



#### **PEM Electrolysis R&D Webinar**

#### **May 23, 2011 Presented by Dr. Katherine Ayers**



### **Outline**

- •Key Messages About Electrolysis
- $\bullet$  Company Intro and Market Discussion
	- Electrolysis Technology Comparison
- Infrastructure Challenges and Solutions
	- System Approaches: Capacity and Delivery Pressure
	- Materials Advancements: Cost and Efficiency Improvements
- •Summary and Future Vision







## **Key Takeaways for Today**

- $\bullet$  Hydrogen markets exist today that can leverage advancements in on-site generation technologies
- $\bullet$  PEM electrolysis already highly cost competitive in these markets
- $\bullet$  PEM technology meets alkaline output capacities and has performance advantages for many applications
- $\bullet$  Multiple fueling stations utilizing hydrogen from electrolysis: can help bridge the infrastructure gap
- $\bullet$  Clear pathways exist for considerable cost reductions and efficiency improvements despite the maturity of the technology





### **Proton Energy Systems/Proton OnSite**

- • **Manufacturer of onsite gas generation products**
- • **Core competencies in Proton Exchange Membrane (PEM) technology**
- • **Founded in 1996 – changed name from Proton Energy Systems in April 2011.**
- •**ISO 9001:2008 registered**
- • **Product development, manufacturing & testing**
- •**Turnkey product installation**
- •**World-wide sales and service**
- • **Over 1,600 systems operating in 62 different countries.**



Cell Stacks



Complete Systems Storage Solutions RFC Integration



**Headquarters in Wallingford, CT**













## **Markets and Products**



**1999:** GC300-600 mL/min



**2003:**H-Series4-12 kg/day



**2006:StableFlow** Hydrogen **Control System** 



**2010:**Lab Line







## **Industrial Hydrogen Markets**

- Hydrogen is fastest growing industrial gas (7%/year)
- • Major industrial gas consuming industries:
	- Power Plants/Electric Power Generator Cooling
		- Over 16,000 hydrogen-cooled generators world-wide
		- Addressable market estimated at over \$2.0 billion
		- Improved plant efficiency and output/reduced greenhouse gas emissions
		- Payback typically less than one year
	- Semiconductor manufacturing
	- Flat panel computer and TV screens
	- Heat treating
	- Analytical chemistry (carrier gases for GC, etc.)







## **Typical Power Plant Implementation**



#### **Environmental Benefits: Pollution reduction**

- $\bullet$  1 ton of  $\mathsf{CO}_2$  for every MW/hr improvement
- $\bullet$  Based on improvement from 95% to 99%  $\mathsf{H}_2$  purity





## **Demonstrated Benefits of Distributed Hydrogen Production**

- $\bullet$  Cost competitive vs. delivered solution
	- Delivered cost can exceed \$15/kg for "remote" installations (>15 ft off major road)
- • Removes price fluctuation based on fossil fuel costs
	- Natural gas is major delivered source, delivered by diesel truck
- $\bullet$  Improves supply reliability
	- Removes delivery logistics, need for inventory tracking and ordering
	- Stack durability of over 50,000 hours demonstrated
- • Improves safety due to automation and inventory reduction
	- Eliminates delivery and change outs of bottles or trucks
	- Reduces inventory by orders of magnitude vs. 12-pack or tube trailer





## **PEM vs. Alkaline Liquid Electrolysis**

- 1. Membrane technology enables high differential pressure
	- • Eliminates need for strict pressure controls and slow turndown
	- • Enables rapid changes in current for renewable integration: fast response time to current signal
	- • Enables low pressure oxygen for safety and lower cost
- 2. Non-corrosive electrolyte
- 3. Stack operates at 4-5X current density of alkaline systems
	- •Counteracts higher cost materials



ON SITE





## **System Efficiency Comparison**

 $\bullet$ NREL-Xcel Energy Wind2Hydrogen Project





Proton Energy **HOGEN 40RE (PEM)** 



HM-100

(Alkaline)

- Actual Measured Efficiency<sup>1</sup>
	- PEM 57%

39% Improvement

– Alkaline 41%

1K. Harrison, Hydrogen Works Conference, San Diego, CA, Feb 17-19, 2009





## **Hydrogen Infrastructure Challenges**

- $\bullet$  Ramp-up
	- Fuel production
	- Storage
	- Transportation
	- End-customer delivery
- Pace with parallel ramp-up of related vehicles
- Continuum of options
	- Large, centralized plants
	- Neighborhood / captive fueling stations
	- Home-based fueling





- Vehicle Fleets
- Buses
- Alternative Markets
	- Materials Handling
	- Military / Aerospace
	- Bikes/Motorbikes
	- Marine



### **PEM Electrolysis Role in Hydrogen Fueling**

- $\bullet$  Traditional fueling station concept: grow capacity with number of vehicles
	- Over 20 demonstrations worldwide at up to 13 kg/day
	- Next generation product opens up next larger fueling opportunities (up to 65 kg/day)
	- Fully packaged solutions developed with Air Products and Linde
- $\bullet$  Home fueling concept to bridge gap
	- Based on less production output but higher pressure
	- Developing neighborhood fueler at up to 2.2 kg/day
		- • Full electrochemical compression to 5000 psi or mechanical compression to 10,000 psi
- $\bullet$ Renewable-based hydrogen production viability for both





## **Proton System R&D Strategy: Leverage Commercial and Military Experience**

#### **Military Markets**

- •Submarine life support
- $\bullet$  Unmanned vehicles
	- UAV
	- UUV
- $\bullet$  Silent Camp
	- Back up power
- $\bullet$  Military fueling needs
	- Fork lifts
	- $-$  Light duty vehicles

#### **Commercial Markets**

- •**Industrial**
- •Vehicle fueling
- $\bullet$ Telecomm backup
- •Renewable energy storage





#### **Early Fueling Station Examples**







#### **Electrolysis System Development**

#### **Larger Capacity**







**13 kg/day 65 kg/day**

#### **Higher Pressure**















### **Next Generation Fueling: 65 kg/day**

- •5 times increase in hydrogen output at 1.5x foot print.
- •Uses stack platform developed for Navy with Hamilton Sundstrand.
- $\bullet$ Balance of plant funded by TARDEC, DOE, and internal funding
- $\bullet$ Increased power supply and drying efficiency
- $\bullet$ Now commercially available, first unit to AC Transit for bus fueling
- $\bullet$ Also relevant for industrial applications









#### **Proton Fueling Station**





#### *Greater than 10,000 miles / 300 H<sub>2</sub> fills to date*





#### **High Pressure: Neighborhood Fueling Prototype**



- • Electrochemical compression to 2400 psi, 2 kg/day
- 10,000 psi fueling capability
- $\bullet$  Qualified for GM vehicle fueling





## **Conceptual Design: Neighborhood Fueler Gen 2**

- Direct electrochemical compression and delivery at 5000 psi
- Currently performing on DOE Phase II SBIR to develop initial prototype











### **5000 psi System Development Progress**

- •Seal design verified at higher temperatures
- • System concept and prototype design completed, hazard analysis completed
- • Concept design of cell and stack components completed, prototypes on order









## **Current Stack Limitations**

- $\bullet$  Efficiency driven by:
	- Membrane resistance
	- Oxygen overpotential
- $\bullet$ Cost driven by:

32%

15%

**System** 

- –Membrane electrode assembly
- –Flow fields/separators





**Activation and Ohmic Overpotentials** 

#### **Established Stack Durability**



ON SITE

### **Technology Roadmaps**

- $\bullet$  Detailed product development pathways laid out internally
	- Balance of plant scale up
	- Cell stack cost and efficiency
	- Product improvements and introductions
- $\bullet$ Balanced portfolio of near and long term implementation
- $\bullet$ Executing on funded programs to address each area





#### **Membrane Resistance Reduction**

- $\bullet$  Standard materials, 25% reduced thickness
	- Internally funded, **implemented 2010**
- $\bullet$  Reinforced membranes, 60% reduced thickness
	- Internal and ONR funding
	- **Leverages W.L. Gore technology**
	- 1000 hours demonstrated, passed 300 cycle accelerated stress test (5-mil fails test)
	- Efficiency > 5-mil Nafion



- $\bullet$  New chemistries (hydrocarbon), 80% reduced thickness
	- NSF funded project, Phase I/II STTR
	- $-$  Reduced H $_{\rm 2}$  crossover, improved voltage at higher temp





#### **High Current Performance, 80** °**C**



![](_page_24_Picture_2.jpeg)

# **O2 Evolution Efficiency**

![](_page_25_Figure_1.jpeg)

#### Bimetallic blends, 50 mV demonstrated efficiency gain

High surface area/utilization, 60 mV demonstrated gain

- $\bullet$ Phase 1 SBIR results
- $\bullet$  Pursuing funding for continued efficiency gains and catalyst loading reductions

![](_page_25_Picture_6.jpeg)

![](_page_25_Picture_7.jpeg)

# **Resulting Efficiency Improvements**<br>Predicted and Measured Cell Potential vs Current Density

![](_page_26_Figure_2.jpeg)

![](_page_26_Picture_3.jpeg)

![](_page_26_Picture_4.jpeg)

## **2002-2011 Progress**

![](_page_27_Figure_1.jpeg)

Improvements have enabled double the current density at the same cell voltage over 3 design generations

![](_page_27_Picture_3.jpeg)

![](_page_27_Picture_4.jpeg)

#### **Noble metal reduction**

- • Optimize current production (25% reduction)
	- Internally funded, 25% reduction **implemented 2009**
- • Next generation process (50% cumulative reduction)
	- Cathode: internally funded, 66% reduction **fully qualified for production 2009**
	- Anode: DOE funded, 55% loading reduction feasibility **demonstrated 2010**
- • Alternate deposition techniques and engineered nanostructures (>90% cumulative reduction)
	- DOE + internal investment. 90% loading reduction **feasibility demonstrated 2010**
	- **Leverages 3M technology**
	- Separate test shows >1500 hours of continuous operation

![](_page_28_Figure_10.jpeg)

![](_page_28_Picture_11.jpeg)

## **Flow Field Cost Reduction**

#### ~\$1.5M DOE funding allocated to date

#### Traditional approaches, 25% savings

#### Implemented 2010 **Phase 1 Verification(160 amps, 435 psi, 50°C)** 2.2502.200 $\bullet$  Cell 1 2.150■Cell 2 2.100Voltage (V) **Voltage (V)** Cell 32.0502.0001.9501.9001.8501.8001.7500 1000 2000 3000 4000 5000 6000**Time (h)**

#### Alternate coating strategies, 30% cumulative savings

![](_page_29_Picture_5.jpeg)

 $Ti-10Zr$ Ti-10V-5Zr

![](_page_29_Picture_7.jpeg)

Ti

#### Unitized parts and low cost manufacturing method, 50% cumulative savings

![](_page_29_Figure_9.jpeg)

#### Laminate designs, 70% cumulative savings (enabled by coating development)

![](_page_29_Figure_11.jpeg)

![](_page_29_Picture_12.jpeg)

# **Cell Stack Cost Reductions**

![](_page_30_Figure_1.jpeg)

#### Noble Metal Reduction

![](_page_30_Figure_3.jpeg)

![](_page_30_Figure_4.jpeg)

![](_page_30_Picture_5.jpeg)

![](_page_30_Picture_7.jpeg)

## **0.6 ft2 Stack Development**

- • Improvement in bipolar plate design
	- –Current 0.1 ft<sup>2</sup> design tested to over 1 million cell hours
	- CFD modeling shows more uniform flow
- $\bullet$  Demonstrated operation up to 425 psi
	- >10,000 hours validated

![](_page_31_Figure_6.jpeg)

![](_page_31_Figure_7.jpeg)

![](_page_31_Picture_8.jpeg)

![](_page_31_Figure_9.jpeg)

![](_page_31_Picture_10.jpeg)

![](_page_31_Picture_11.jpeg)

#### **Next Steps: Scale Up**

- $\bullet$ Fully tested at 1-3 cell level
- TARDEC FY11 program: Scale up to 50 kg/day full size design point

![](_page_32_Picture_3.jpeg)

![](_page_32_Picture_4.jpeg)

![](_page_32_Picture_5.jpeg)

![](_page_32_Picture_6.jpeg)

#### **Impact of Scale Up on Balance of Plant Cost**

![](_page_33_Figure_1.jpeg)

![](_page_33_Picture_2.jpeg)

![](_page_33_Picture_3.jpeg)

### **Summary and Future**

- • Commercial products leveraging PEM electrolysis are growing in capacity and advancing in cost and efficiency
- $\bullet$  These products serve existing markets and can directly leverage investments in PEM fuel cell technology
- $\bullet$ PEM electrolysis can help to bridge the infrastructure gap and has already been demonstrated at relevant scale
	- Additional advantages in potential for zero carbon footprint
- • Cost/efficiency targets can be achieved through leveraging of existing science, without major new invention
- $\bullet$  Investment in electrolysis is key to move demonstrated cost and efficiency improvements from the lab to production

![](_page_34_Picture_7.jpeg)

![](_page_34_Picture_8.jpeg)

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