

# NOx Adsorber Regeneration Phenomena In Heavy Duty Applications

ORNL/ITEC CRADA

**Brian West**

**John Thomas, Mike Kass, John Storey, Sam Lewis**

**Oak Ridge National Laboratory**

## **Industrial Partners**

**Xinqun Gui, Shouxian Ren**

**Ken Price, Danan Dou**

**DELPHI**



**2003 Diesel Engine Emissions Reduction Workshop**

**August 24-28, 2003**

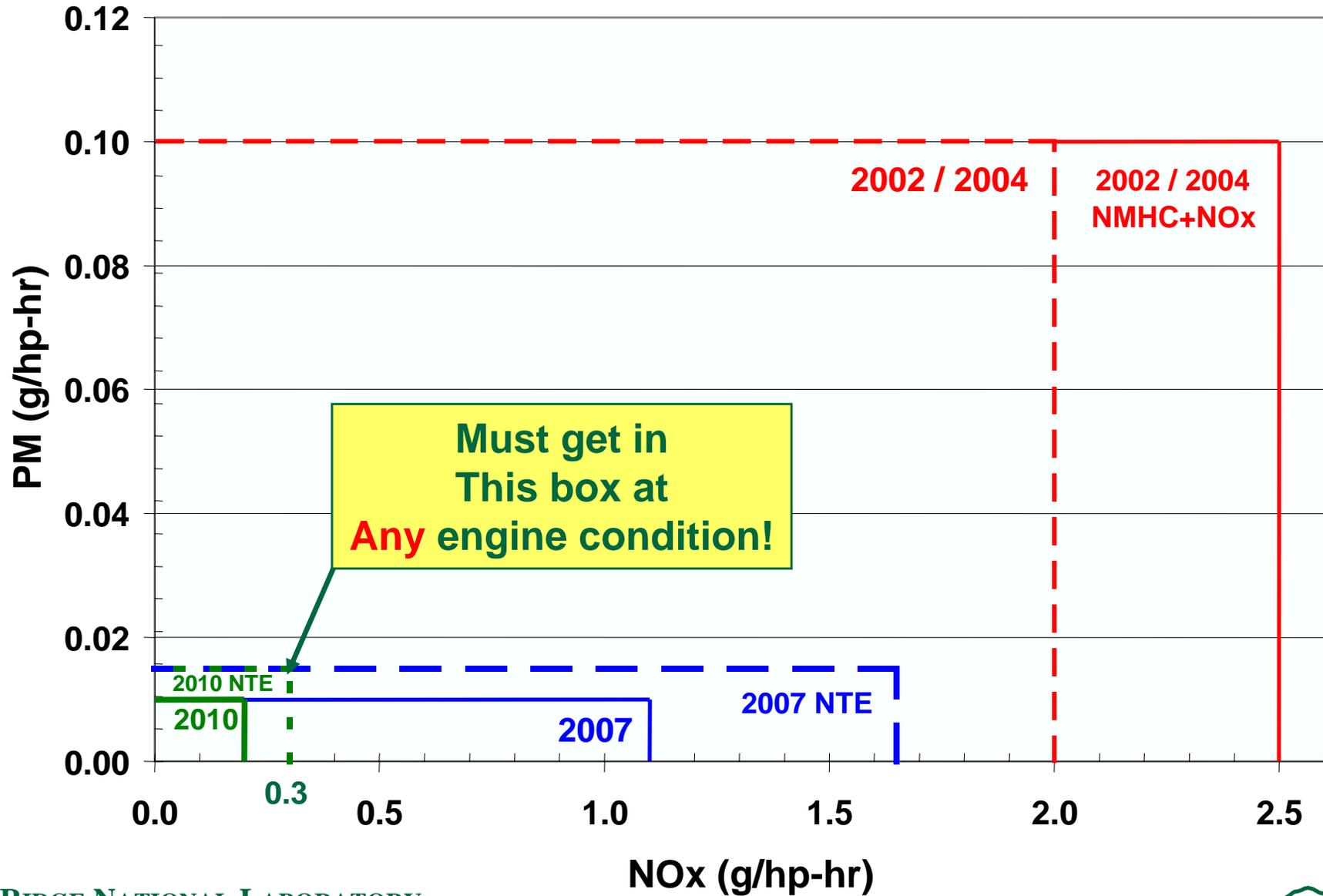
**Sponsor: U.S. Department of Energy, OFCVT**

**Team Leader: Gurpreet Singh**

**OAK RIDGE NATIONAL LABORATORY**  
**U. S. DEPARTMENT OF ENERGY**

The logo for UT-Battelle features a green silhouette of a mountain range above the text "UT-BATTELLE" in black capital letters, which is underlined.

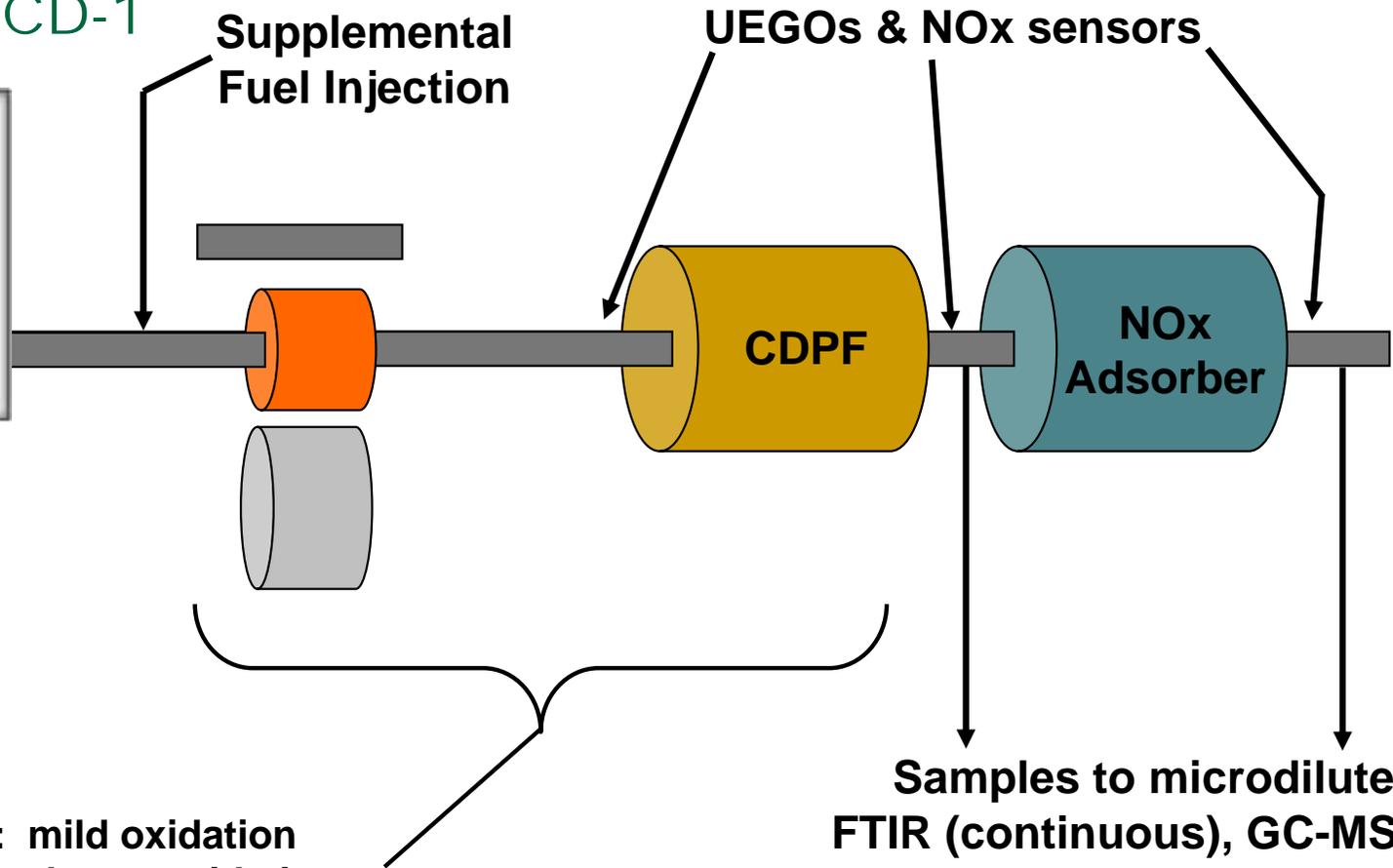
Impending HD standards call for drastic emissions reductions. NTE limits impose significant challenge



Diesel oxidation cats inserted downstream of injection site. CDPF and NOx adsorber in all experiments. Unless otherwise specified, test fuel is ECD-1



**T444E Engine**  
w/ Throttle, EGR



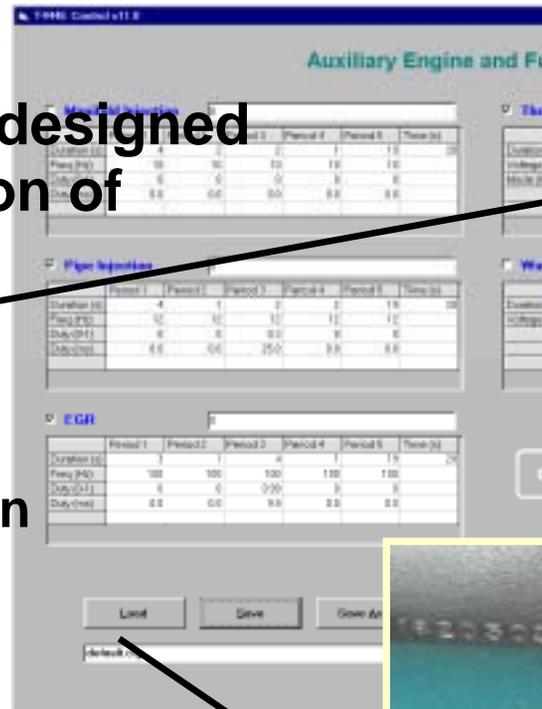
Straight Pipe + CDPF: mild oxidation  
2.5 L DOC + CDPF: moderate oxidation  
5 L DOC + CDPF: aggressive oxidation

Samples to microdiluter for  
FTIR (continuous), GC-MS (bags)

# ITEC T444E Engine modified to control aftertreatment system

## □ PC-based auxiliary controller designed and built for transient operation of

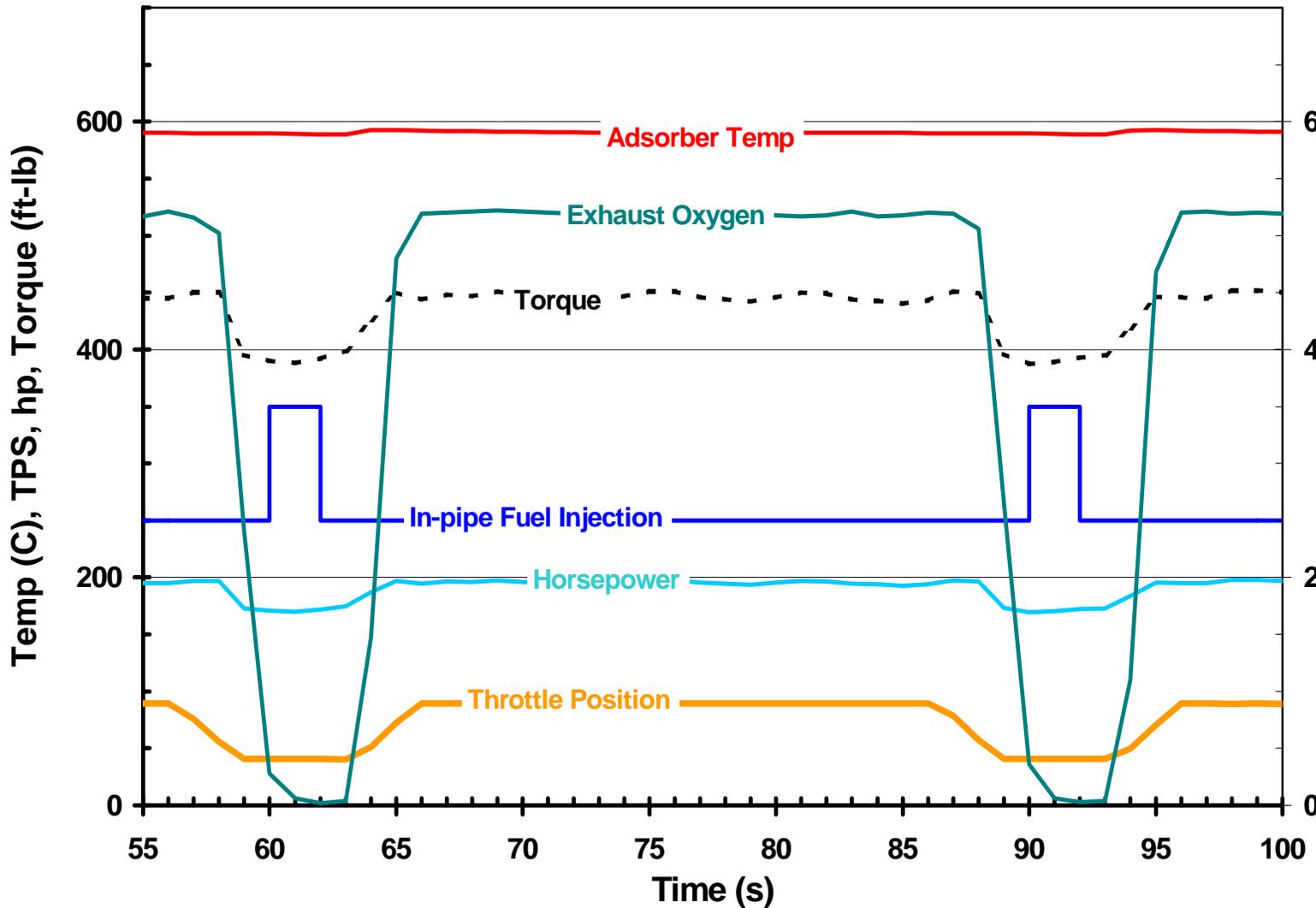
- Electronic throttle
- Electronic EGR valve
- Wastegate
- Post-combustion fuel injection
  - In-manifold (pre-turbo)
  - In-pipe (after turbo)



## □ Aftertreatment system includes diesel oxidation catalyst(s), catalyzed diesel particulate filter, and NOx adsorber



# Sample strategy for regeneration with in-pipe injection



2300 RPM, 450 ft-lb

Adsorber temperature 600C

30 s cycle time

2 s throttle ramp to 40%, hold 5 s

3 s rich pulse

No attempt to mitigate torque loss

Exhaust O2 %

All experiments used same NOx adsorber with CDPF upstream. CDPF augmented with DOCs

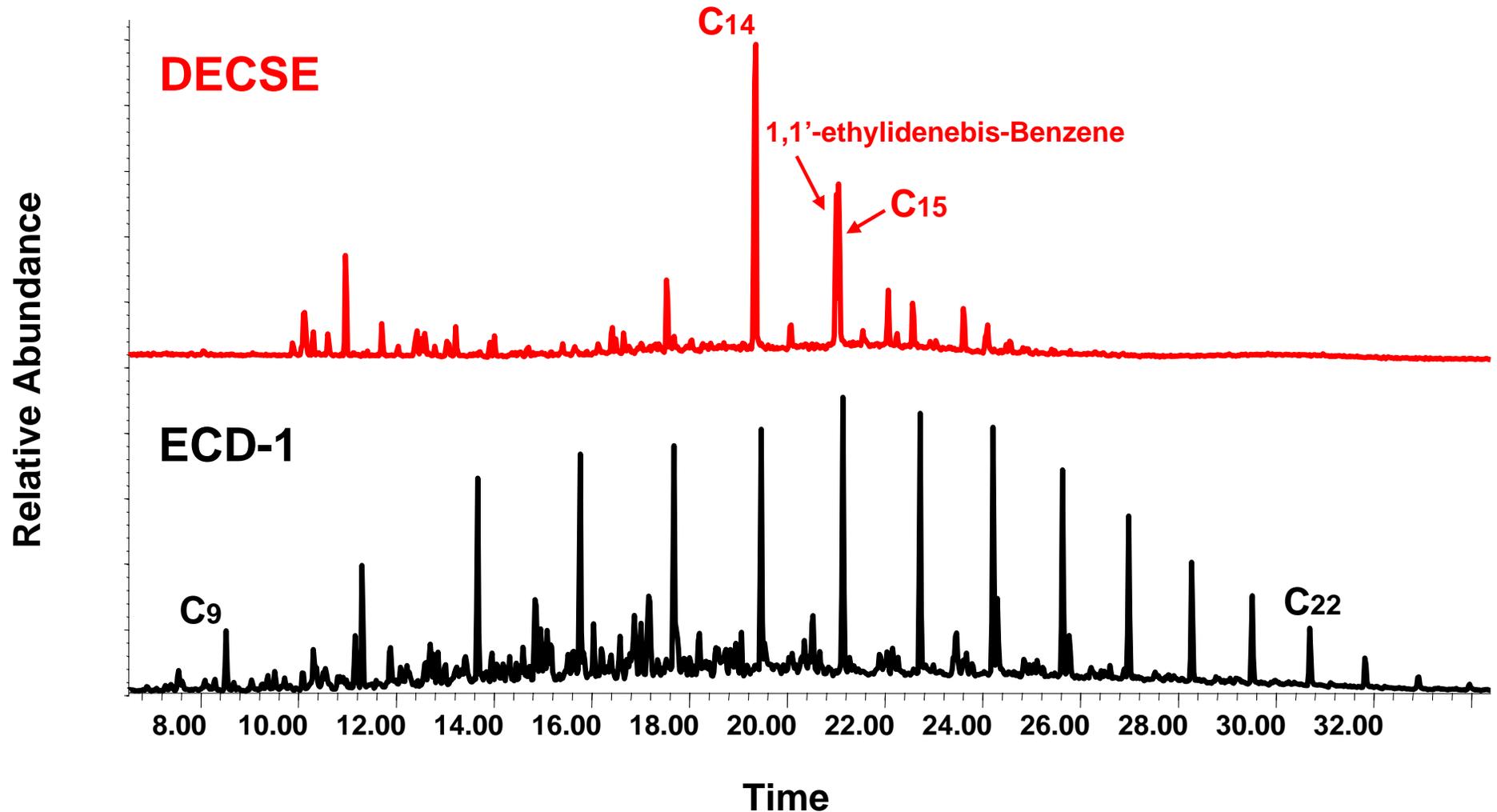
<b>Device</b>	<b>Volume (L)</b>	<b>Min SV (1000/hr) (Regen)</b>	<b>Max SV (1000/hr) (Lean operation)</b>	<b>PGM g/ft<sup>3</sup></b>
<b>Small DOC</b>	2.5	204	307	70
<b>Large DOC</b>	5	102	154	70
<b>CDPF (not Delphi part)</b>	15	34	51	75
<b>NOx Adsorber (Ba-K type)</b>	14	36	55	100

# Fuel used in this study is largely BP (Arco) ECD-1. Cursory look at DECSE

- **EPA's 2006 Diesel Fuel spec differs from today's only in sulfur level**
- **EPA and CARB certification fuel specs differ in aromatics (EPA >27; Cal <10) and cetane**
- **BP (Arco) ECD-1 "looks" like CARB fuel**
- **"DECSE" (Chevron Phillips ULS), BP15, and S-zorb™ "look" like 2006 EPA fuels**
  - **Aromatics, boiling range, sulfur**

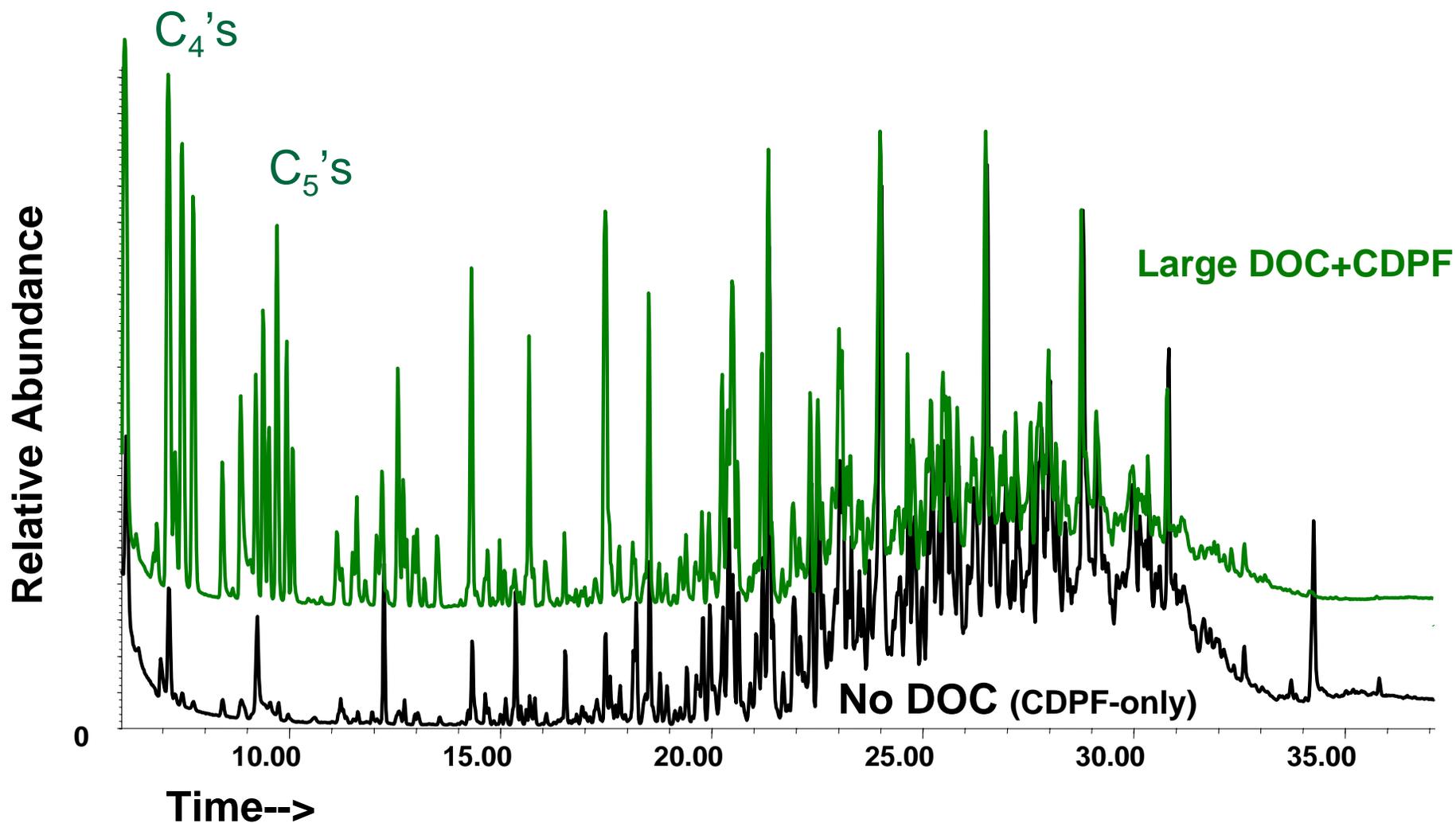
# DECSE fuel meets all specs, but contains narrow range of HCs

Chromatogram shows individual compounds in DECSE and ECD-1 fuel



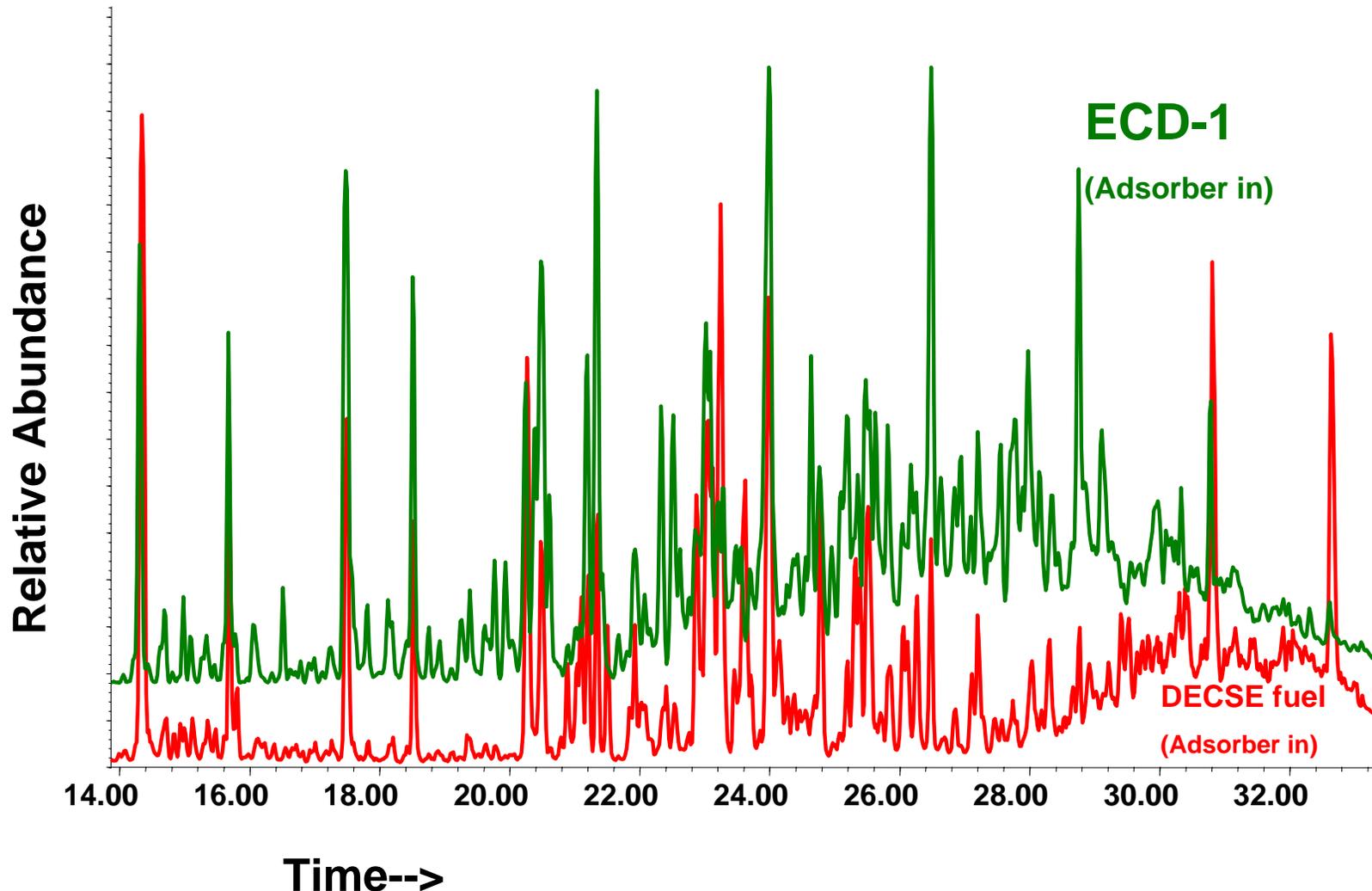
# Large DOC provides extensive HC cracking and lighter HCs to Adsorber

Large DOC vs no DOC, 0.4 DC, ECD-1, Adsorber in



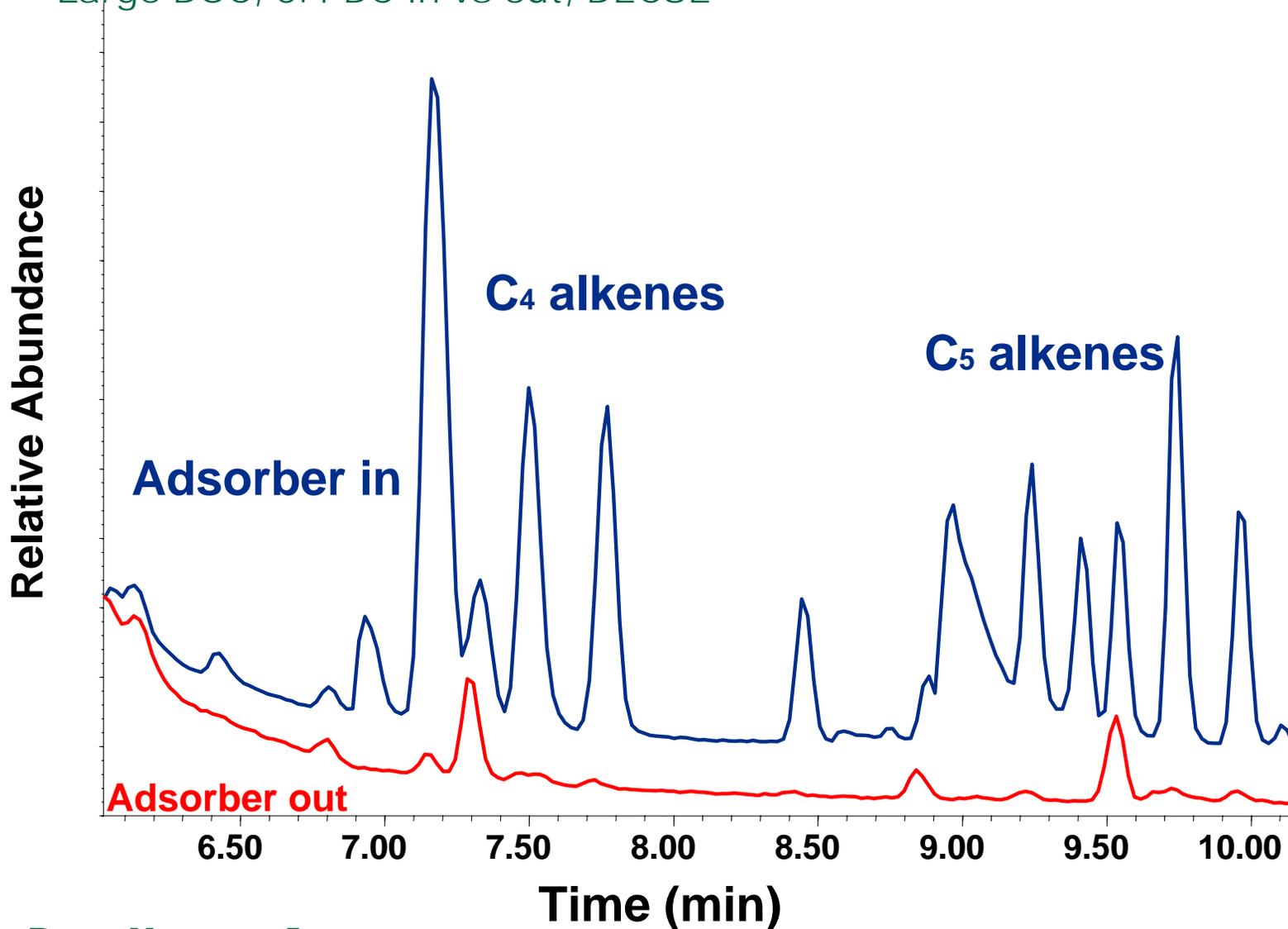
# ECD-1 Fuel yields broader range of HCs at Adsorber inlet than DECSE fuel

Large DOC, 0.4 DC, DECSE vs ECD, Adsorber in

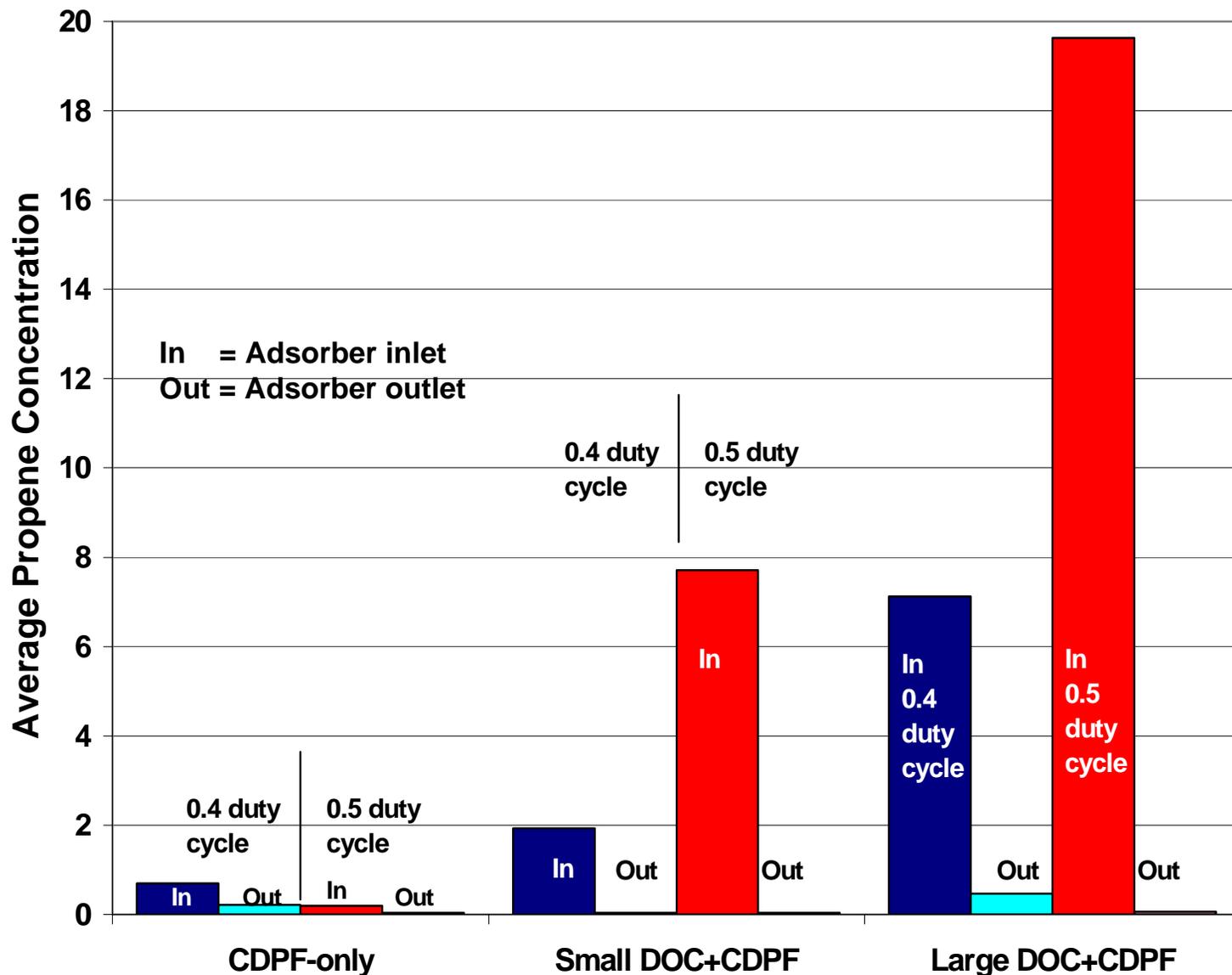


GC-MS shows C4 and C5 HCs at adsorber inlet, all utilized by NOx adsorber catalyst. Light alkenes are formed in upstream catalysts.

Large DOC, 0.4 DC in vs out, DECSE



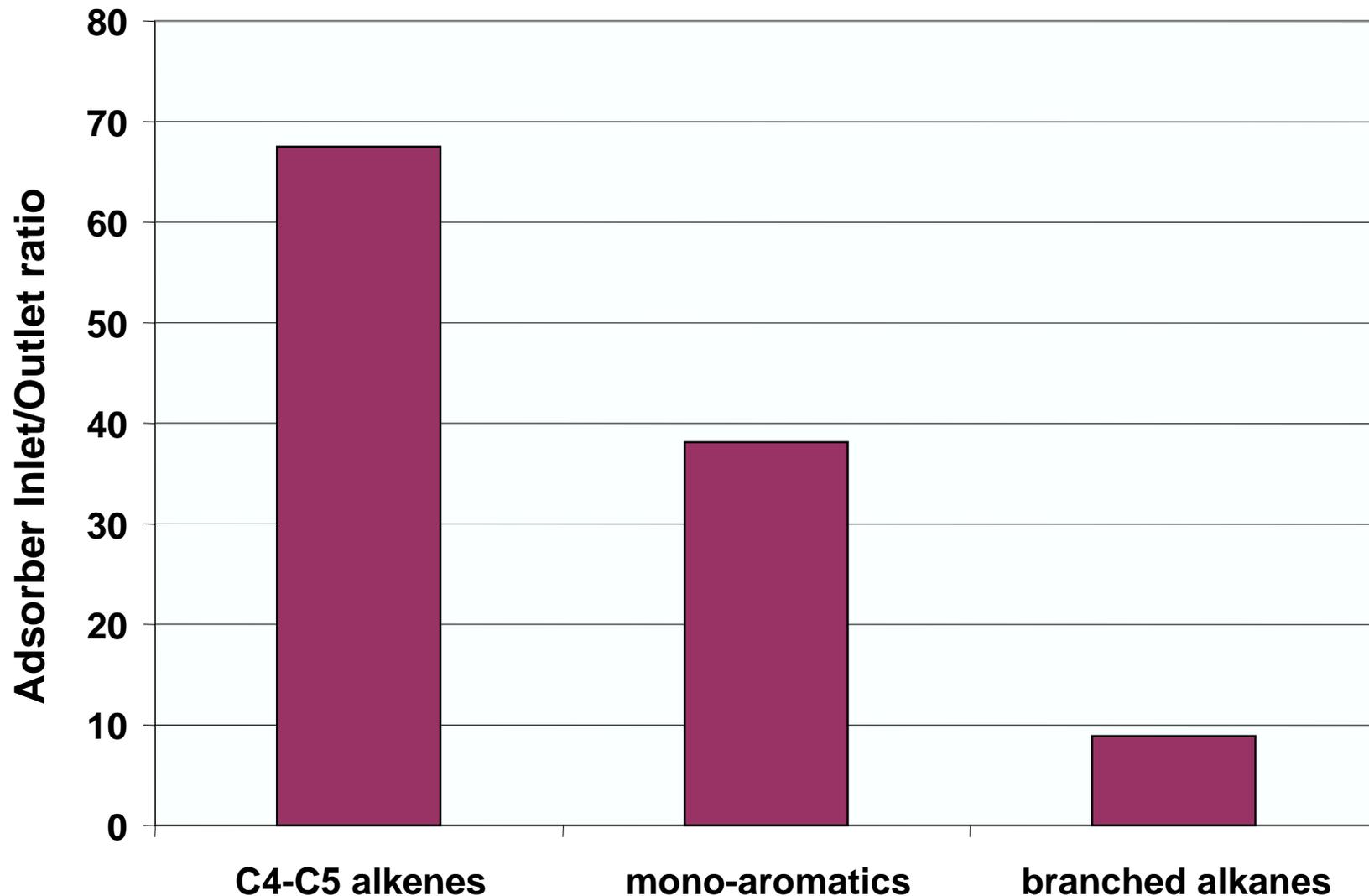
# Oxidation catalysts promote propene formation, readily utilized by NOx adsorber



- Data from FTIR
- Larger diesel oxidation catalyst (DOC) makes most propene
- Richest calibration produces most propene w/ DOC
- Duty cycle is fractional on time for periodic in-pipe injector

Light alkenes and mono-aromatics are readily utilized by NO<sub>x</sub> adsorber. Branched alkanes are less preferred. *Are aromatics good?*

Average adsorber inlet/outlet concentration of families of compounds shown for several cases, both ECD-1 and DECSE fuels, with oxidation catalyst and CDPF upstream of NO<sub>x</sub> adsorber.



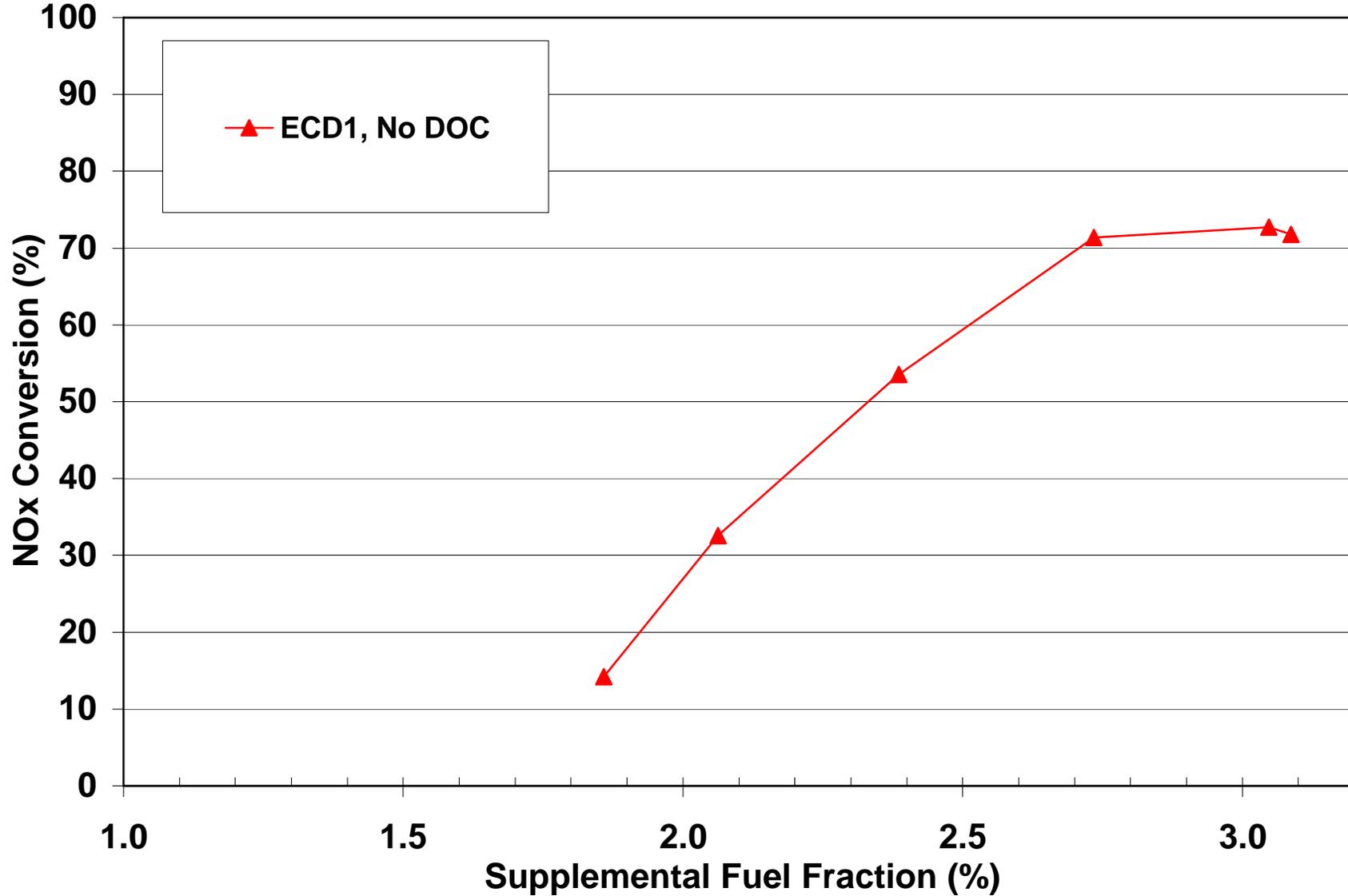
- **Monoaromatics and light alkenes**
  - Formed in exhaust from raw fuel
  - Well utilized by NO<sub>x</sub> adsorber
  
- **All tailpipe HC emissions are below NTE limit of 0.21 g/hp-hr**

We have shown that fuel cracking in DOCs provides different species to the NO<sub>x</sub> adsorber.

What affect does this have on NO<sub>x</sub> reduction?

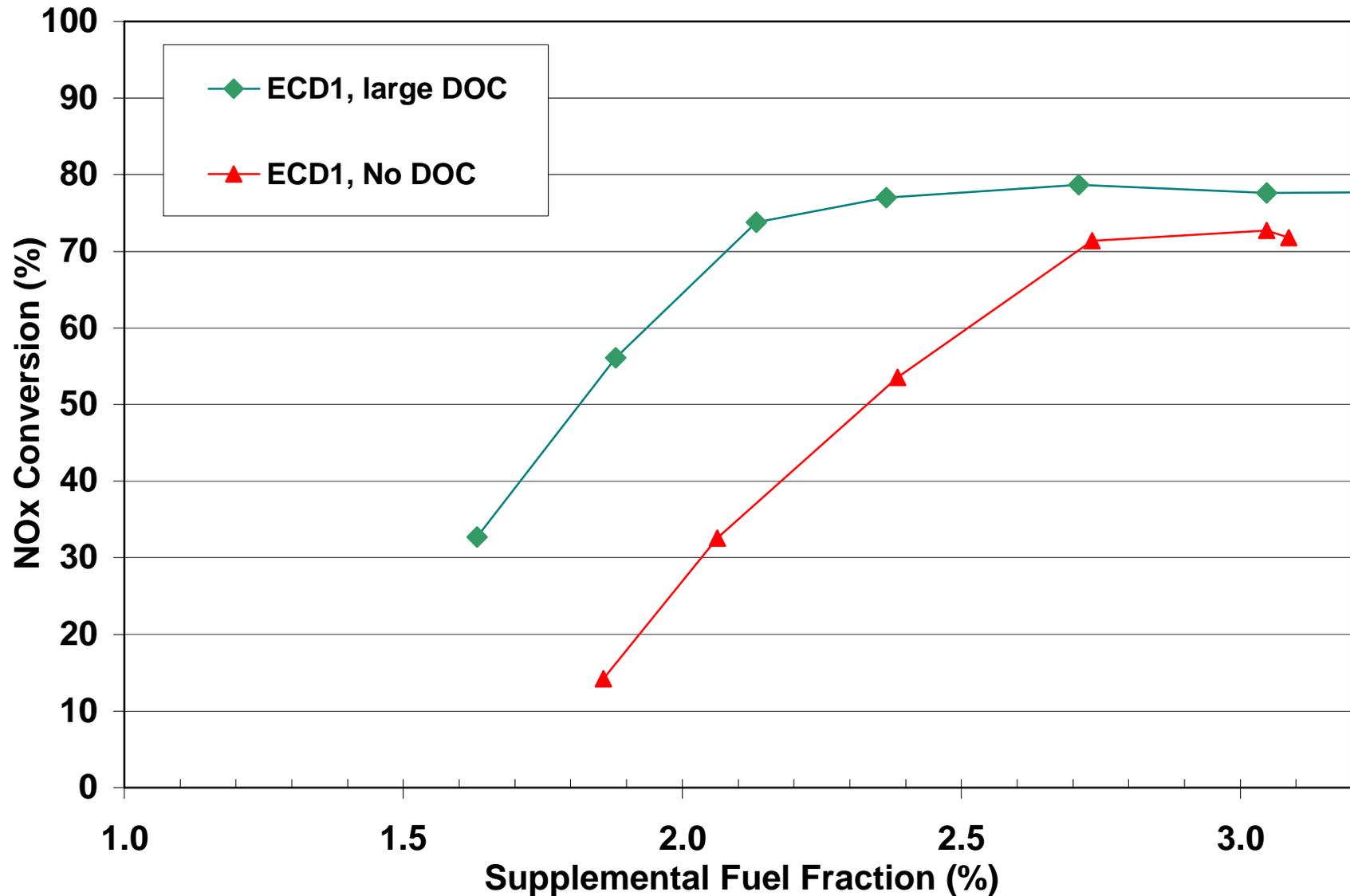
# With no upstream DOC, 70% NOx reduction achieved at ~2.7% excess fuel

Full Load, Rated Speed condition, 600C Catalyst temperature



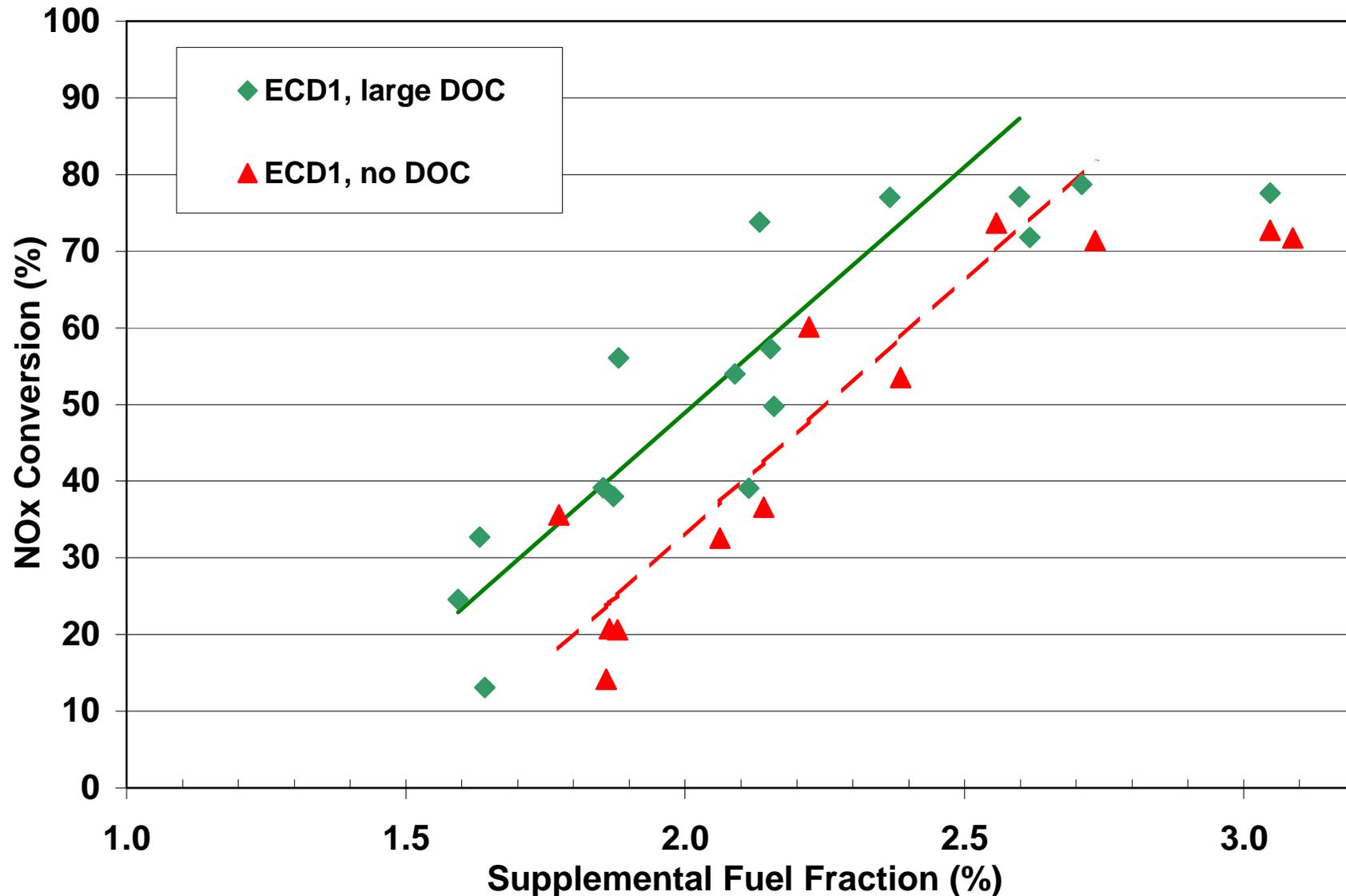
# Fuel cracking in DOC lowers fuel penalty for equivalent NOx reduction

Full Load, Rated Speed condition, 600C Catalyst temperature



# Data from multiple runs shows consistent 10% reduction in fuel penalty with DOC

Full Load, Rated Speed condition, 600C Catalyst temperature



# Summary and Conclusions-1

- **Light alkenes, mono-aromatics preferred by NO<sub>x</sub> adsorber**
  - Branched alkanes not as good
  - Suspect an increase in HC sensitivity at lower temperatures (we were at 600°C)
  - Understanding preferred HC species may help choose “best” certification fuel
    - Many “clean” diesel fuels are low aromatic

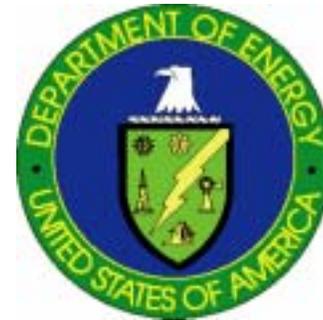
# Summary and Conclusions-2

- ~70% NO<sub>x</sub> reduction achieved at 600 °C NTE condition
  - Caveats:
    - Large, “young” catalyst (150-200 hours)
      - Negligible sulfur poisoning, no desulfations as yet
    - High engine-out NO<sub>x</sub> (~5 g/hp-hr)
    - Only 2 - 2.5% excess fuel
  - 70% NO<sub>x</sub> reduction will require <1.0 g NO<sub>x</sub>/hp-hr **engine-out** in 2010 to meet NTE
  - 2.0 g NO<sub>x</sub>/hp/hr engine-out will require **>85%** reduction
    - Larger/improved adsorber, more frequent regen, best reductant
- NTE imposes *significant* challenge

# Acknowledgments

- **Program sponsors:**

Gurpreet Singh, Kevin Stork, OFCVT



- **Industrial Partners:**

Xinqun Gui, Shouxian Ren



Ken Price, Danan Dou

**DELPHI**