

Low-Temperature Hydrocarbon/CO Oxidation Catalysis in Support of HCCI Emission Control

CRADA: PNNL – Caterpillar

PNNL:

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Caterpillar:

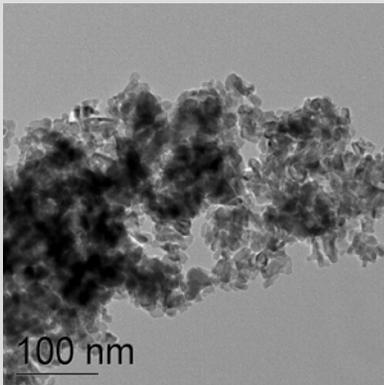
Ron Silver, Svetlana Zemskova, Colleen Eckstein,
Bethanie Moss

2007 DEER (Diesel Engine-Efficiency &
Exhaust Reduction) Conference
Detroit, Michigan
August 15, 2007

Overview

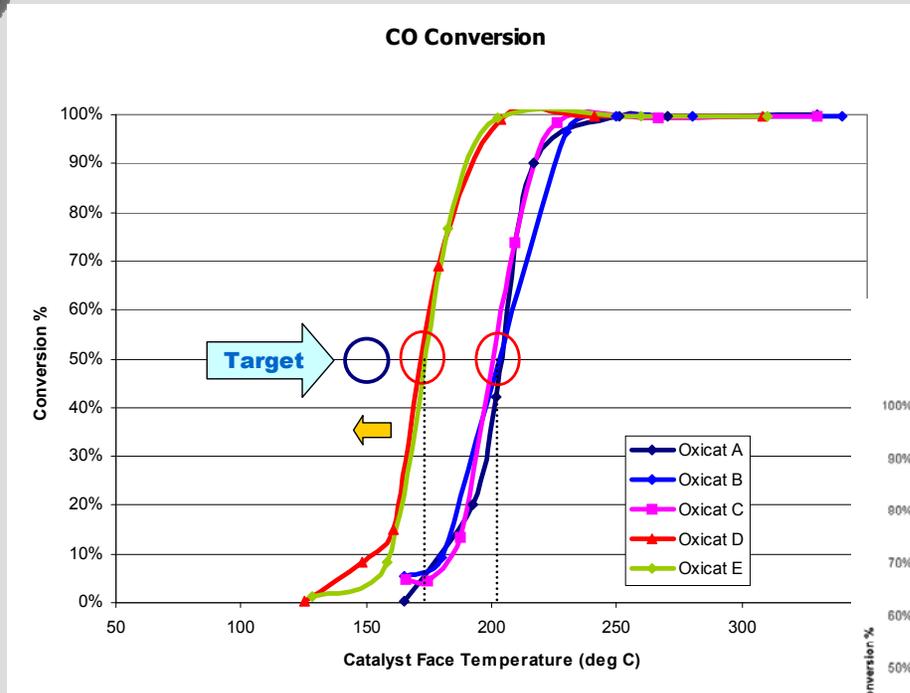
Low-Temperature Oxidation Catalysts for HCCI Emissions Control

- ▶ HCCI shows promise for meeting 2010 HD NO_x limits (Duffy *et al.*, DEER 2004)
 - One of the major hurdles with implementation is high hydrocarbon (up to 2000 ppm C₁) and CO emissions (0.1-0.4%)
 - Low exhaust temperatures are below typical light-off for standard oxidation catalysts
- ▶ Program initiated Summer 2004 (at PNNL) to survey work in low temperature oxidation (CO) and propose roadmap



Objectives

Develop low-temperature HC & CO oxidation catalysts to enable HCCI application

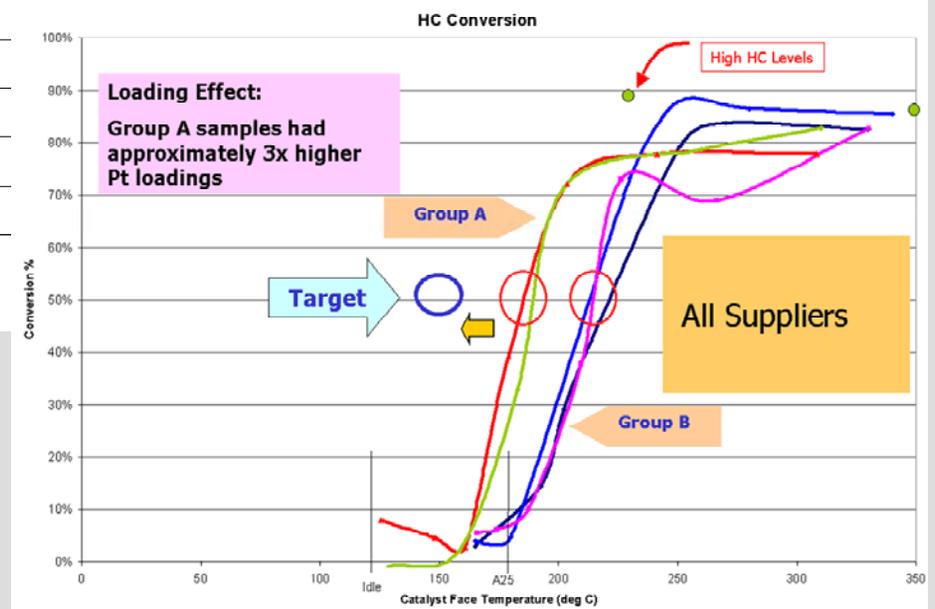


Specifications to vendors:

HC oxidation: 90% at 175°C and higher
HC light-off: 50% at < 150°C

CO oxidation: 99% at higher temperatures
CO light-off: 50% at < 150°C

Akin to the cold start problem, except the exhaust never reaches light-off temperatures on commercial catalysts.



Technical Summary

Low Temperature CO/HC Oxidation Catalyst Literature Survey

- Multi-component Pt systems
- Nano-phase Au systems
- Other PGM (e.g. Pd, Ru)
- Non PGM (e.g. Co, Cu, Ag, Sn)

Extensive catalyst synthesis & screening efforts (>75 formulations to date):

► Supports

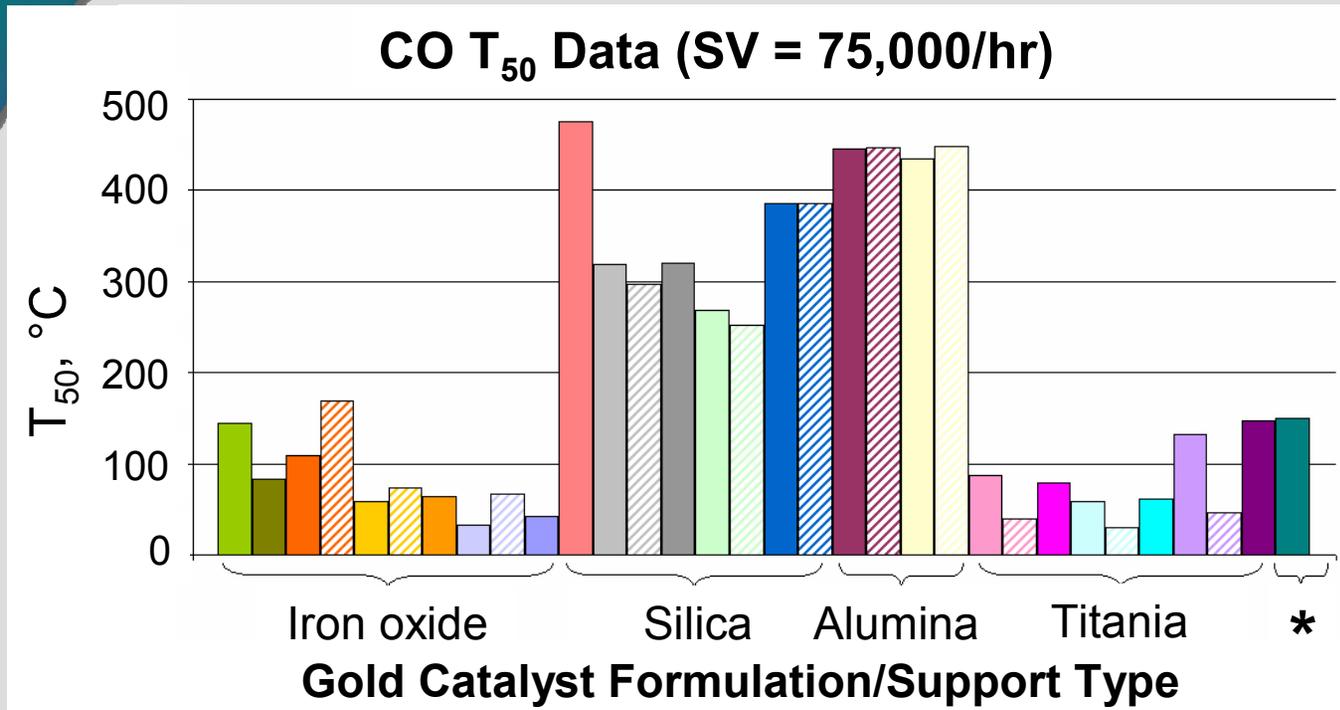
- Engelhard γ -Al₂O₃, Aldrich SnO₂, Davison SiO₂
- Multiple CeO₂ formulations
- Multiple Ce_xSn_yO₂, Ce_xPr_yO₂, Ce_xTb_yO₂ blends
- CeO₂/ γ -Al₂O₃ sequential formulations
- Other supports employed: ZnO₂, ZrO₂, Ce-Y zeolite, ZSM-5

► Metals

- Predominantly Pt- & Pd-based; multiple Rh & Ru formulations also interrogated
- Multi-component formulations combining PGMs Pd, Pt, Rh, Ru, & non-PGMs Mn, Co, Ni
- Multi-component Pt/Sn, Pt/Ce, & Pd/Ce on γ -Al₂O₃ and CeO₂

Technical Summary

Nano-Phase Gold (Au) Catalyst Investigations

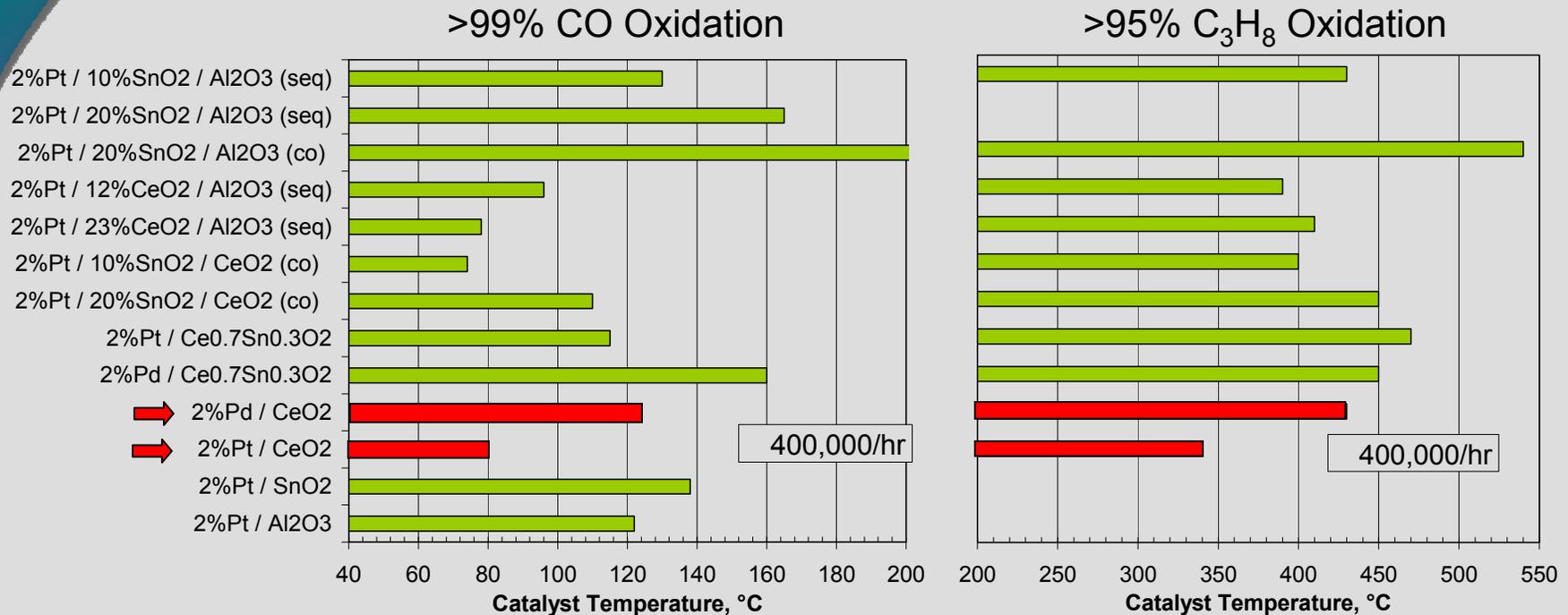


Testing currently in progress to evaluate durability and suitability for monolith coating.

- ▶ Extensive literature search assisted in narrowing selection for study.
- ▶ Four (4) 1-5% Au catalyst supports interrogated; *2%Pt/ γ -Al₂O₃ tested & shown for comparison.
- ▶ Various formulations include variables such as precursor materials, preparation/drying conditions and calcination temperature.

Technical Summary

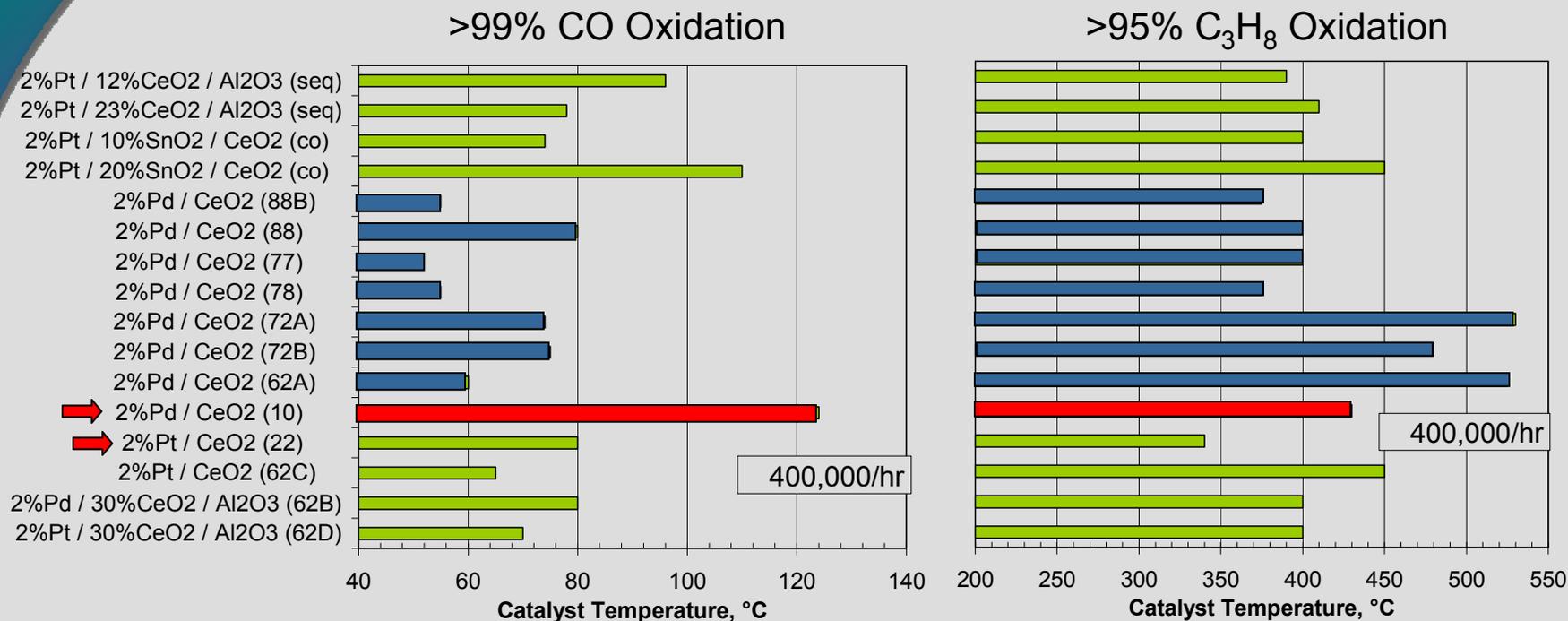
Initial Screening Efforts – CO, C₃H₆, C₃H₈ & CH₄ investigated



- ▶ Completed screening activities on initial catalyst formulations.
- ▶ GHSV 400K shown; 200K & 800K GHSV also characterized.
- ▶ Targeted activity achieved for CO.
 - 50% oxidation at < 150°C; 99% oxidation at higher temperatures
- ▶ **Pt/CeO₂ & Pd/CeO₂** systems show promise, warrant further investigation

Technical Accomplishment Summary – PNNL

Target system: Pd/CeO₂ – CO & C₃H₈ activity shown



- ▶ GHSV 400K hr⁻¹ shown; 200K & 800K hr⁻¹ also characterized
- ▶ Screening efforts include additional **10+ Pd/Pt CeO₂**-based formulations
- ▶ Excellent low-temperature activity achieved with re-formulated **Pd/CeO₂** system; showing improvement with C₃H₈ activity

Technical Accomplishment Summary

2%Pd/CeO₂ System

Summary of Pd- and Ce-source investigations

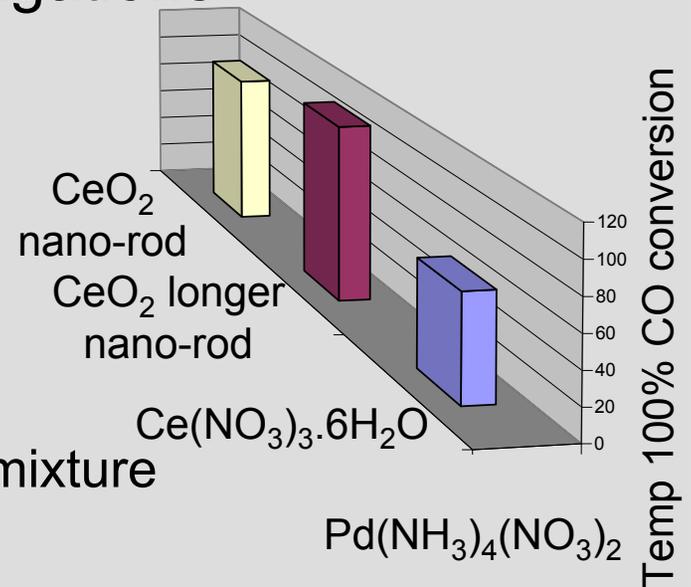
▶ Pd-source:

- ✓ Pd(NO₃)₂
- ✓ Pd(NH₃)₄(NO₃)₂
- Pd-acetyl acetonate (PdACAC)

▶ Ce-source:

- Calcination of CeO₂ sol and surfactant mixture
- ✓ Decomposition of Ce(NO₃)₃•6H₂O
- Calcination of CeO₂ nano-rod solution
- Calcination of CeO₂ *longer* nano-rod solution

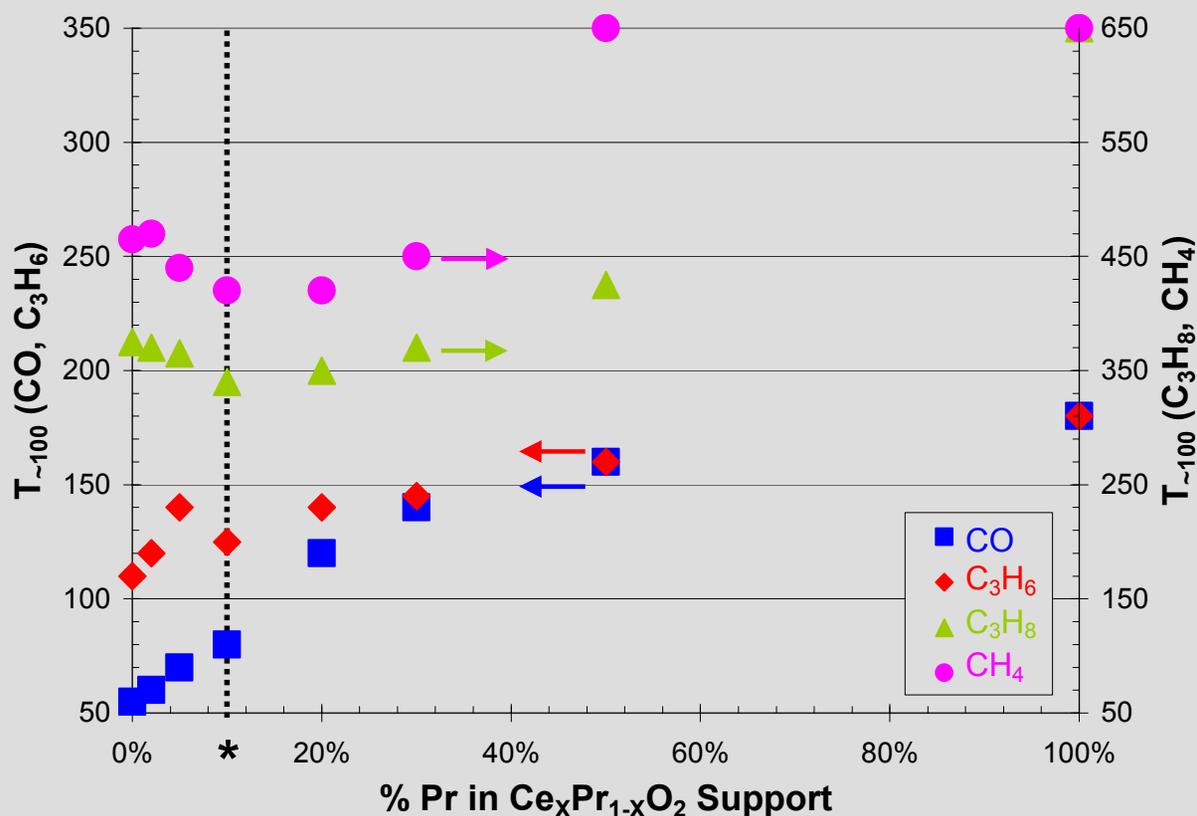
- ▶ Significant improvements made in low temperature activity [T₉₉(CO)~60°C]; need to improve higher temperature HC activity (e.g. C₃H₈).



Technical Summary

2%Pd/Ce_xPr_{1-x}O₂ System Investigations

Addition of transition metals praseodymium (Pr) and terbium (Tb) believed to enhance low-temperature REDOX capacity of the CeO₂ catalyst, improving the low-temperature oxidation capacity.



Ferrer, V. et al *Catal. Today*
2005, 107-108, 487-492

Logan, A. D. et al *J. Mater.*
Res. **1994**, 9, 468-475

X = 1 [CeO₂], 0.98,
0.95, 0.9, 0.8, 0.7,
0.5, 0 [PrO₂]

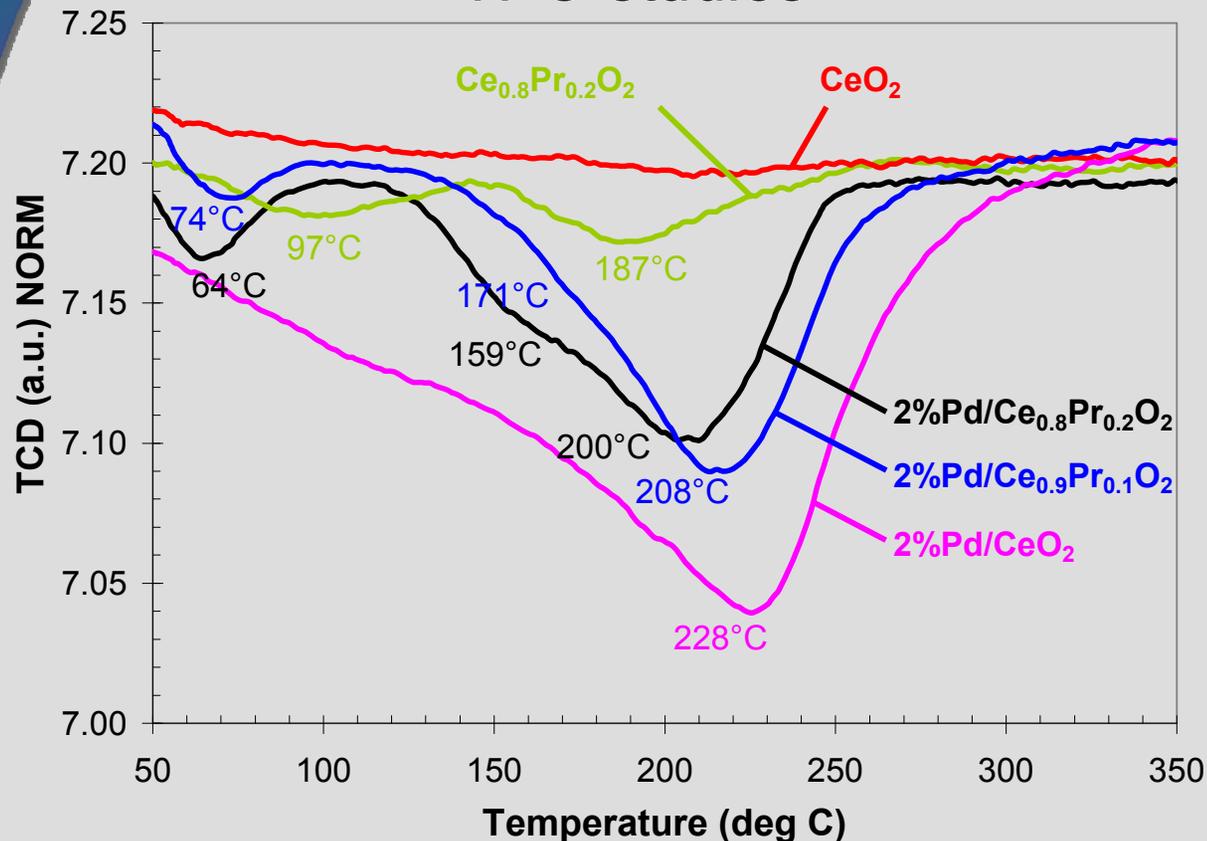
Pd source:
Pd(NH₃)₄(NO₃)₂

Ce/PrO₂ source:
decomposition of
Ce & Pr(NO₃)₃•6H₂O
solutions

Technical Summary

2%Pd/Ce_xPr_{1-x}O₂ System Investigations

TPO studies



Shoulder at 159-171°C is due to Pr, and more noticeable upon ↑ Pr.

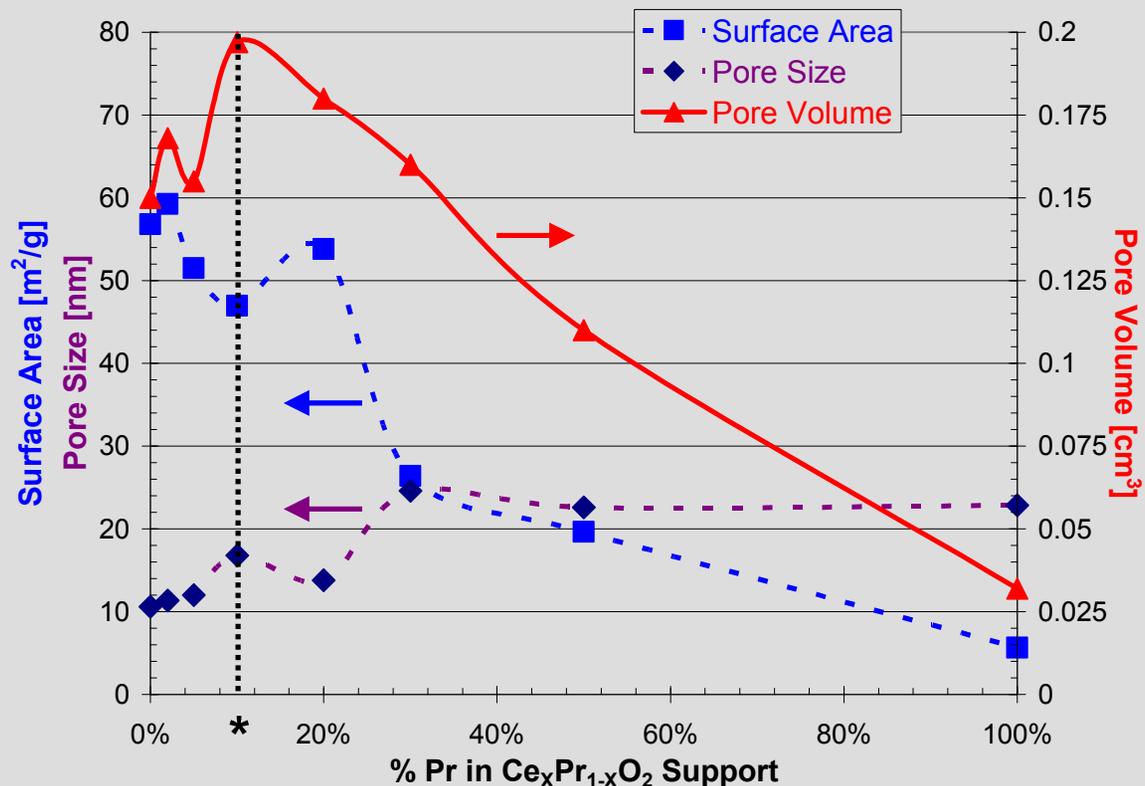
This is seen again by Pd oxidation at 64-74°C.

200-228°C is Pd oxidation and more readily oxidized as Pr ↑ (i.e. ↑ Pr increased interaction of Pd with CeO₂ support).

Technical Summary

2%Pd/Ce_xPr_{1-x}O₂ System: BET Results

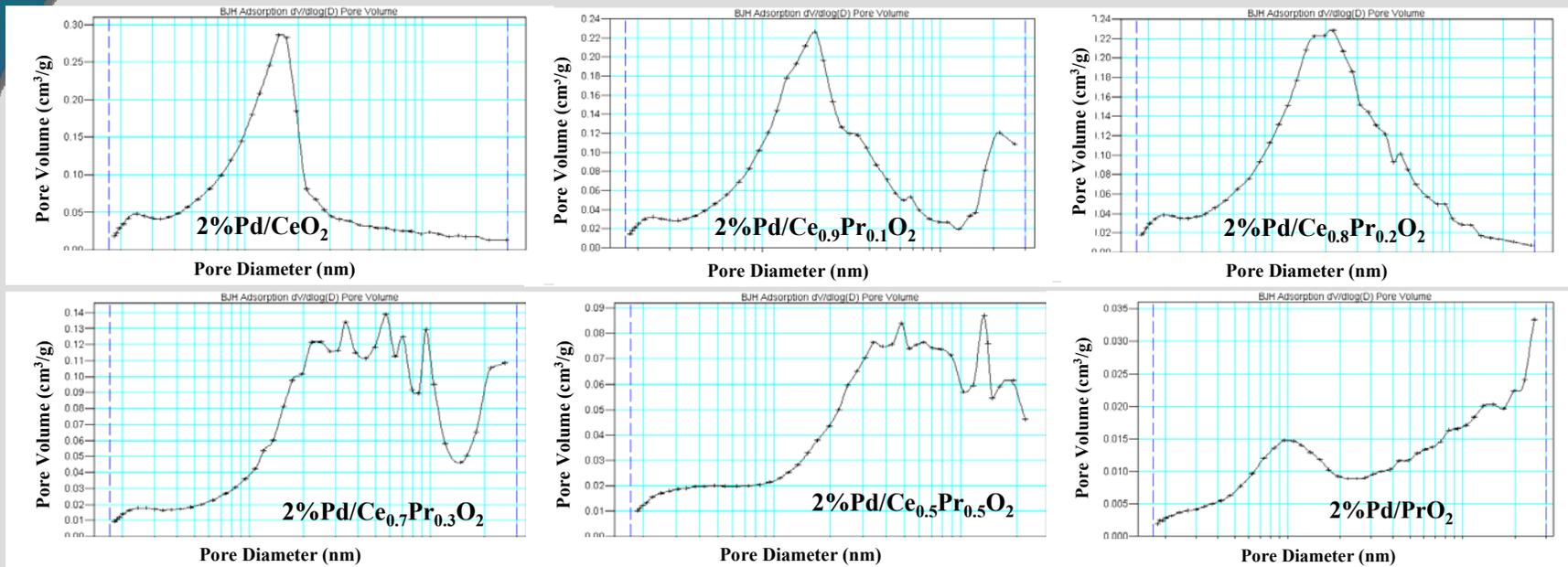
Total pore volume reaches maximum (*) at 10% Pr.



- ▶ Small amounts of Pr (0-20%) believed to not reduce surface area of CeO₂, larger amounts (>20%) impact the surface up to 100% PrO₂ with surface area <10 m²/g.

Technical Summary

2%Pd/Ce_xPr_{1-x}O₂ System: Pore Distribution



- ▶ 10%-20% Pr brings in larger (≥ 20 nm) pores, shifts the maxima slightly to larger pores asymmetrically.
- ▶ $>20\%$ significantly decreases the maxima with drastic broadening of the peak towards the larger pore sizes asymmetrically.

Technical Summary

2%Pd/Ce_xPr_{1-x}O₂ System: Pd Dispersion

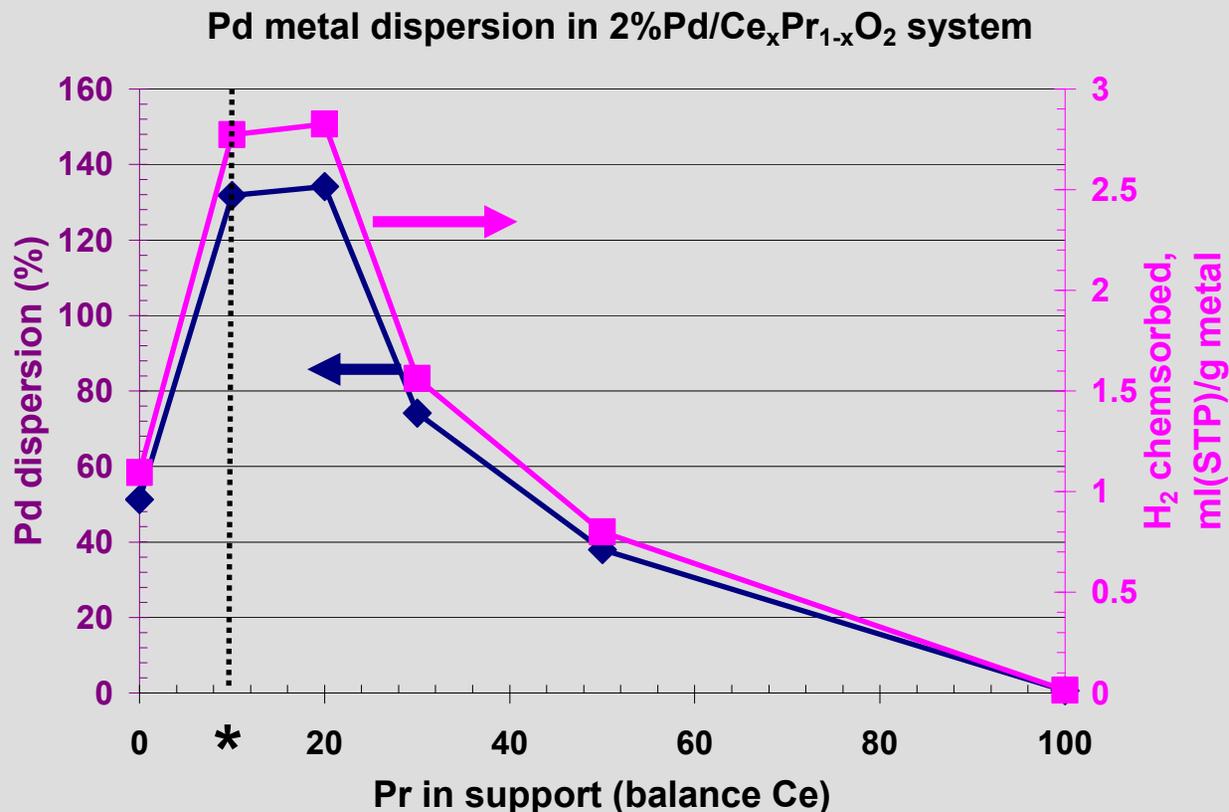
Effective Pd dispersion maximized at 10-20% Pr loading in Ce_xPr_{1-x}O₂ support.

Increased synergy of Pd with support at 10-20% Pr loading; 'spill-over' effect* results in >100% effective dispersion.

* Gatica, J. et al *J. Phys. Chem. B* 2001, 105, 1191-1199

De Leitenburg, C. et al *J. Cat.* 1997, 166, 98-107

Eriksson, S. et al *Appl. Cat. A: Gen.* 2007, 326, 8-16



Optimal metal-support interaction at 10-20% Pr loading.

Technical Summary

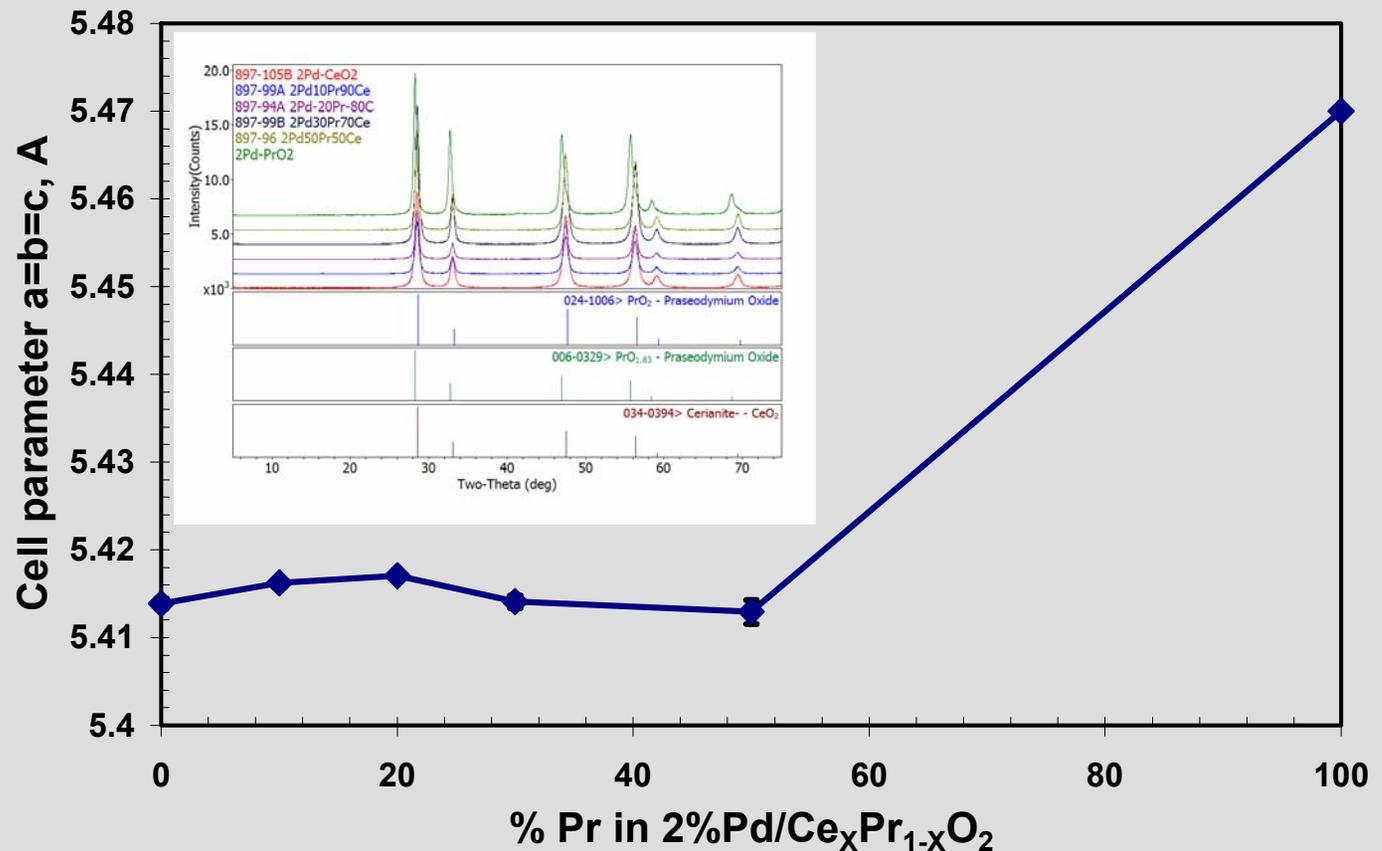
2%Pd/Ce_xPr_{1-x}O₂ System: XRD Analyses

10%-20% Pr results in 'swelling' of the crystal structure.

This is lost with >20% Pr.

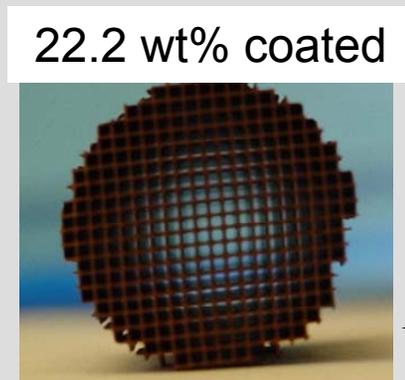
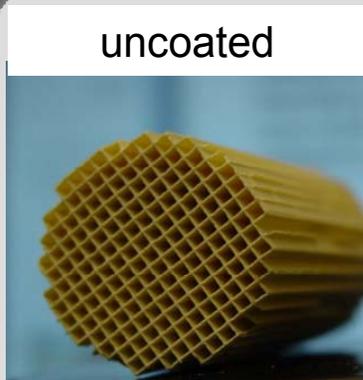
Structure similar to PrO₂ (versus PrO_{1.83}) would account for no XRD shift from 10-50% Pr.

Crystal cell parameter (cubic structure)



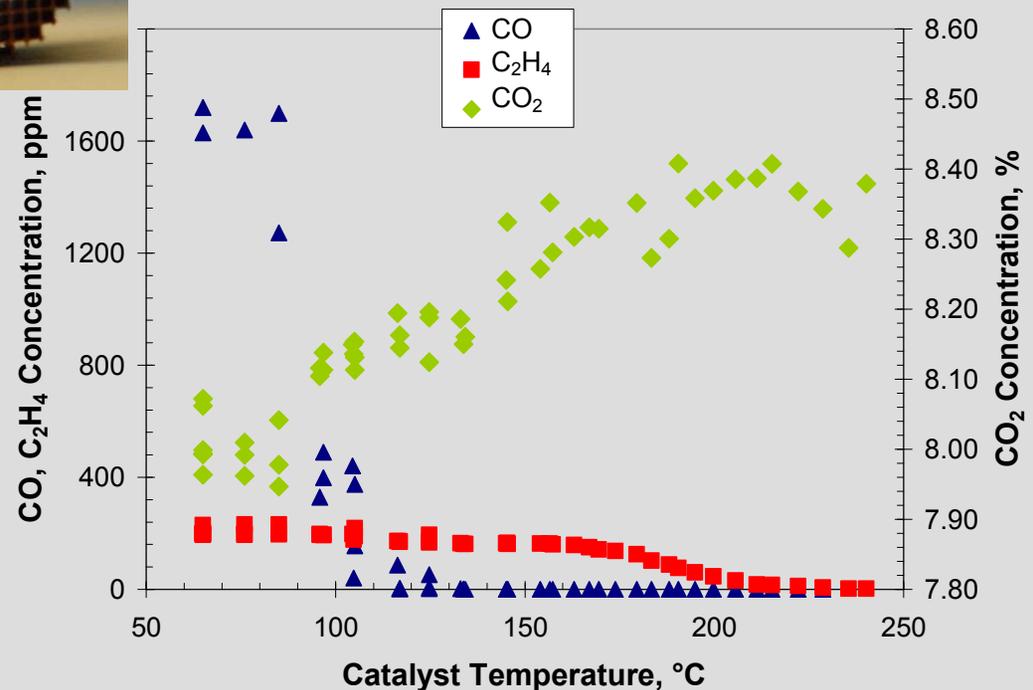
Technical Summary

Catalyst core test efforts – preliminary results



- ▶ Core test bench on-line
- ▶ Currently testing first cores
 - 2%Pd / Ce_{0.8}Pr_{0.2}O₂
 - 2.0 g catalyst on 9.0 g core (22.2 wt%)
 - Catalyst thickness ~77μm (ρ ~ 1.3 g/cm³)
 - SV = 25,000/hr

- ▶ CO activity very similar to 200,000 hr⁻¹ on powder catalyst; powder & core bench correlate well with one another.
- ▶ CO target <150°C achieved

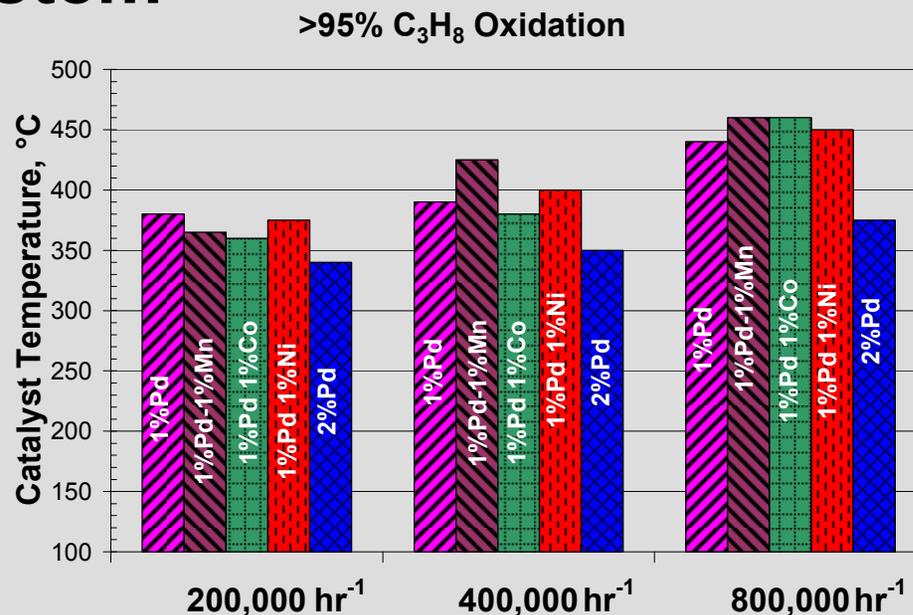
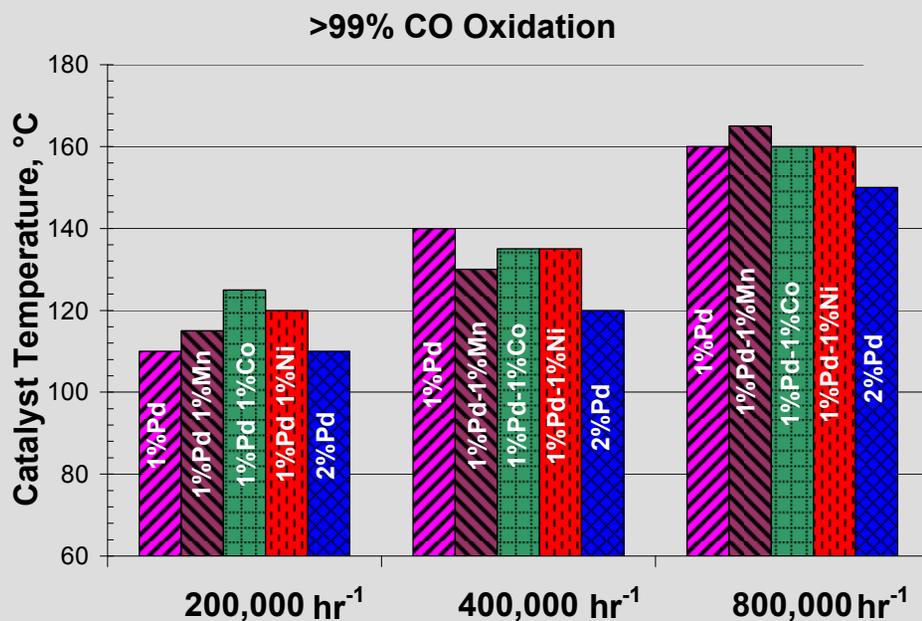


Technical Summary

2%Pd/Ce_{0.8}Pr_{0.2}O₂ System

Non-PGMs

- ▶ Investigation into replacing PGM with a non-PGM (Mn, Co, Ni).



- ▶ No significant improvement.
- ▶ This represents just a glimpse; not comprehensive.

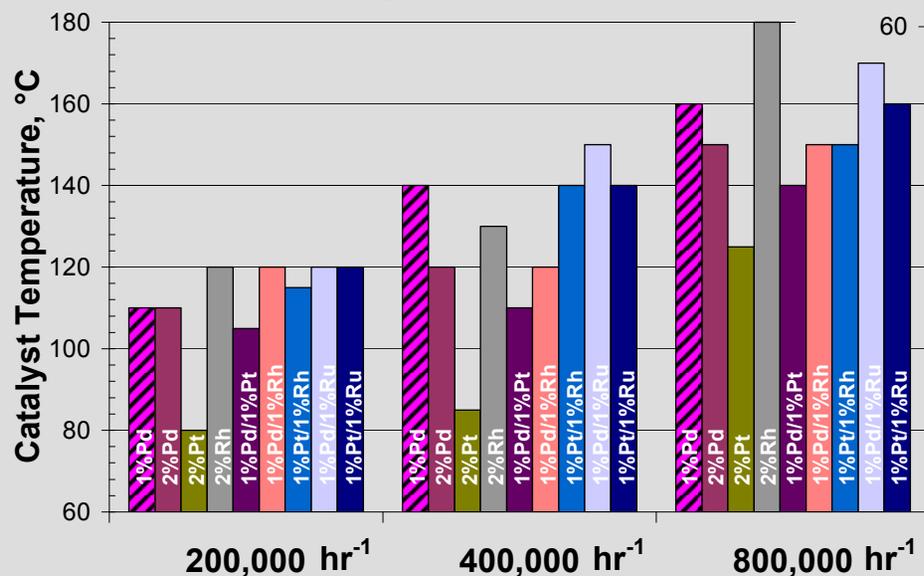
Technical Summary

2%Pd/Ce_{0.8}Pr_{0.2}O₂ System

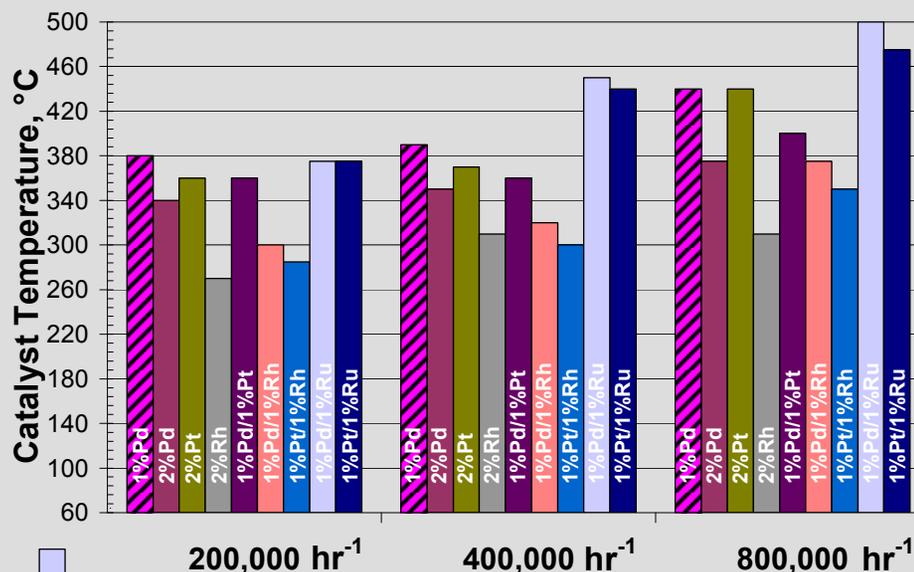
Other-PGMs

- Investigation into the effect of other PGMs, including Pt, Rh, Ru.

>99% CO Oxidation



>95% C₃H₈ Oxidation



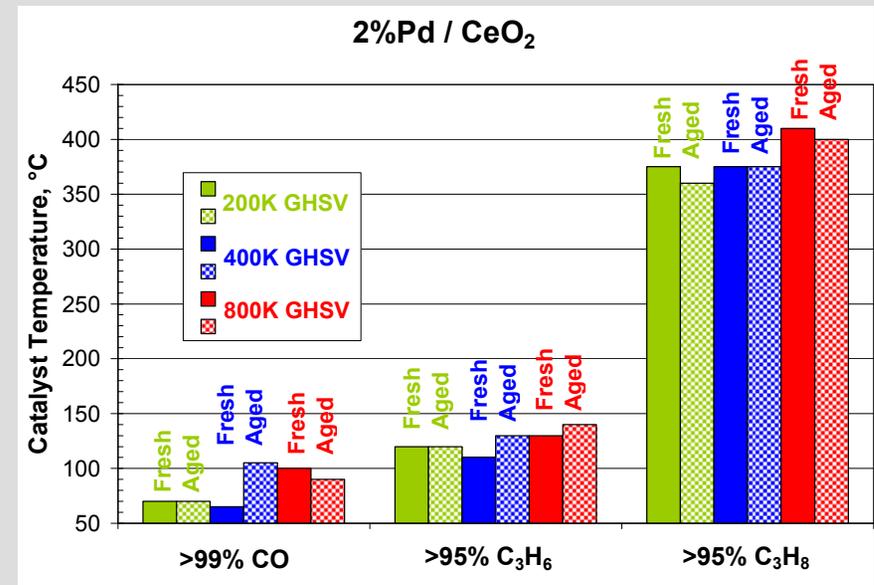
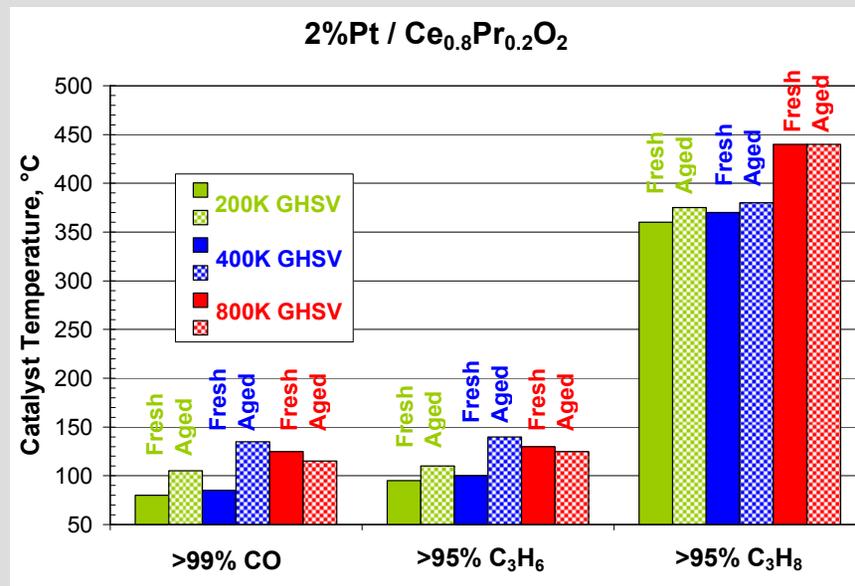
- Pt excellent for CO, olefin oxidation.
- Rh excellent for paraffin oxidation.
- Pt/Rh catalyst is promising.

Technical Summary

2%Pd/Ce_xPr_{1-x}O₂ System:

Preliminary Durability Investigations

- ▶ Results of hydrothermal aging tests.
- ▶ Samples aged in 10% H₂O in air at 350°C for 100 hours.



- ▶ Effect of aging:
 - Minimal effect on Pd.
 - Slight deactivation of Pt.

Summary

Identified CeO_2 system as promising area for investigation. Results of incorporating Pr into support has decreased the temperature required for activity.

Employing characterization tools (BET, XRD, TPO/TPR, etc.) for the assessment of structure-property activity relationships.

Blending in of 10% to 20% Pr 'swells' the oxide crystal structure; >20% Pr appears to cause loss of smaller pores (<20nm) and loss of surface area.

Increased synergy of precious metal with 10% to 20% Pr blended into the CeO_2 support.

Beginning core-configured investigations.

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U.S. Department of Energy

Energy Efficiency and Renewable Energy

FreedomCAR & Vehicle Technologies Program

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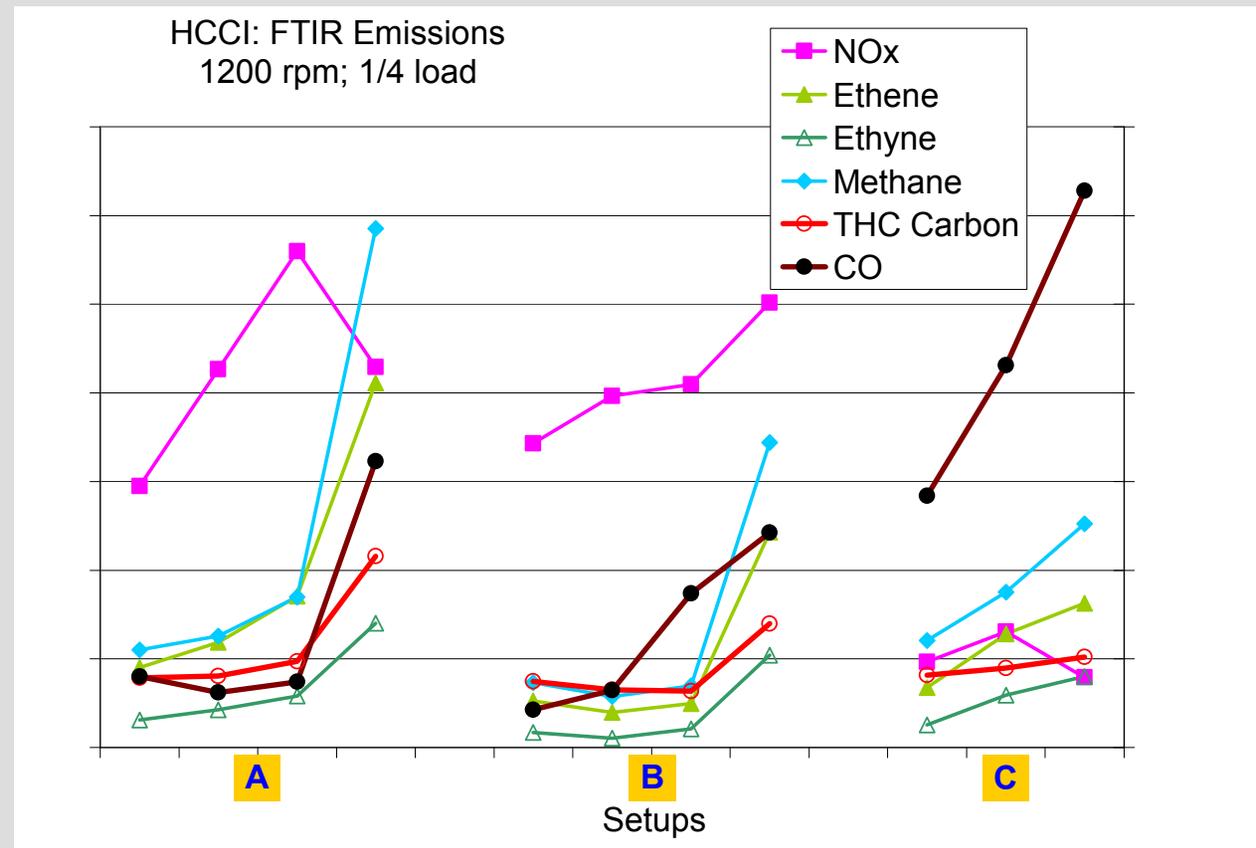
Pacific Northwest National Laboratory
U.S. Department of Energy

Appendix

HCCI emission hydrocarbon speciation efforts

Caterpillar speciation efforts complete for HCCI exhaust characterization.
Vendor supplied catalysts tested.

Trade-off:
NO_x versus CO levels



Cat ID and composition	88C, 2Pd- CeO₂	99A, 2Pd- Pr_{0.1}Ce_{0.9}O₂	94A 2Pd- Pr_{0.2}Ce_{0.8}O₂	99B 2Pd- Pr_{0.3}Ce_{0.7}O₂	96 2Pd- Pr_{0.5}Ce_{0.5}O₂	97 2Pd- Tb_{0.5}Ce_{0.5}O₂
BET, m²/g	56.8	47.0	53.8	26.4	19.7	5.94
Pore volume, cc/g	0.15	0.20	0.18	0.16	0.11	0.05
Pore size, nm	10.6	16.8	13.8	24.6	22.6	31.7