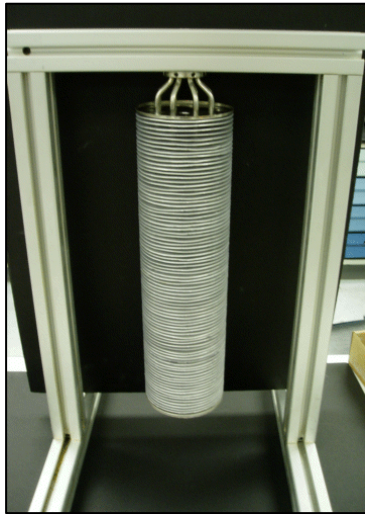
- Tubing positioning



30% reduction in HX mass

# Fabrication

Finned Tube  
Heat Exchanger



Stainless Steel Liner



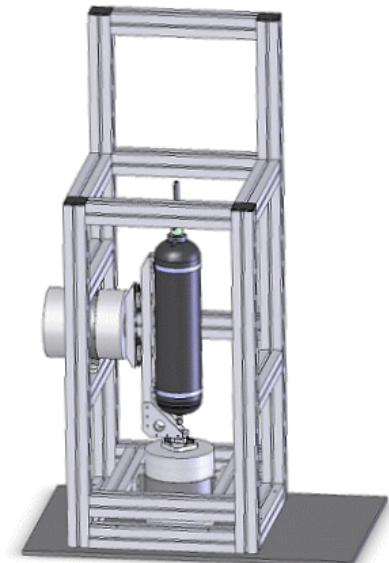
Carbon Fiber / Epoxy  
Overwrap



5' x 5' x 4' Assembly  
Glove Box



Shaker System





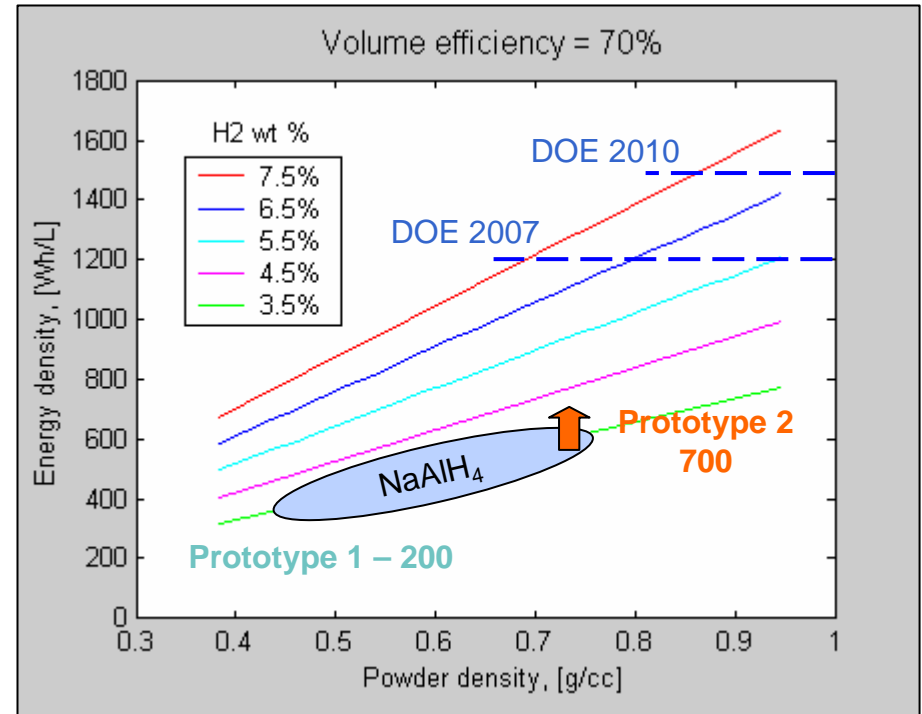
# Storage Volumetrics Overview

Energy density is the product of

- *Hydride powder density*
- $H_2$  weight % capacity
- System volumetric efficiency

Prototype improvement

- Prototype 1: 200 Wh / L
- Prototype 2: 700 Wh / L

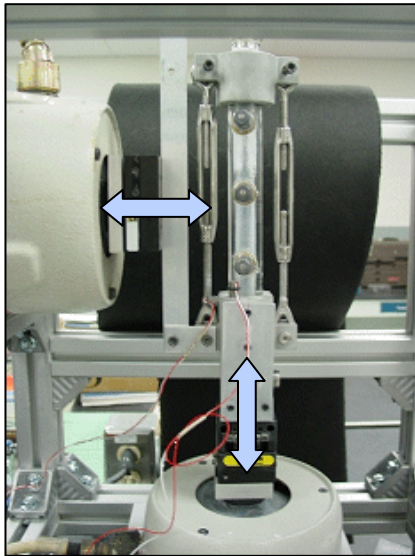


Hydride powder density is as important as  $H_2$  weight % capacity for system volumetric capacity

# Powder Loading – Procedure Development

## Development of loading procedure

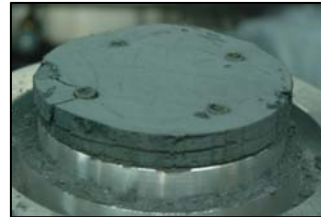
Results for second prototype hydride powder



Dual axis vibratory shaker  
Controlled amplitudes and  
frequencies



Powder column  
 $0.72 \pm 0.02$  g/cc



Disassembled finned  
test article  
 $> 0.77$  g/cc



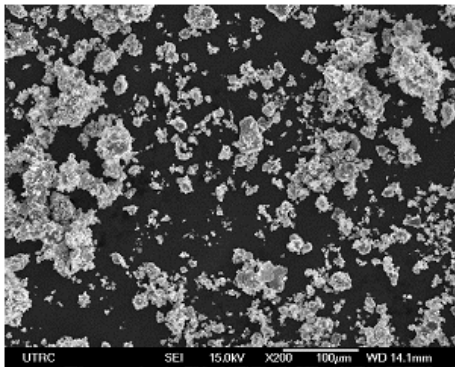
Prototype 2  
 $0.72$  to  $0.76$  g/cc  
Prototype 1  
 $0.44$  g/cc

Consistent densities across multiple configurations & geometries

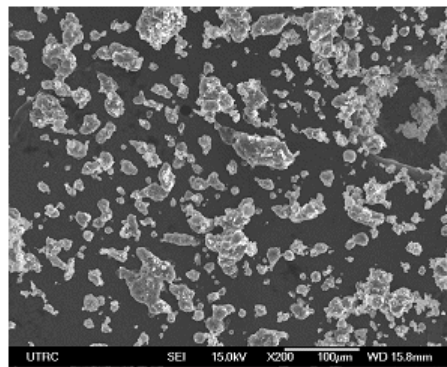
# Milling and Densification (Powder Column)

Ball milling procedures affect not only kinetics, but also powder densification.

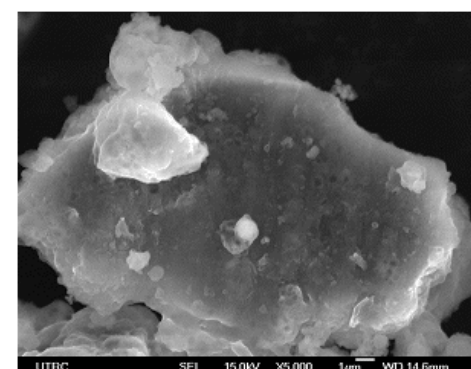
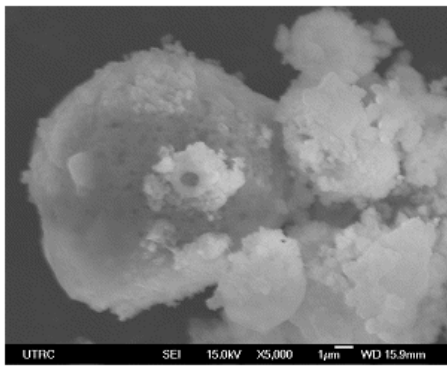
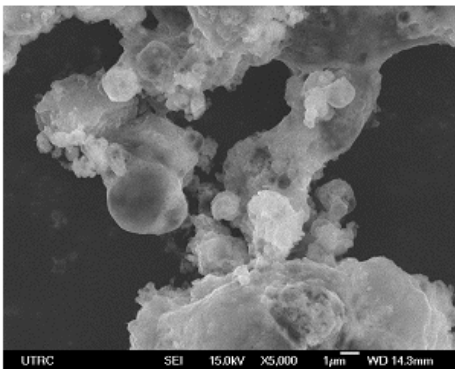
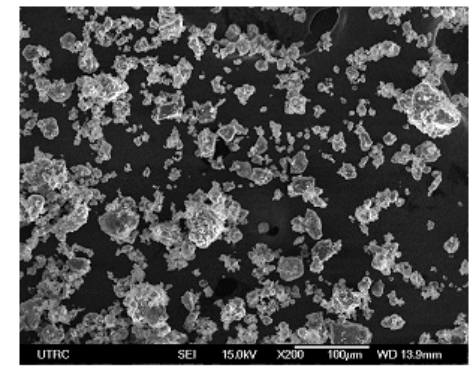
0.64 g/cc



0.85 g/cc



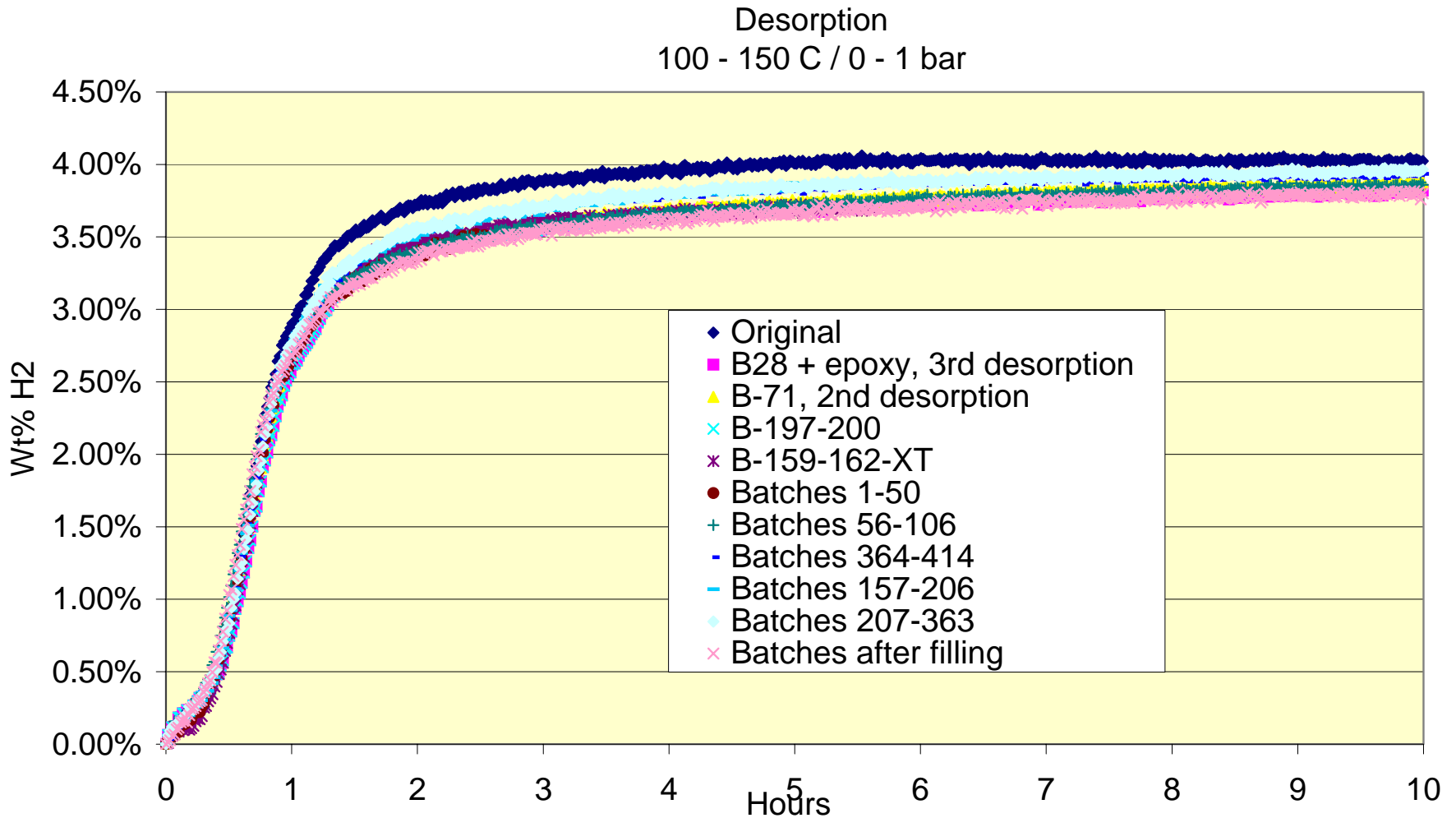
0.72 g/cc



Used for projection

Prototype 2 material

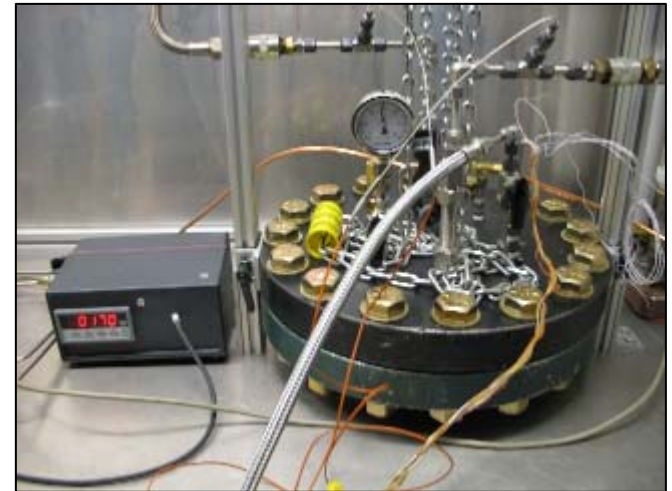
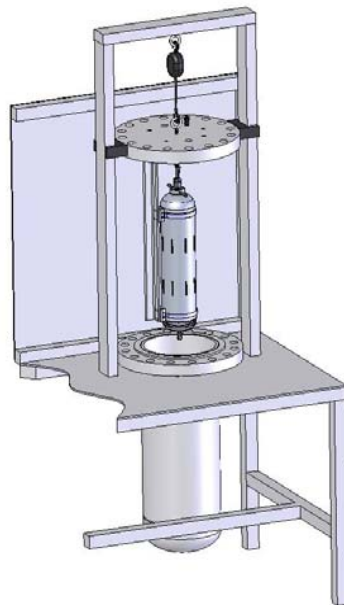
# Material Quality Assurance – Batch Testing



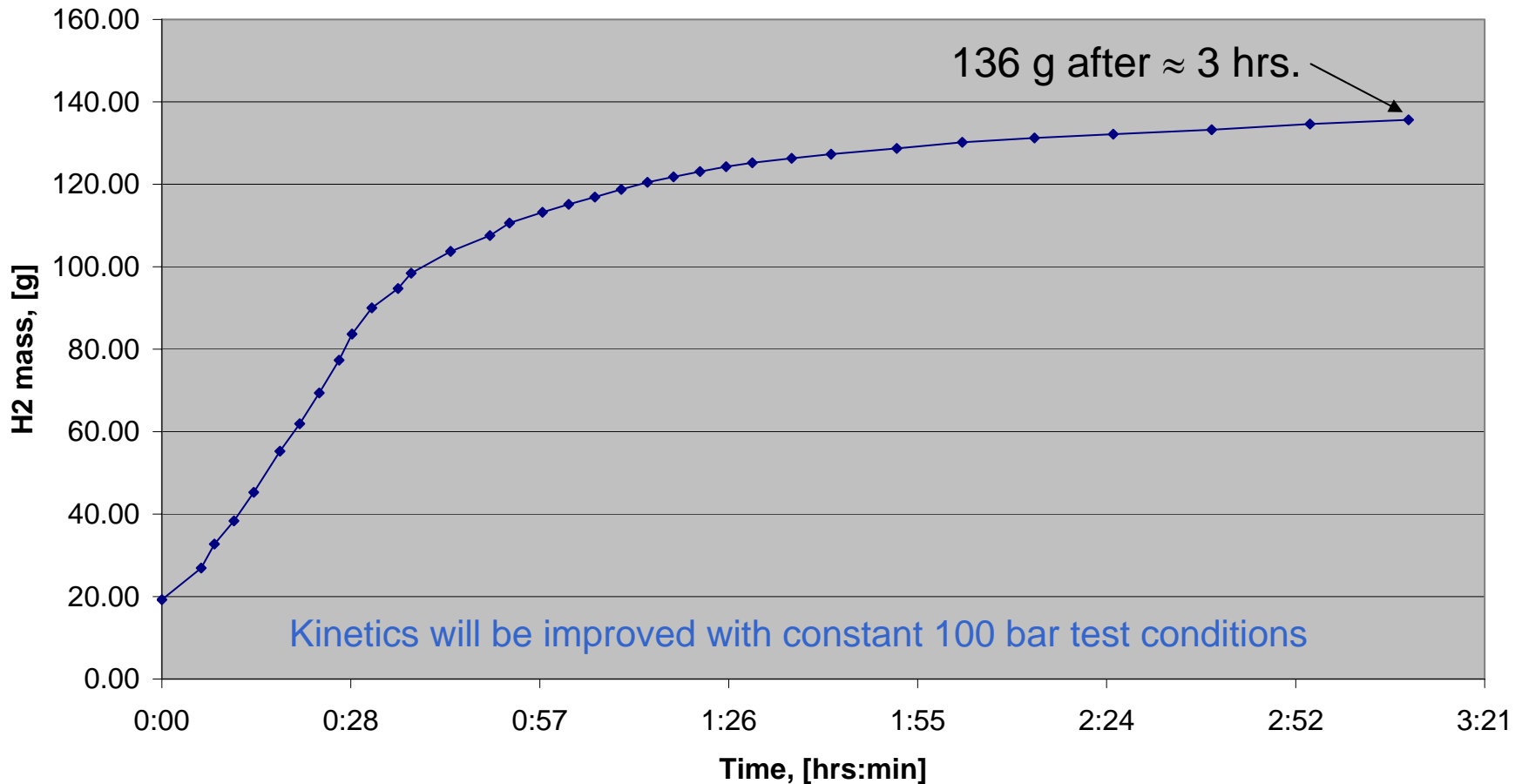
At desorption temperatures ramping from 100 to 150 C,  
capacity is nominally 3.5 to 3.7 wt%

# Prototype 2 Testing Apparatus

- Addition of secondary vessel for risk reduction
- First test – modified Sievert's apparatus approach with 100 bar dosing



# Absorption Test

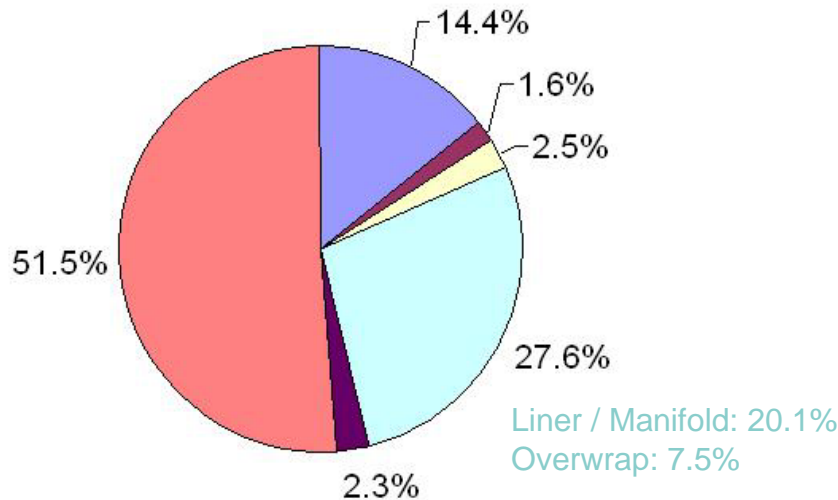


- Hydrogen was added to the prototype in doses from an accumulator volume.
- System charging pressure is reduced from its starting value of  $\approx 100$  bar after dosing.
- The first point includes both compressed gas and absorbed hydrogen storage.
- Desorption: 150 C &  $\approx 1$  atm.

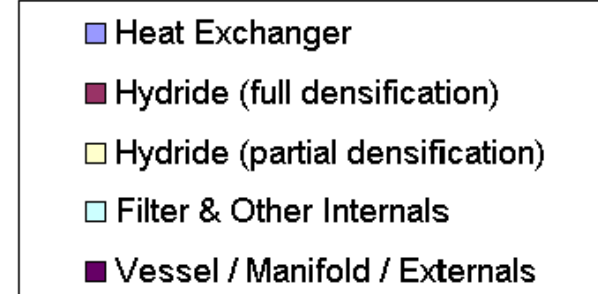
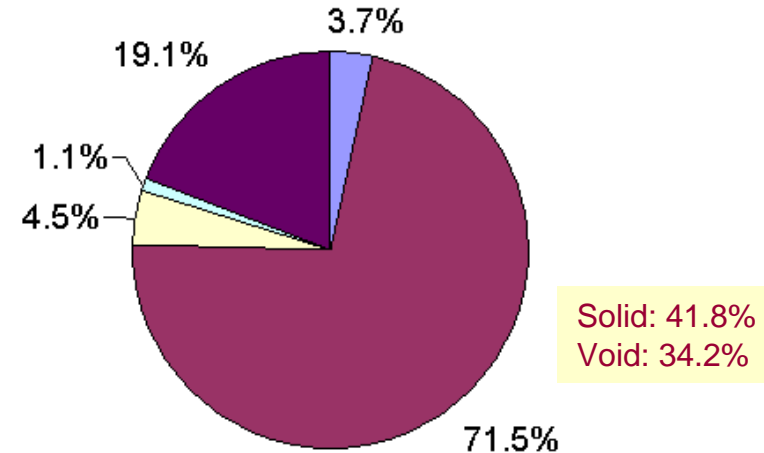
# Weight and Volume

- Hydride material: 3.5 kg, 0.72 g/cc
- Gravimetric capacity =  $136 / 6846 = 0.020$  (g H<sub>2</sub> / g System)
- Volumetric capacity =  $136 / 6450 = 0.021$  (g / cc)

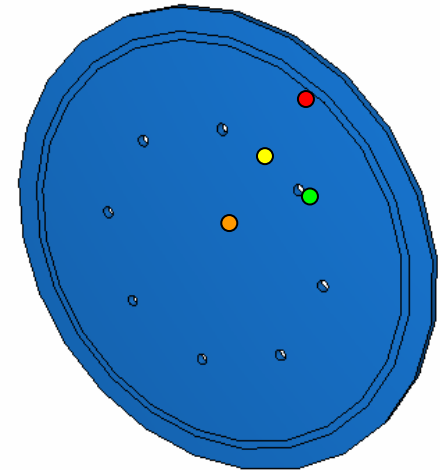
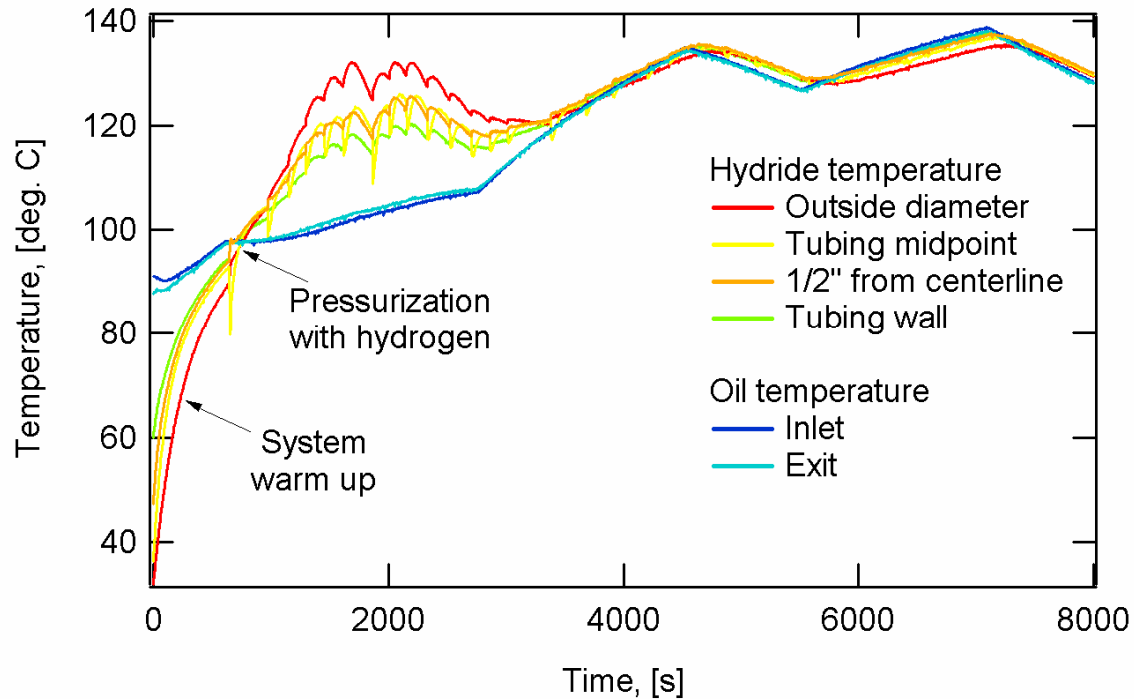
Weight




Volume



# Absorption Test – Temperatures



- Four internal thermocouples located at  $\frac{1}{4}$  length and as given in the figure.
- Sheathed type K with 0.032" diameter– some averaging → 
- Apparent exothermic reaction for slightly less than 1 hr.
- Pressure data only at dosing points, not continuous.
- Detailed model comparisons will be made with subsequent data.



# Testing Status

## Modifications and Issues:

- Improvements in oil temperature management.
- Significant noise in pressure transducer data was reduced.
- Addition of [Coriolis force flow meter](#) – will use burst flow to improve accuracy.
- After being dormant for almost 2 months, a [leak has occurred](#):
  - Pressurization to 1420 psi was normal, 1510 psi resulted in rapid leak rate.
  - Due to possible ejection of powder into secondary containment vessel, our [neutralization process](#) was applied before removing the lid. Upon opening secondary vessel, no ejected powder was noted.
  - The system was leaked check with helium and the source confirmed to be the O-ring. A metal-to-metal seal was used to keep the Viton O-ring from being exposed to hydride which did not perform as expected. A [Kalrez O-ring](#) is now being installed.



# System Scaling and Projection







## Elements of preliminary projection:

- Potential hydride mass =  $0.85 \text{ g/cc} * 4900 \text{ cc} = 4165 \text{ g}$  for subscale
- Scaling vessel to **full size** (10X)
  - Liner retains 0.020" thickness; liner mass scales as  $(\text{Volume})^{(2/3)}$
  - Hydrogen valve has the same mass
- Resulting full scale gravimetric efficiency is 0.63 (kg hydride / kg system)
- At 0.85 g/cc, 140 C and 100 bar, the compressed gas storage is effectively 0.25 wt% (kg H<sub>2</sub> gas / kg hydride).
- With a **3.4 wt% material**, system would be
$$(3.4\% + 0.25\%) * 0.63 = 2.3\%$$

All of these projection elements have been demonstrated separately, substantiating that such a 2.3 wt% system could be constructed with the currently developed technology.

# Performance Metrics and Projections

## Complex Compound Hydride Storage System (CCHSS) Performance Metrics

Material & Version:		NaAlH <sub>4</sub> Prototype 2	NaAlH <sub>4</sub> Projected	TBD hydride	TBD hydride	DOE Targets	
Characteristics & Metrics	Units					2007	2010
Material gravimetric capacity	% kg H <sub>2</sub> / kg hydride	3.4%	3.4% 	6.5% 	8.0%		
H <sub>2</sub> charging pressure	bar	100	100	70	50		
Packed powder density	kg hydride / m <sup>3</sup> powder	720 	850	800	850		
Material volumetric capacity	kg H <sub>2</sub> / m <sup>3</sup> powder	24	29	52	68		
System gravimetric efficiency	kg hydride / kg system	0.515 	0.63 	0.67 	0.75		
System volumetric efficiency	m <sup>3</sup> powder / m <sup>3</sup> system	0.76	0.76	0.7	0.7		
Normalized compressed gas	% kg H <sub>2</sub> gas / kg hydride	0.5%	0.3%	0.3%	0.2%		
System gravimetric capacity	% kg H <sub>2</sub> / kg system	<b>2.0%</b>	<b>2.3%</b>	<b>4.5%</b>	<b>6.1%</b>	<b>4.5%</b>	<b>6.0%</b>
	kWh / kg	<i>0.66</i>	<i>0.8</i>	<i>1.5</i>	<i>2.0</i>	<i>1.5</i>	<i>2.0</i>
System volumetric capacity	kg H <sub>2</sub> /m <sup>3</sup>	<b>21.1</b>	<b>24.0</b>	<b>37.8</b>	<b>48.6</b>	<b>36</b>	<b>45</b>
	kWh / L	<i>0.70</i>	<i>0.80</i>	<i>1.26</i>	<i>1.62</i>	<i>1.2</i>	<i>1.5</i>

 Notes

a: Improved catalysts & processing

b: Demonstrated powder packing enhancement

c: Improved densification & size scaling

d: Materials discovery

e: Reduction of charging pressure & vessel mass

Need 8 wt% material and 75% mass efficiency of system to meet 6 wt% system

# Evaluation of New Materials – System Integration

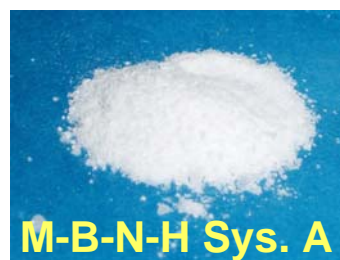
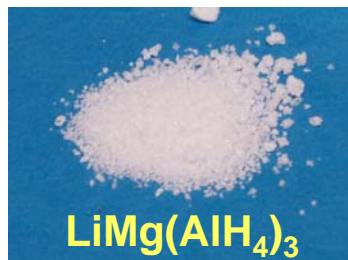
Compound	Theoretical Rev. H <sub>2</sub> wt fraction	Initial Density kg H <sub>2</sub> /liter	Vibratory Settling kg H <sub>2</sub> /liter	Enhanced Settling kg H <sub>2</sub> /liter
LiMg(AlH <sub>4</sub> ) <sub>3</sub> *	0.089	0.010	0.014	0.019
M-B-N-H System A *	0.088	0.033	0.041	0.042
M-B-N-H System B *	0.082	0.035	0.044	0.044
NaAlH <sub>4</sub> - best result **	0.056	0.026	0.041	0.042



Powder column densification rig

\* Densification of as-received new materials, with no further processing.

\*\* 6% TiF<sub>3</sub>-NaAlH<sub>4</sub>, dehydrided, and paint shaken, close to “as-received.”



Use of systems development methods to evaluate novel materials.

# Conclusions

Second prototype system development resulted in significant gravimetric and volumetric improvements:

		As-Fabricated		Projected	
Metric	Units	Prototype 1	Prototype 2	Prototype 1	Prototype 2
Gravimetric efficiency	<i>kg hyd. / kg sys.</i>	0.14	0.515	0.48	0.60 – 0.63
Gravimetric density	<i>% kg H2 / kg sys.</i>	0.4%	2.0%	1.7%	2.3%
Powder density	<i>g / cc</i>	0.44	0.72	0.60	0.85
Volumetric density	<i>kWh / L</i>	0.20	0.70	0.60	0.80